



# Lattice Boltzmann methods for CFD

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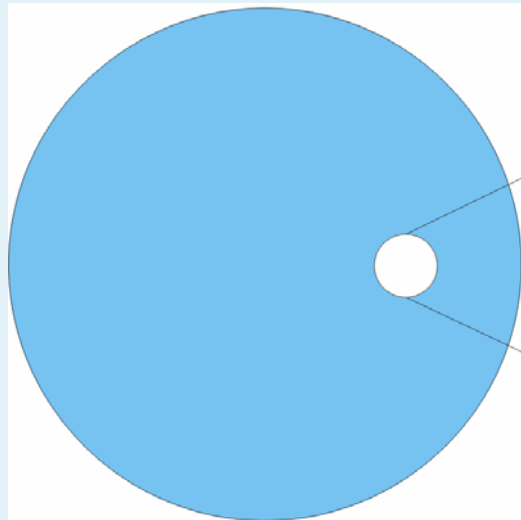
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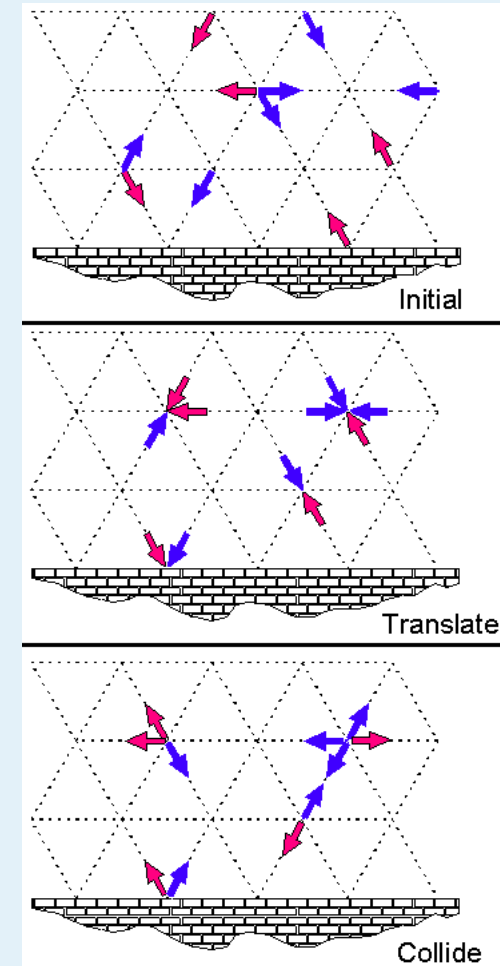
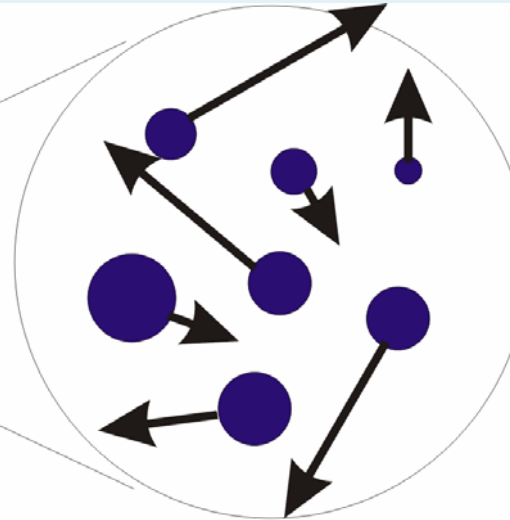
## Overview

- **Lattice Gases:**  
A short trip back to the roots of physics of fluids
- **The mesoscopic picture:**  
The Lattice-Boltzmann equation
- **hydrodynamic limits and moments of distributions**

continuous fluid



particle ensemble  
(real gas)



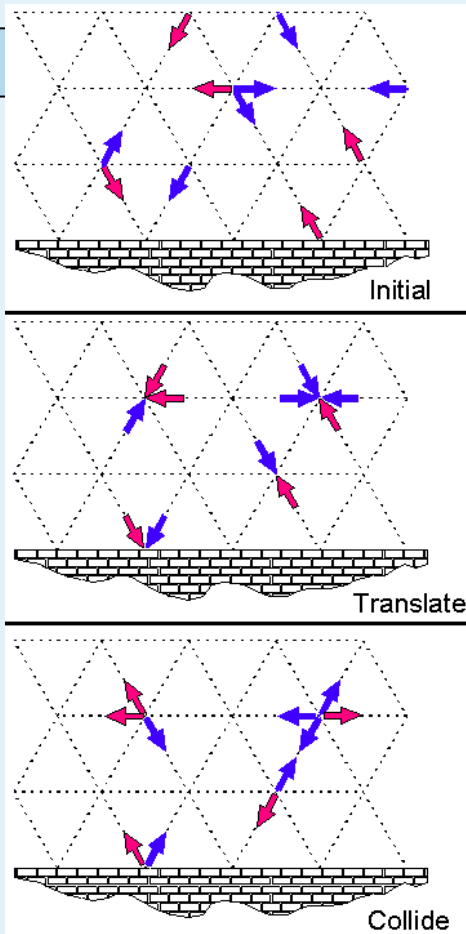
$$p, \nu, \vec{v}(\vec{r}, t), \rho$$

$$m_i, \omega, \vec{v}_i(\vec{r}, t)$$

$$\frac{\partial \vec{u}}{\partial t} + \vec{u} \nabla \otimes \vec{u} = -\nabla p^* + \nu \Delta \vec{u}$$

$$m_i \frac{\partial v_i}{\partial t} = \sum_{i \neq j} \frac{\partial V(\|\vec{r}_i - \vec{r}_j\|)}{\partial \vec{r}_j}$$

$$\vec{e}_i(\vec{r}, t)$$



### Evolution equation for ,digital‘ particles:

$$n_i(\vec{x} + \vec{e}_i \delta t, t + \delta t) - n_i(\vec{x}, t) = \Omega_i$$

### Coupling to ,real world properties‘ via moments:

$$\rho = \sum_{i=0}^{m-1} n_i$$

$$\vec{u} = \frac{1}{\rho} \sum_{i=1}^{m-1} n_i \vec{e}_i$$

$$p_\infty = c_s^2 (\rho - \rho_0)$$

Chapman-Enskog expansion shows:

Dynamics of velocity and pressure is (for  $\text{Kn}, \text{Ma} \rightarrow 0$ )  
equivalent to that given by the Navier-Stokes equations:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot \vec{u} = 0$$

$$\frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u} = -\frac{1}{\rho_0} \nabla p_\infty + \nu \nabla^2 (\rho \vec{u})$$





## Problems

- Lack of Galilean Invariance
- Anomalous velocity dependence of the fluid pressure

$$\langle n_i^{eq} \rangle = \frac{\rho}{b} (1 + e_{i\alpha} u_\alpha / c_s^2 + G Q_{\alpha\beta} u_\alpha u_\beta / 2c_s^4)$$

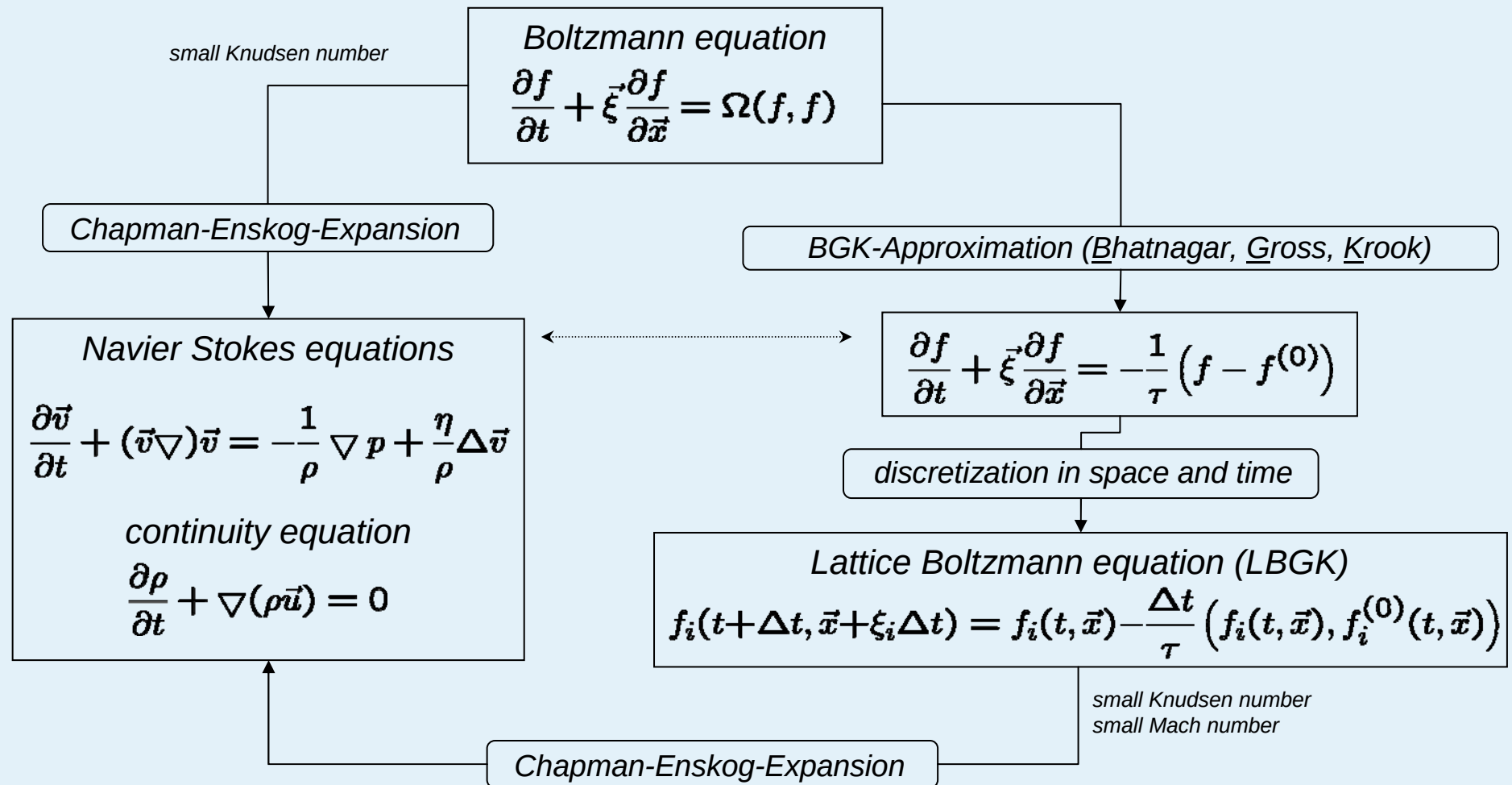
$$G(\rho) = \frac{1 - 2\frac{\rho}{b}}{1 - \frac{\rho}{b}} \neq 1$$

$$\sum_i \langle n_i^{eq} \rangle e_{i\alpha} e_{i\beta} = \rho (g u_\alpha u_\beta + c_s^2 (1 - g Ma^2) \delta_{\alpha\beta})$$

$$g(\rho) = \frac{D}{D+2} G(\rho) \neq 1$$

- Statistical noise
- High viscosity (low „element Re“)
- Exponential complexity of collision operator
- Spurious invariants

## from Boltzmann to Navier Stokes and LBGK





## Lattice-Bhatnagar-Gross-Krook (LBGK) models for Navier-Stokes problems

Starting with the Boltzmann equation

$$\frac{\partial f}{\partial t} + \vec{v} \nabla f = \Omega$$

the phase space can be discretized resulting in

$$\frac{\partial f_i(\vec{x}, t)}{\partial t} + \vec{e}_i \nabla f(\vec{x}, t) = \Omega_i(\{f_j(\vec{x}, t)\}), i, j \in \{1, \dots, n\} \quad (1)$$

Additional simplification (Bhatnagar Gross-Krook):

$\Omega$  is described by a 'Single Time Relaxation Approximation' (STRA) of the form

$$\Omega_i = -\frac{1}{\tau} (f_i - f_i^{eq})$$



Macroscopic flow variables and can be defined as moments of  $f_i$

$$\rho = \sum_{i=0}^{m-1} f_i \quad \vec{u} = \frac{1}{\rho} \sum_{i=1}^{m-1} f_i \vec{e}_i$$

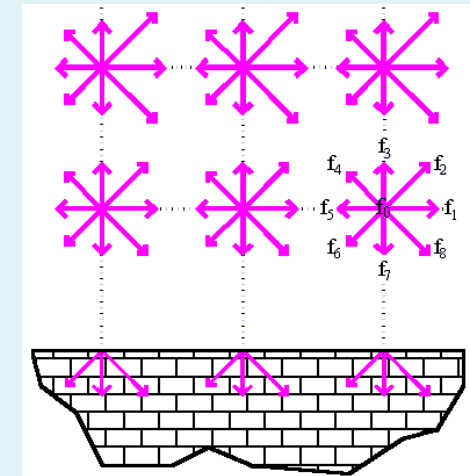
Equations (1) can be solved e.g. by FD schemes

$$f_i(\vec{x} + \vec{e}_i \delta t, t + \delta t) - f_i(\vec{x}, t) = -\frac{1}{\tau} (f_i(\vec{x}, t) - f_i^{eq}(\vec{x}, t))$$

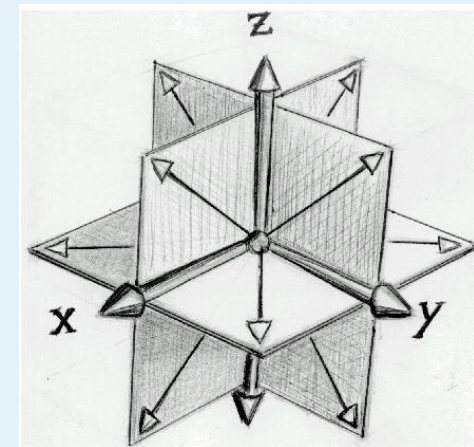
The kinematic viscosity

can be identified as

$$\nu = \frac{2\tau - 1}{6} \frac{\delta h^2}{\delta t}$$



D3Q19 model





The LB-equation 
$$f_i(\vec{x} + \vec{e}_i \delta t, t + \delta t) - f_i(\vec{x}, t) = \Omega_i(\{f_j(\vec{x}, t)\})$$

Typical claims (prejudices ??) found in the literature:

- suited for flows in complex geometries
- efficient for complex fluids (especially multiphase problems)
- easy to vectorize
- very good scaling on parallel machines
- no numerical scheme („cellular automata“)
- easy to program



Do LB methods really do a better job than ,conventional‘ approaches ?  
or  
are they numerically efficient ?

structural advantages:

- **Linear** and **exact** advection operator
- conservative scheme for mass and momentum
- no numerical viscosity
- local shear stress tensor

$$S_{\alpha\beta} = \left( \frac{\Delta t}{2\tau} - 1 \right) \sum_i v_{i\alpha} v_{i\beta} f_i^{(neq)}$$

structural disadvantages:

- conditionally stable
- cartesian grids
- inherently transient scheme
- more DOF per node than Navier-Stokes CFD solvers  
(3/9 in 2D, 13-27/4 in 3D)





## Chapman-Enskog expansion in a nutshell:

rescaling  $\Theta = \frac{\partial \hat{f}}{\partial \hat{t}} + \hat{v} \nabla \hat{f} = -\frac{1}{\varepsilon} (\hat{f}_i - \hat{f}_i^{eq}), \varepsilon = \frac{c_r \tau}{L_r}$

expansion:  $f = \sum_{k=0}^{\infty} \varepsilon^k f^{(k)}, f^{(0)} = f^{(eq)}$

Definition of moments:

$$\rho = \int f d\vec{v} = \int f^{(0)} d\vec{v} \quad \rho u_{\alpha} = \int v_{\alpha} f d\vec{v} = \int v_{\alpha} f^{(0)} d\vec{v}$$

$$D_{\alpha\beta} = \int v_{\alpha} v_{\beta} f d\vec{v}$$

Taking into account terms for  $k=0,1,2, \dots$  results in a hierarchy of equations

$$\Theta^0(\hat{f}^{(0)}) = 0$$

$$\Theta^1(\hat{f}^{(0)}, \hat{f}^{(1)}) = 0$$

$$\Theta^2(\hat{f}^{(0)}, \hat{f}^{(1)}, \hat{f}^{(2)}) = 0$$



Analysis of the first order terms  $\{\hat{f}^{(0)}, \hat{f}^{(1)}, \hat{f}^{(2)}\}$  shows, that the dynamics of the hydrodynamic moments of  $f$  ( $\rho$  and  $\vec{u}$ ) in the limit of low Mach- und Knudsen numbers is described by the Navier-Stokes equations

$$\frac{\partial \rho}{\partial t} + \nabla(\rho \vec{u}) = 0$$

$$\frac{\partial \rho \vec{u}}{\partial t} + \nabla(\rho \vec{u} \vec{u}) = -\nabla p + \nabla \cdot \overline{\tau}$$

$$\overline{\tau} = \mu(\nabla \vec{u} + (\nabla \vec{u})^T) - \frac{2}{3} \mu(\nabla \vec{u}) \overline{I}$$

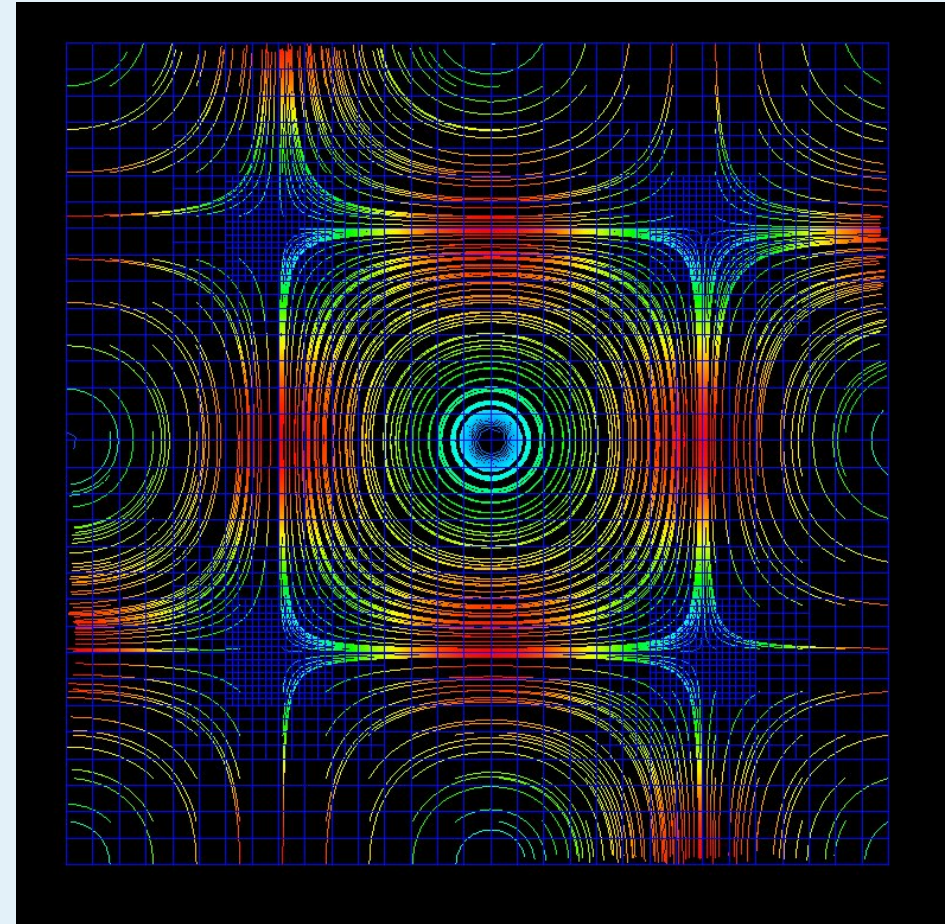


## Computational aspects

- no Poisson equation is solved for the pressure
- Boundary conditions of Dirichlet and Neumann type can (have to) be set via  $f$
- Convergence properties:
  - LBE can be tuned to second-order accuracy with respect to the corresponding solution of one-phase Navier-Stokes flow
- Because of their explicit nature LBGK models are optimally suited for vectorization and parallelization
- For many practical applications LBGK's computational efficiency has been shown to be comparable to state-of-the-art FV, FE or FD discretizations of the corresponding Navier-Stokes problem
- Implicit and multigrid discretizations or FEM and FV variants can be constructed

$$NS = LB + O(Kn^2) + O(Ma^2) + O(dt \cdot Ma) + O(dx^2)$$

→ test case: Taylor vortex





$$E2(T) = \frac{\sqrt{\sum_i (u(\vec{x}, t) - u_{ex}(\vec{x}, t))^2}}{\sum_i u_{ex}(\vec{x}, t)^2}$$

Re=50  
periodic BCs

| level | Ma       | E2       | exponent  |
|-------|----------|----------|-----------|
| 5     | 0,026041 | 0,002272 | -2,075082 |
| 6     | 0,013020 | 0,000550 | -1,904702 |
| 7     | 0,006501 | 0,000140 | -1,973622 |
| 8     | 0,003250 | 0,000034 | -1,989559 |
| 9     | 0,001625 | 0,000008 | -2,001034 |



- Chapman-Enskog Analysis
- Derivation of the discrete Boltzmann equation
- Finite Difference Discretisation
- Multi-Relaxation-Time



## The Boltzmann equation

$$\frac{\partial f(t, \mathbf{v}, \mathbf{x})}{\partial t} + \mathbf{v} \bullet \nabla f(t, \mathbf{v}, \mathbf{x}) = \Omega(t, \mathbf{v}, \mathbf{x})$$

$f$  Particle distribution function

$\Omega$  collision operator

$\mathbf{v}$  microscopic velocity

$\mathbf{x}$  Position



Macroscopic quantities are moments with respect to  $\mathbf{v}$  :

Dichte  $\rho(t, \mathbf{x}) = \int_{-\infty}^{+\infty} f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v}$

Impuls  $\mathbf{u}(t, \mathbf{x}) = \int_{-\infty}^{+\infty} \mathbf{v} f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v}$

pressure tensor (scalar pressure +shear stresses):

$$P_{\alpha\beta}(t, \mathbf{x}) = \int_{-\infty}^{+\infty} (v_{\alpha} - u_{\alpha})(v_{\beta} - u_{\beta}) f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v}$$

$$P_{\alpha\beta}(t, \mathbf{x}) = -\rho u_{\alpha} u_{\beta} + \int_{-\infty}^{+\infty} v_{\alpha} v_{\beta} f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v}$$





collision operator:

mass conservation:

$$\int_{-\infty}^{+\infty} \Omega(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} = 0$$

momentum conservation:

$$\int_{-\infty}^{+\infty} \mathbf{v} \Omega(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} = 0$$



uniform state solution: Maxwell distribution

$$f^{eq}(t, \mathbf{v}, \mathbf{x}) = \frac{\rho}{(2\pi c_s^2)^{D/2}} \exp\left(-\frac{(\mathbf{v} - \mathbf{u})^2}{2c_s^2}\right)$$

continuum limit:

$$Kn = \frac{\lambda_r}{L_r} \ll 1$$

$Kn$  Knudsen number

$\lambda_r$  mean free path of particles

$L_r$  macroscopic reference length



continuum limit:

small deviations from equilibrium:

simplified collision operator

$$\Omega = -\frac{1}{\tau}(f - f^{eq})$$

$\tau$  relaxation time

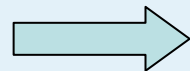
Ansatz: solution  $f$  should only depend on  
macroscopic (i.e. hydrodynamic and beyond) moments



zero order moment of the Boltzmann-equation:

$$\int_{-\infty}^{+\infty} \left( \frac{\partial f(t, \mathbf{v}, \mathbf{x})}{\partial t} + \mathbf{v} \bullet \nabla f(t, \mathbf{v}, \mathbf{x}) - \Omega(t, \mathbf{v}, \mathbf{x}) \right) d\mathbf{v} = 0$$
$$\frac{\partial}{\partial t} \int_{-\infty}^{+\infty} f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} + \nabla \bullet \int_{-\infty}^{+\infty} \mathbf{v} f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} = 0$$

continuity equation:


$$\frac{\partial}{\partial t} \rho(t, \mathbf{x}) + \nabla \bullet \rho \mathbf{u}(t, \mathbf{x}) = 0$$



first order moment of the Boltzmann-equation:

$$\int_{-\infty}^{+\infty} \mathbf{v} \left( \frac{\partial f(t, \mathbf{v}, \mathbf{x})}{\partial t} + \mathbf{v} \bullet \nabla f(t, \mathbf{v}, \mathbf{x}) = \Omega(t, \mathbf{v}, \mathbf{x}) \right) d\mathbf{v}$$

$$\frac{\partial}{\partial t} \int_{-\infty}^{+\infty} v_{\alpha} f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} + \frac{\partial}{\partial x_{\beta}} \int_{-\infty}^{+\infty} v_{\alpha} v_{\beta} f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} = 0$$

where  $\int_{-\infty}^{+\infty} v_{\alpha} v_{\beta} f(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} = \rho u_{\alpha} u_{\beta} + P_{\alpha\beta}(t, \mathbf{x})$

momentum equation:

$$\Rightarrow \frac{\partial}{\partial t} \rho u_{\alpha}(t, \mathbf{x}) + \frac{\partial}{\partial x_{\beta}} \rho u_{\alpha} u_{\beta}(t, \mathbf{x}) + \frac{\partial}{\partial x_{\beta}} P_{\alpha\beta} = 0$$



Problem:

pressure tensor should be expressed in macroscopic quantities!

first order appr.:  $f(t, \mathbf{v}, \mathbf{x}) \approx f^{eq}(\rho(t, \mathbf{x}), u(t, \mathbf{x}), \mathbf{v})$

$$P_{\alpha\beta}^{(0)}(t, \mathbf{x}) = \int_{-\infty}^{+\infty} (v_{\alpha} - u_{\alpha})(v_{\beta} - u_{\beta}) f^{eq}(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} = c_s^2 \rho(t, \mathbf{x})$$

Euler equation:

$$\longrightarrow \frac{\partial}{\partial t} \rho u_{\alpha}(t, \mathbf{x}) + \frac{\partial}{\partial x_{\beta}} \rho u_{\alpha} u_{\beta}(t, \mathbf{x}) + \frac{\partial}{\partial x_{\alpha}} c_s^2 \rho(t, \mathbf{x}) = 0$$



Chapman-Enskog expansion (dimensionless):

Knudsen number:

$$\varepsilon = \frac{c_r \tau}{L_r} \ll 1$$

$$f = \sum_{k=0}^{\infty} \varepsilon^k f^{(k)}$$

Boltzmann equation:

$$\begin{aligned} \frac{\partial}{\partial t} (f^{(0)} + \varepsilon f^{(1)}) + \mathbf{v} \bullet \nabla (f^{(0)} + \varepsilon f^{(1)}) = \\ - \frac{1}{\varepsilon} (f^{(0)} + \varepsilon f^{(1)} - f^{(eq)}) \end{aligned}$$



sorting the equations order by order:

order

equation

$1 / \varepsilon$

$$f^{(0)} = f^{(eq)}$$

1

$$\frac{\partial}{\partial t} f^{(0)} + \mathbf{v} \bullet \nabla f^{(0)} = f^{(1)}$$

$\varepsilon$

$$\frac{\partial}{\partial t} f^{(1)} + \mathbf{v} \bullet \nabla f^{(1)} = f^{(2)}$$





estimation of  $f^{(1)}$  (dimensional):

$$f^{(1)} = -\tau \left( \frac{\partial}{\partial t} f^{(0)} + \mathbf{v} \bullet \nabla f^{(0)} \right) =$$
$$-\tau \left( \frac{\partial f^{(0)}}{\partial \rho} \frac{\partial \rho}{\partial t} + \frac{\partial f^{(0)}}{\partial u} \frac{\partial u}{\partial t} + \mathbf{v} \bullet \nabla f^{(0)} \right)$$

$$\frac{\partial \rho}{\partial t} \longrightarrow \text{continuity-equation}$$

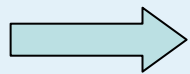
$$\frac{\partial u}{\partial t} \longrightarrow \text{Euler-equation}$$



$$P_{\alpha\beta} = P_{\alpha\beta}^{(0)} + P_{\alpha\beta}^{(1)} =$$

$$c_s^2 \rho + \int_{-\infty}^{+\infty} (v_\alpha - u_\alpha)(v_\beta - u_\beta) f^{(1)}(t, \mathbf{v}, \mathbf{x}) d\mathbf{v} =$$

$$c_s^2 \rho - c_s^2 \rho \tau \left( \frac{\partial u_\alpha}{\partial x_\beta} + \frac{\partial u_\beta}{\partial x_\alpha} \right)$$



Navier-Stokes equation

$$\frac{\partial}{\partial t} \rho u_\alpha + \frac{\partial}{\partial x_\beta} \rho u_\alpha u_\beta + \frac{\partial}{\partial x_\beta} (c_s^2 \rho \delta_{\alpha\beta} - \mu \left( \frac{\partial u_\alpha}{\partial x_\beta} + \frac{\partial u_\beta}{\partial x_\alpha} \right)) = 0$$

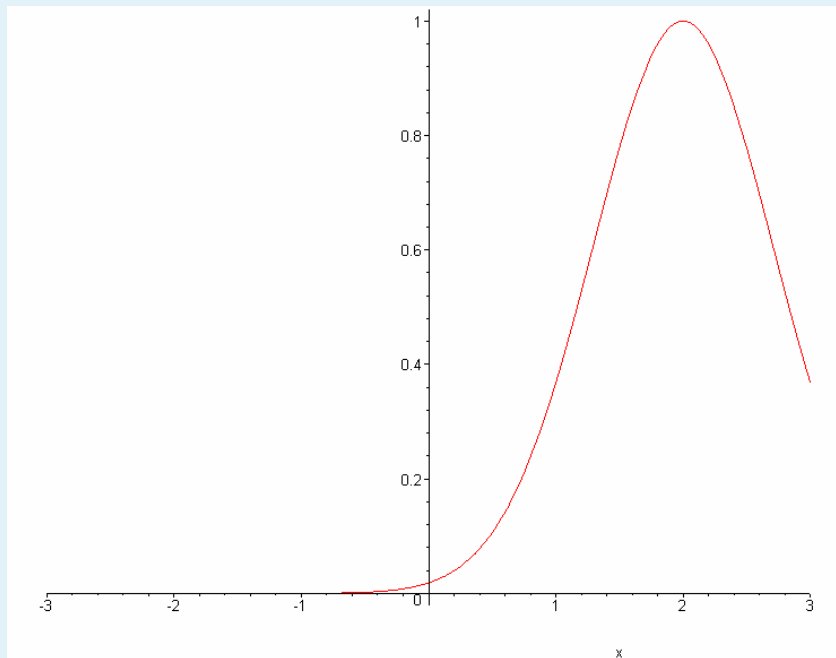
viscosity:

$$\mu = c_s^2 \rho \tau$$

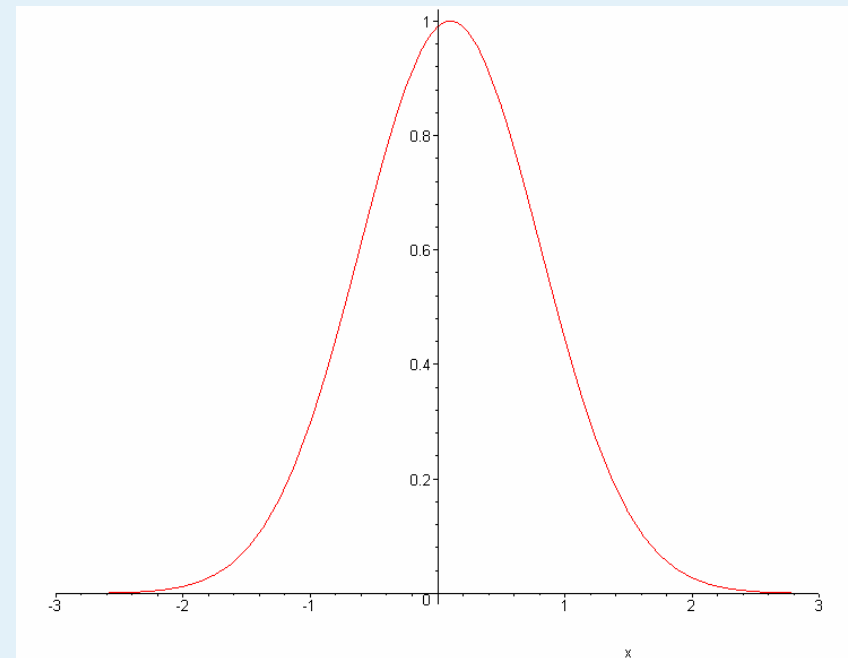


## The discrete Boltzmann equation

small Knudsen+  
large Mach number



small Knudsen+  
small Mach number





small Knudsen+  
large Ma

Expansion about local eq.



Galerkin Method



Grad's 13 Moment-System



Elimination of small time scale effects



Navier-Stokes equation

small Knudsen+  
small Mach

Expansion about global eq.



Collocation



Discrete Boltzmann equation



Ansatz (in 2D):

$$f^{abs}(t, \mathbf{v}) = \frac{\rho}{(2\pi c_s^2)^{D/2}} \exp\left(-\frac{v_1^2 + v_2^2}{2c_s^2}\right)$$

$$f(t, \mathbf{v}, \mathbf{x}) = f^{abs}(t, \mathbf{v}) \sum_{k=0}^8 a_k(t, \mathbf{x}) \theta_k(\mathbf{v})$$

Hermite-Polynomials:

$$\int_{-\infty}^{+\infty} f^{abs} \theta_k \theta_l d\mathbf{v} = \begin{cases} 0, & \text{if } k \neq l \\ A_k, & \text{if } k = l \end{cases}$$
$$H_0(x) = 1$$
$$H_1(x) = 2x$$
$$H_2(x) = 4x^2 - 2$$



$$\theta_0 = 1$$

$$\theta_1 = H_1(v_1)$$

$$\theta_2 = H_1(v_2)$$

$$\theta_3 = H_2(v_1)$$

$$\theta_4 = H_2(v_2)$$

$$\theta_5 = H_1(v_1)H_1(v_2)$$

$$\theta_6 = H_1(v_1) \cdot (H_2(v_1) + H_2(v_2))$$

$$\theta_7 = H_1(v_2) \cdot (H_2(v_1) + H_2(v_2))$$

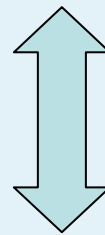
$$\theta_8 = (H_2(v_1) + H_2(v_2))^2$$

|       |                      |
|-------|----------------------|
| $a_0$ | density              |
| $a_1$ | momentum in x        |
| $a_2$ | momentum in y        |
| $a_3$ | ~pressure tensor xx  |
| $a_4$ | ~pressure tensor yy  |
| $a_5$ | ~pressure tensor xy  |
| $a_6$ | ~heat flux in x      |
| $a_7$ | ~heat flux in y      |
| $a_8$ | ~higher order moment |

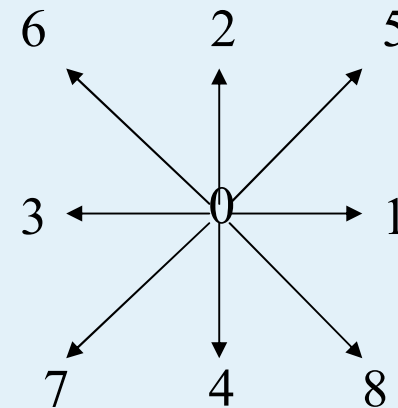


## Hermite polynomial coefficients (representation in moment space)

linear transformation



discrete  $f_i$  at collocation points (D2Q9)  
(representation in distribution space)





caveat:

equilibrium distribution  $f^{eq}$  must be projected into the space spanned by the Hermite-Polynomials (orthogonal projection):

$$\tilde{f}^{eq}(t, \mathbf{x}, \mathbf{v}) = f^{abs}(t, \mathbf{v}) \sum_{k=0}^{k=8} \tilde{a}_k(t, \mathbf{x}) \theta_k(\mathbf{v})$$

$$\tilde{a}_k(\rho, \mathbf{u}) = \int_{-\infty}^{+\infty} f^{abs} f^{eq} \theta_k d\mathbf{v} / \int_{-\infty}^{+\infty} f^{abs} \theta_k \theta_k d\mathbf{v}$$

Quadrature: evaluation of equilibrium distr. at collocation points  $\mathbf{v}_i$

$$\tilde{f}^{eq}(\rho, \mathbf{u}, \mathbf{v}_i) = \tilde{f}_i^{eq}(\rho, \mathbf{u}) = w_i \rho \left( 1 + \frac{3}{2} \mathbf{v}_i \cdot \mathbf{u} + \frac{9}{2} (\mathbf{v}_i \cdot \mathbf{u})^2 - \frac{3}{2} \mathbf{u}^2 \right) \quad i = 0, \dots, m$$





As a result we obtain the discrete Boltzmann equation:

$$\frac{\partial f_i(t, \mathbf{x})}{\partial t} + \mathbf{v}_i \cdot \nabla f_i(t, \mathbf{x}) = -\frac{1}{\tau} \left( f_i(t, \mathbf{x}) - \tilde{f}_i^{eq}(t, \mathbf{x}) \right) \quad i = 0, \dots, 8$$

macroscopic moments can now be obtained as sums

|                    |                                                                                                           |
|--------------------|-----------------------------------------------------------------------------------------------------------|
| density            | $\rho = \sum_{i=0}^m f_i$                                                                                 |
| momentum           | $\rho \mathbf{u} = \sum_{i=0}^m \mathbf{v}_i f_i$                                                         |
| pressure<br>tensor | $P_{\alpha\beta} = \sum_{i=0}^m (\mathbf{v}_{i\alpha} - u_{\alpha})(\mathbf{v}_{i\beta} - u_{\beta}) f_i$ |
| strain tensor      | $S_{\alpha\beta} \propto \sum_i \mathbf{v}_{i\alpha} \mathbf{v}_{i\beta} f_i^{(neq)}$                     |



## From the discrete BE to LBGK:

### Finite Difference discretization

$$\frac{f_i(\vec{x}, t + \Delta t) - f_i(\vec{x}, t)}{\Delta t} + c \frac{f_i(\vec{x} + \vec{e}_i \Delta t, t + \Delta t) - f_i(\vec{x}, t + \Delta t)}{\Delta x} = -\frac{1}{\tau} (f_i(\vec{x}, t) - f_i^{eq}(\vec{x}, t))$$



$$\Delta t = c \Delta x$$



$$f_i(\vec{x} + \vec{e}_i \Delta t, t + \Delta t) - f_i(\vec{x}, t + \Delta t) = -\frac{\Delta t}{\tau} (f_i(\vec{x}, t) - f_i^{eq}(\vec{x}, t))$$

Taylor expansion + Chapman-Enskog analysis:

viscosity:

$$\mu = c_s^2 \rho \left( \tau - \frac{\Delta t}{2} \right)$$



## Multi-Relaxation-time approach

Linear transformation:

$$\vec{m} = \mathbf{M} \vec{f}$$

$$\vec{m} = [\rho, e, \varepsilon, j_x, q_x, j_y, q_y, p_{xx}, p_{xy}]$$

$$\vec{m}^{eq} = [0, e^{eq}, \varepsilon^{eq}, 0, q_x^{eq}, 0, q_y^{eq}, p_{xx}^{eq}, p_{xy}^{eq}]$$

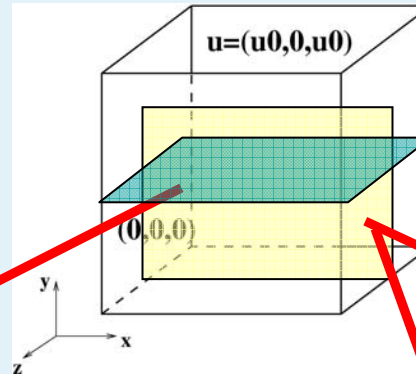
collision in moment space:

$$\tilde{\Omega}_i = s_i (m_i - m_i^{eq}) \quad i \in \{0, \dots, m\}$$

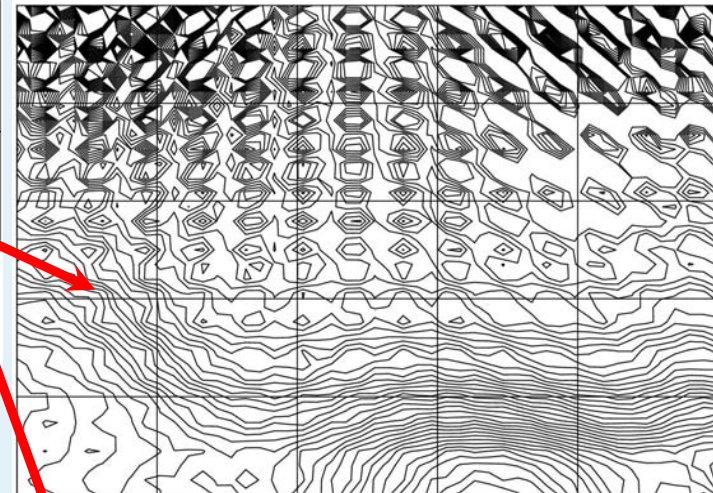
$$\tilde{f} = \mathbf{M}^{-1} \tilde{\Omega}_i$$

D. d'Humières, I. Ginzburg,  
M. Krafczyk, P. Lallemand,  
L. Luo (2002)

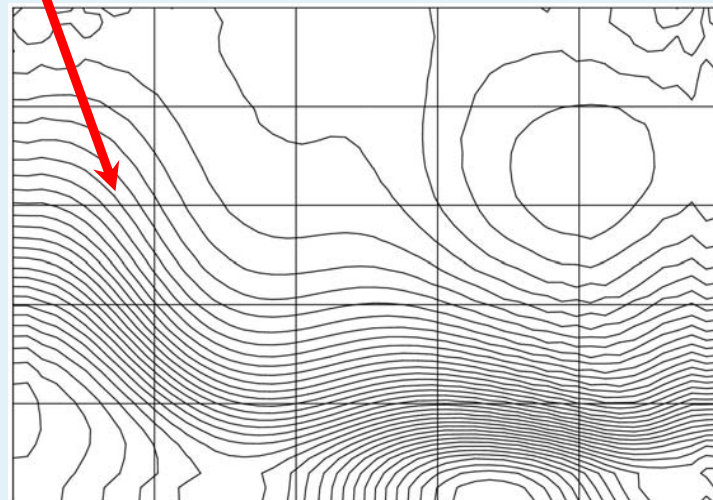
Re=2000  
(52<sup>3</sup> nodes)



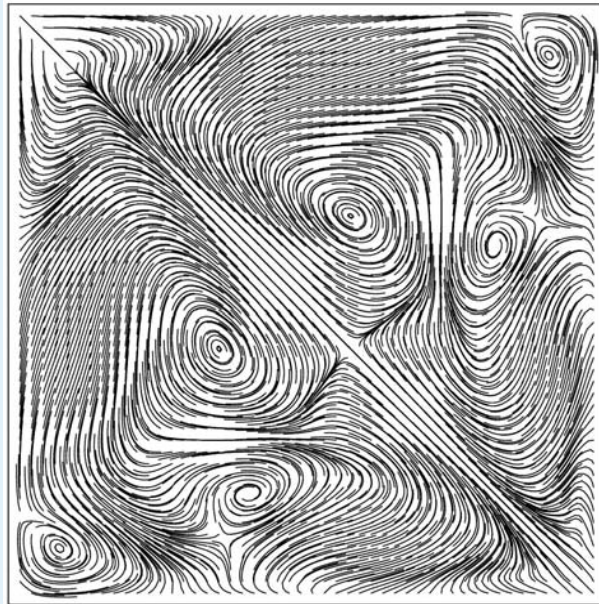
LBGK



GLBE



efficiency gain  
up to ~ 1:100





choose free parameter  $s_i$  to maximize Galilean invariance, stability and isotropy (dispersion):

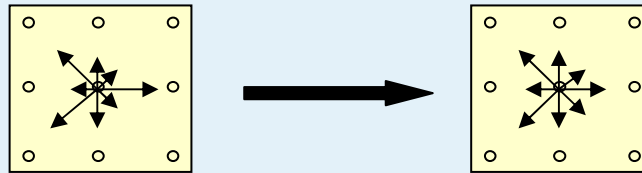
| <i>Method</i>                                      | <i>Max. Cell-Reynolds-number</i> |
|----------------------------------------------------|----------------------------------|
| Navier-Stokes Expl. Euler and centered Differences | 2                                |
| LBGK                                               | ~ 30                             |
| MRT                                                | ~ 200                            |

## flow field simulation with Lattice Boltzmann

$$LBE \quad f_{i,l}(t + \Delta t_l, \vec{x} + \vec{e}_i \Delta t_l) = f_{i,l}(t, \vec{x}) + \Omega_{i,l}(t, \vec{x})$$

$$\rho = \sum_i f_i \quad \rho \vec{u} = \sum_i \vec{e}_i f_i$$

collision:

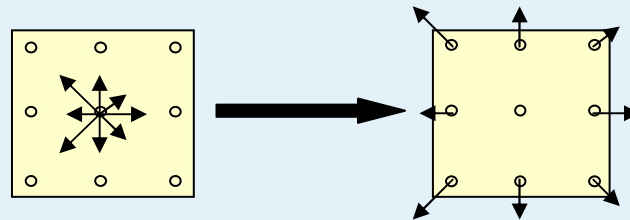


$$\tilde{f}_i(t, \vec{x}) = f_i(t, \vec{x}) + \Omega_{i,l}(t, \vec{x})$$

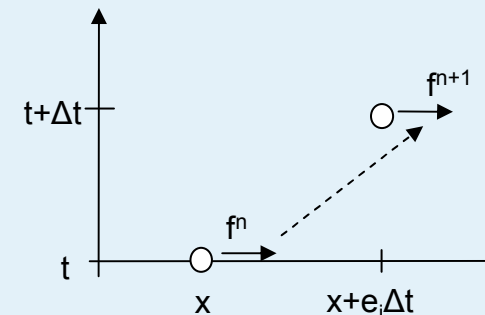
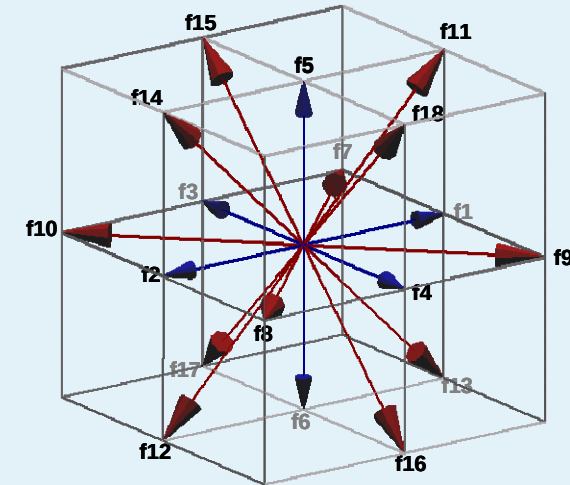
• *STR*:  $\Omega_{i,l}(t, \vec{x}) = -\frac{\Delta t_l}{\tau_l} \left( f_i(t, \vec{x}) - f_i^{eq}(t, \vec{x}) \right), \quad \tau_l = 3\frac{\nu}{c^2} + \frac{1}{2}\Delta t_l$   
(Quian, 1992)

• *MRT*:  $\Omega_{i,l}(t, \vec{x}) = M^{-1} S_l \left[ \underbrace{(M f(t, \vec{x}))}_m - m^{eq,l}(t, \vec{x}) \right]$   
(d'Humières, 1992)

propagation:



$$f_{i,l}(t + \Delta t_l, \vec{x} + \vec{e}_i \Delta t_l) = \tilde{f}_{i,l}(t, \vec{x})$$







# **Single phase LB: Boundary & Initial Conditions, Force evaluation and Fluid-Structure Interaction**

**Manfred Krafczyk**

**contributors:**

**B. Ahrenholz, S. Freudiger, S. Geller, B. Nachtwey, M. Stiebler, J. Tölke**

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**<http://www.cab.bau.tu-bs.de>**



## Overview

- **No-slip BC: from bounce back to Multi-Reflection**
- **Initialization: a semi-Poisson LB-solver**
- **Force evaluation**
- **FSI**





## Sources of accuracy degradation due to boundary conditions

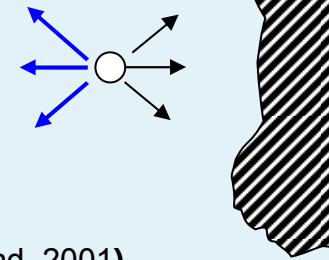
The LB bulk scheme (fluid nodes) can be shown to be second order accurate in space. Boundary conditions potentially decrease the order of convergence. Two different effects have to be distinguished:

- geometric approximation of curved boundaries by a Cartesian voxel grid  
-> consideration of subgrid distances between lattice links and surfaces
- kinetic boundary layer (error terms) produce a shift of the effective boundary location.  
This problem cannot be cured for BGK models !  
(see the work of I. Ginzburg and D. d'Humieres)

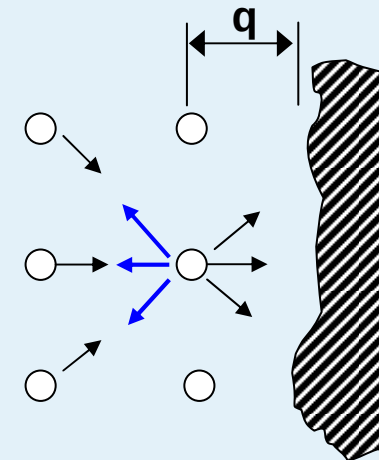
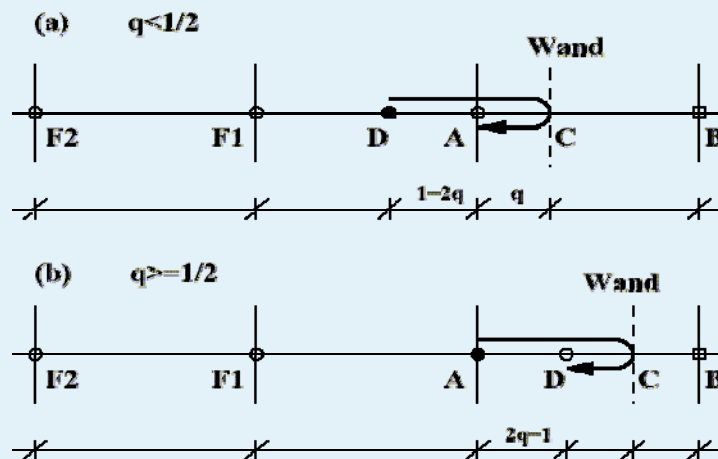
## Boundary Conditions (no slip)

- Simple Bounce-Back

$$f_{inversDirection}(x, t + \Delta t) = \tilde{f}_{Direction}(x, t)$$



- Second Order Bounce-Back (Bouzidi, Firdaouss, Lallemand, 2001)



- Multi-Reflection BCs (Ginzburg, d'Humières, 2003)



## Dirichlet Boundary Conditions

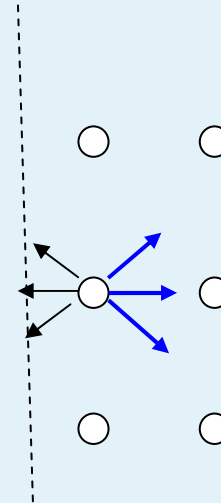
**Velocity boundary (first order):**

$$f_i^{t+1} = f_{invers} + \frac{2}{c_s^2} \rho w_i \vec{e}_i * \vec{u}_0 \quad (\text{Ladd, 92})$$

**pressure has to evolve**

**Pressure/Density boundary:**

$$f^{t+1} = -f_{invers} + f_{invers}^{eq}(P_o, \vec{u}) + f^{eq}(P_o, \vec{u})$$



**simple outflow:**

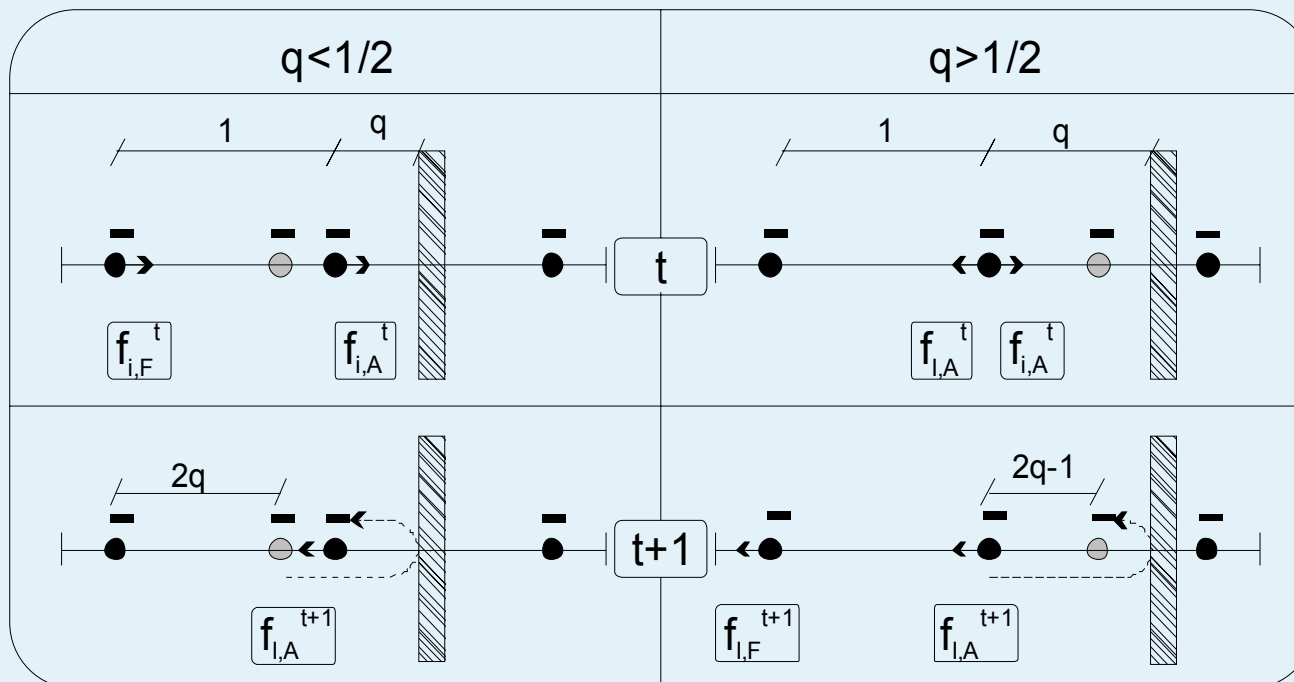
**equ. distributions from computed velocity and desired pressure (~zero gradient)**



## Velocity boundary (second order): (Bouzidi, Firdaouss, Lallemand, 2001)

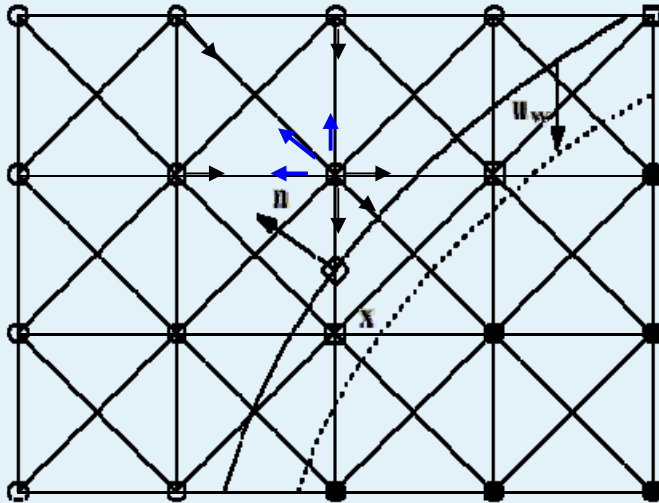
$$f_{IA}^{t+1} = (1-2q) \cdot f_{iF}^t + 2q \cdot f_{iA}^t - 6 \frac{\mathbf{e}_i \mathbf{u}_w}{c^2}, \quad 0.0 < q < 0.5$$

$$f_{IA}^{t+1} = \frac{2q-1}{2q} \cdot f_{IA}^t + \frac{1}{2q} \cdot f_{iA}^t - 3 \frac{\mathbf{e}_i \mathbf{u}_w}{qc^2}, \quad 0.5 \leq q \leq 1.0$$





## Moving Boundaries



- initialization of new fluid nodes  
→ local Poisson type iteration

**Problem:** Given an initial velocity field, determine a consistent pressure field and consistent non-equilibrium distributions.

**Idea:** Iterate the collision and propagation cycle starting from  $u_0$  and  $p_0$ , but let the pressure evolve and keep the velocity field fixed to the initial value until convergence.

The use of BGK may (for small viscosities) result in large iteration numbers.

As usual, one can speed up convergence using the MRT version. (R. Mei, L. Luo, P. Lallemand, D. d'Humieres, 2006)

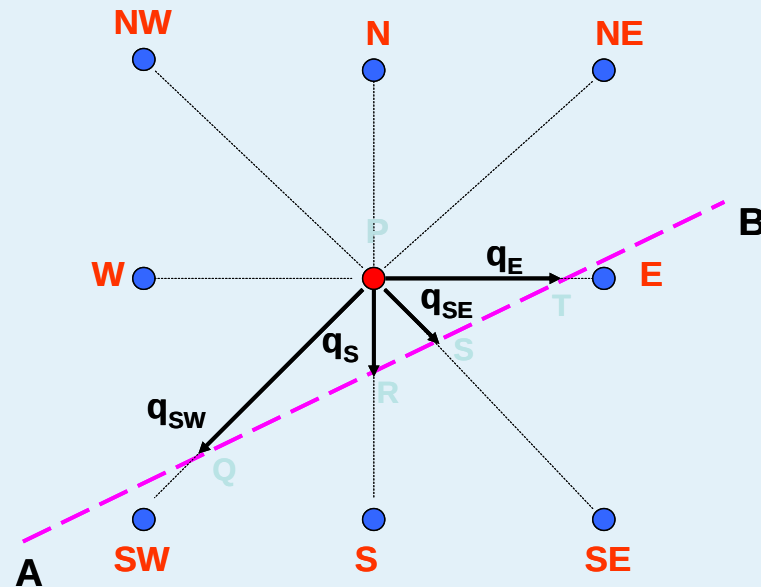
After convergence, the resulting pressure field can be shown to obey the Poisson equation and the resulting non-equilibrium distribution will be consistent in terms of higher order moments (e.g. stresses).



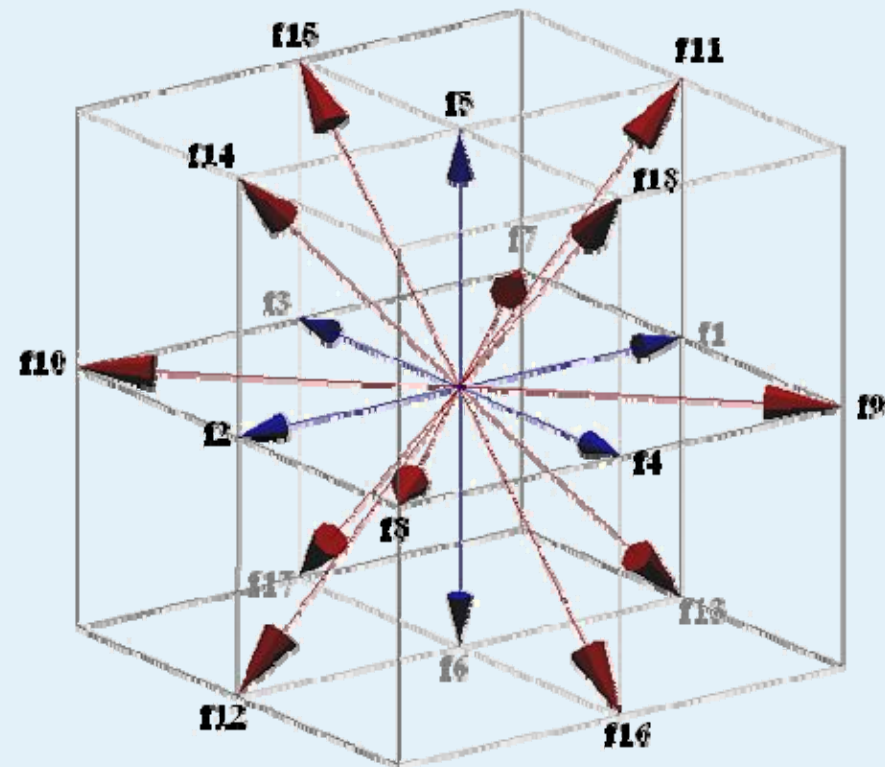
## Grid generation

## Calculation of subgrid distances q's

## D2Q9-Model

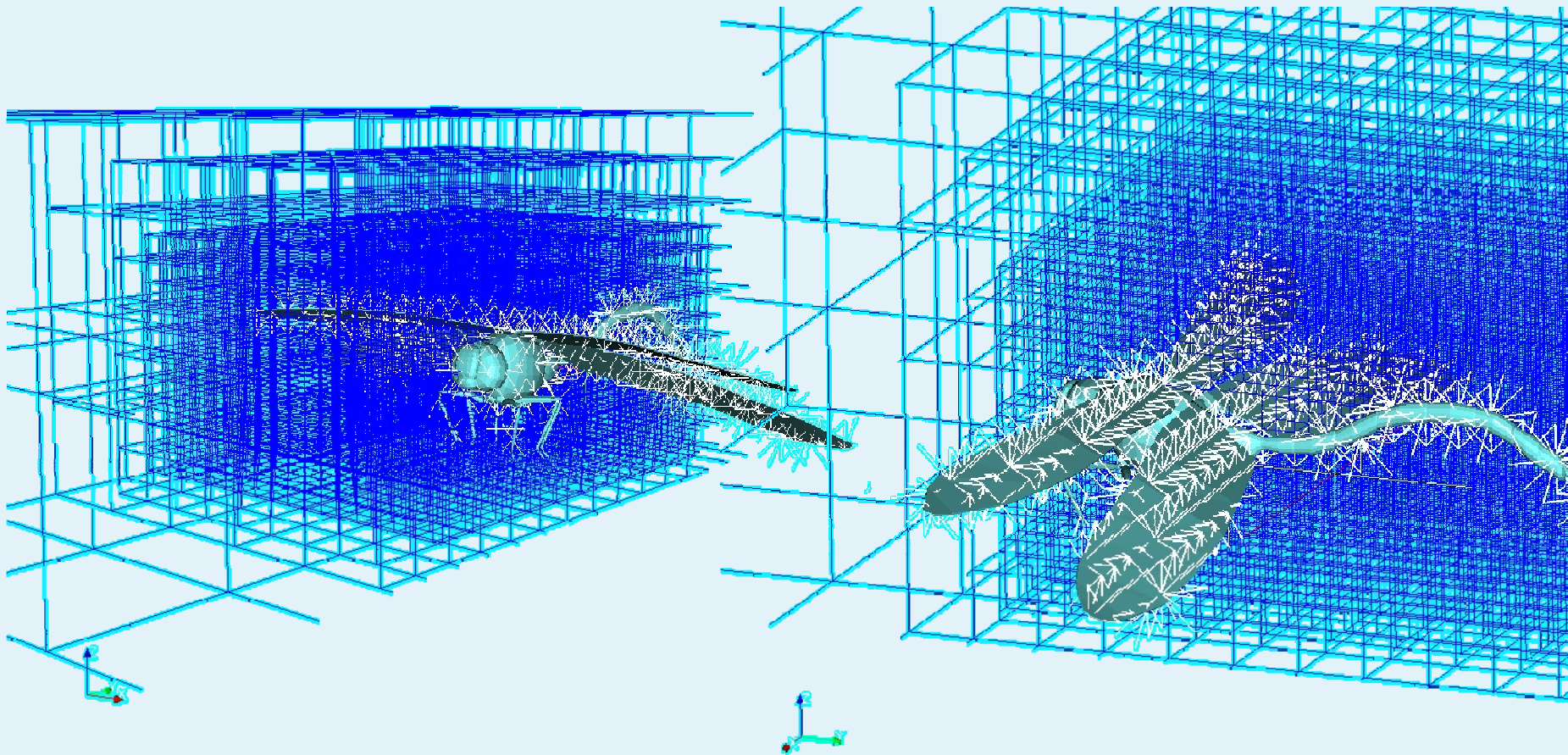


## D3Q19-Model





## 3D grid generation

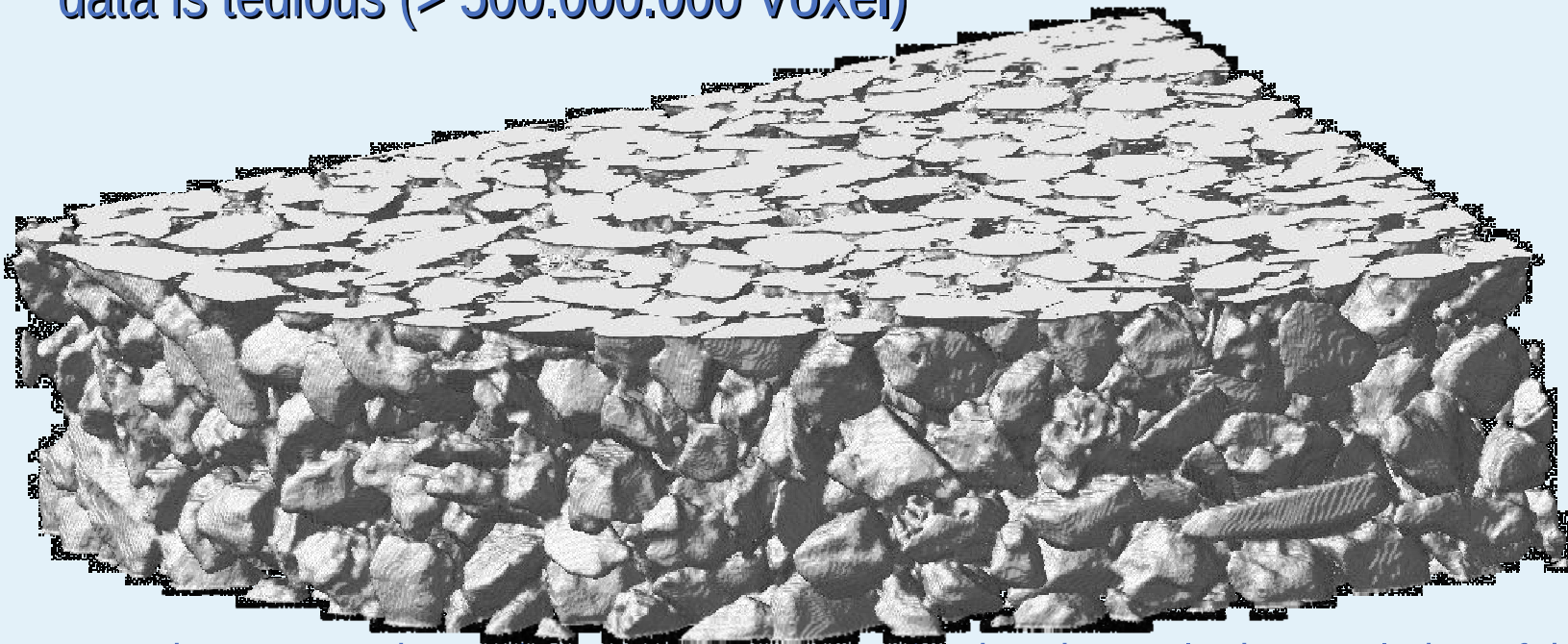






Preprocessing of subgrid links for high resolution porous media tomographic data is tedious (> 500.000.000 Voxel)

(tomographic data courtesy of  
A. Kästner, P. Lehmann, ETH Zürich)



For such systems, the surface can be parametrized to decouple the resolution of the tomography data from the resolution of the numerical grid

(Ahrenholz, Tölke, Krafczyk, preprint)

Applications: soil physics, particle filters, fuel cells etc.





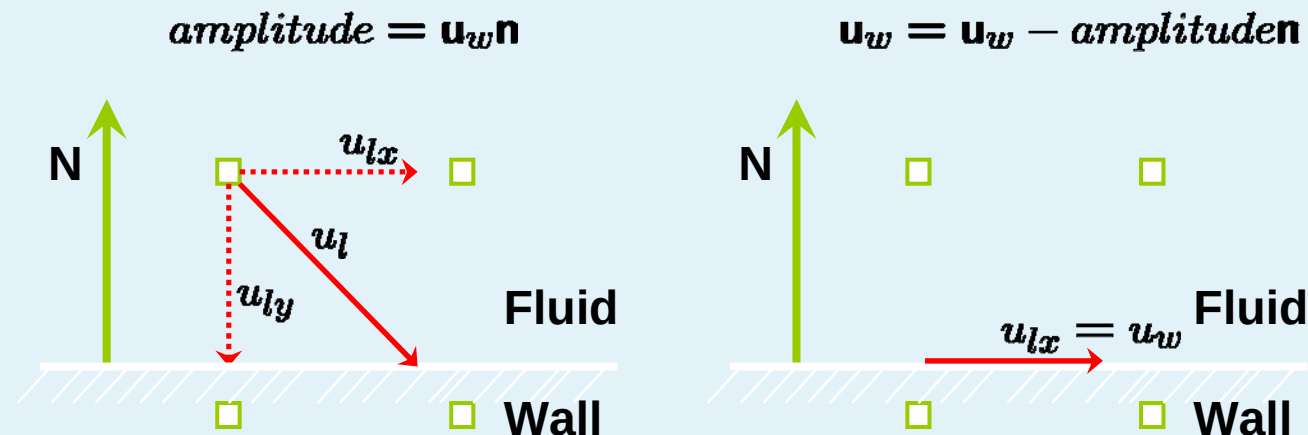
## Second-order accurate slip boundary conditions

- Velocity boundary conditions

$$f_{IA}^{t+1} = (1-2q) \cdot f_{iF}^t + 2q \cdot f_{iA}^t - 6 \frac{\mathbf{e}_i \mathbf{u}_w}{c^2}, \quad 0.0 < q < 0.5$$

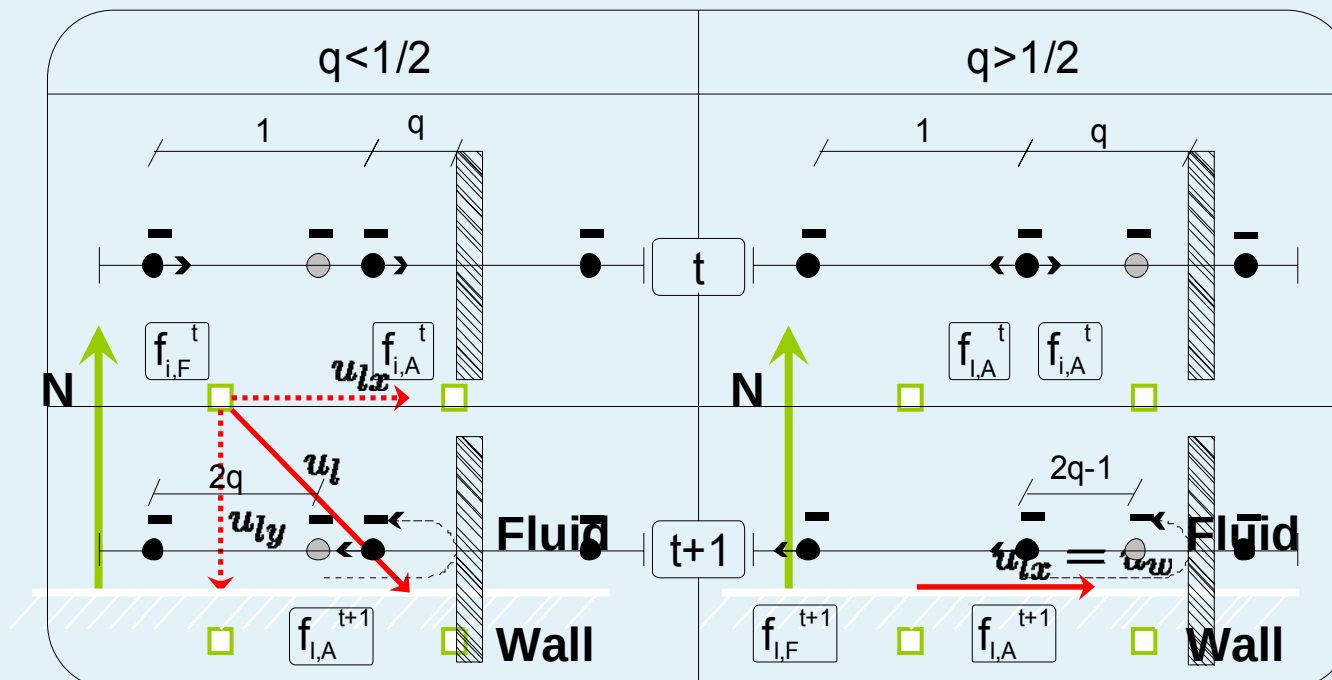
$$f_{IA}^{t+1} = \frac{2q-1}{2q} \cdot f_{IA}^t + \frac{1}{2q} \cdot f_{iA}^t - 3 \frac{\mathbf{e}_i \mathbf{u}_w}{qc^2}, \quad 0.5 \leq q \leq 1.0$$

- Calculation of the velocity component
  - Calculate the amplitude from local velocity and the wall normal
  - Calculate the velocity at the wall using the normal, the local velocity and the amplitude



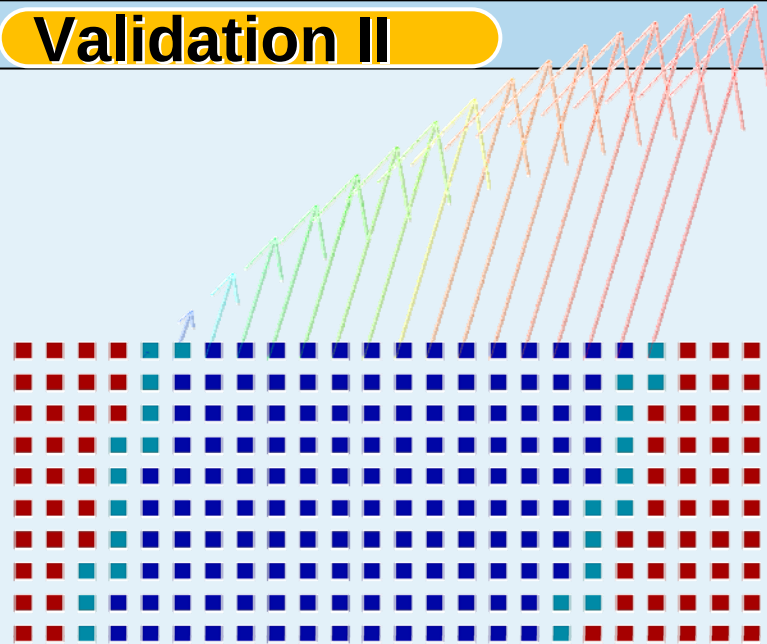


- works for arbitrary geometries  
(in contrary to specular reflection)
- only prerequisite is the local normal vector of the wall and the subgrid distances.

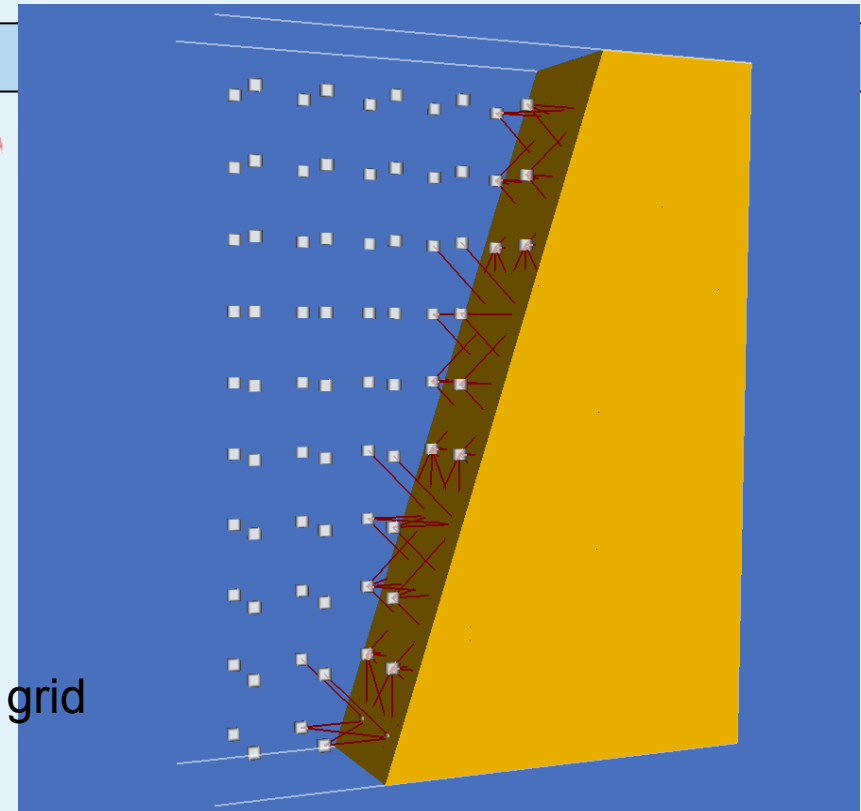




## Validation II



Velocity profile and discretized node grid



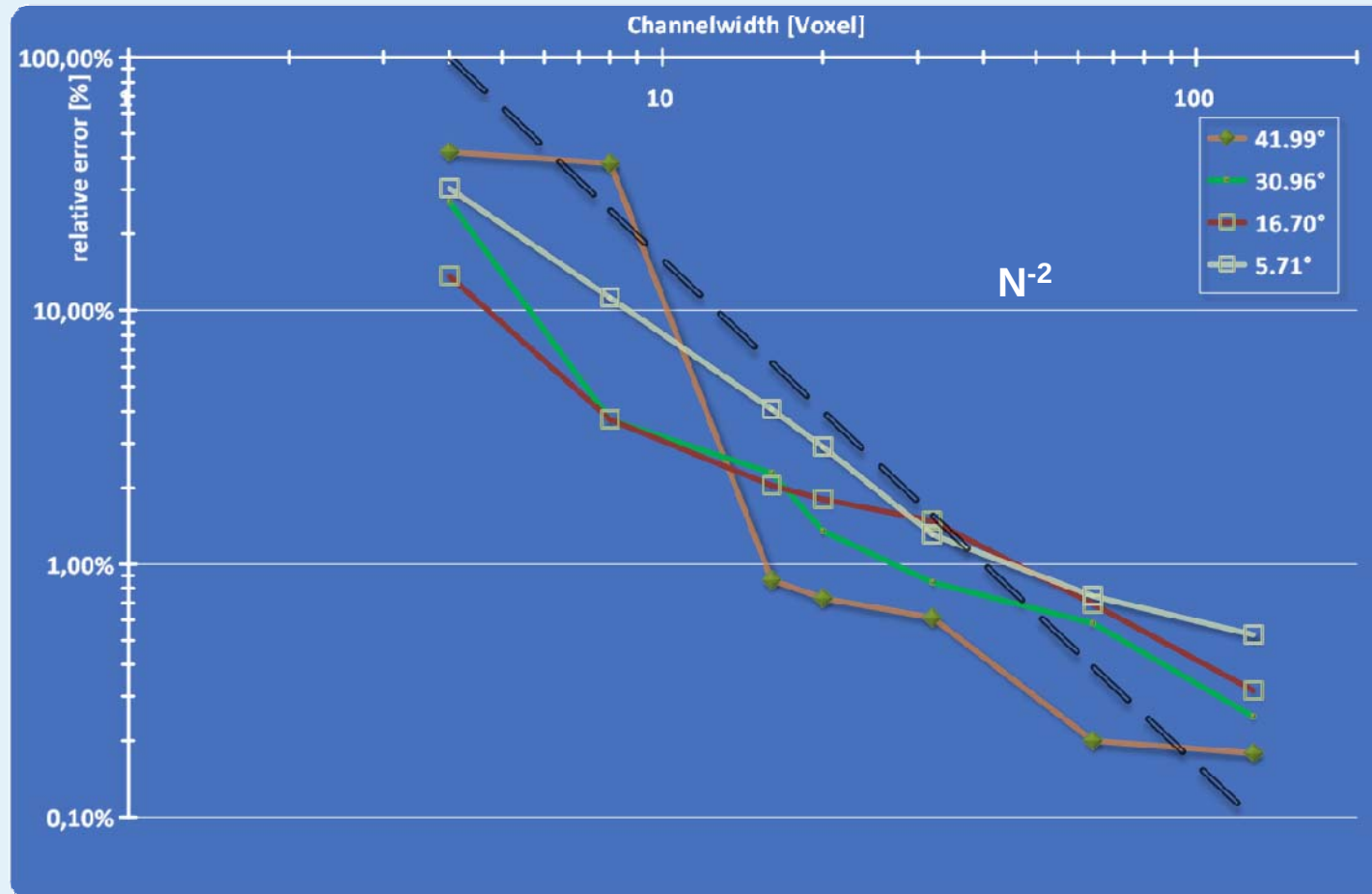
Node grid with q-links to the wall

- Results:
  - order of accuracy for simple bounce back for grid aligned walls is  $N^{-2}$
  - order of accuracy for simple bounce back for inclined walls is  $N^{-1}$
  - order of accuracy for linear interpolated bounce back for inclined walls is close to  $N^{-2}$



## Validation III

- Results:



Relative error of the 2-dimensional Poiseuille Flow  
compared to the analytical solution at different inclination angles



## Can LB be regarded as an efficient approach for CFD ?

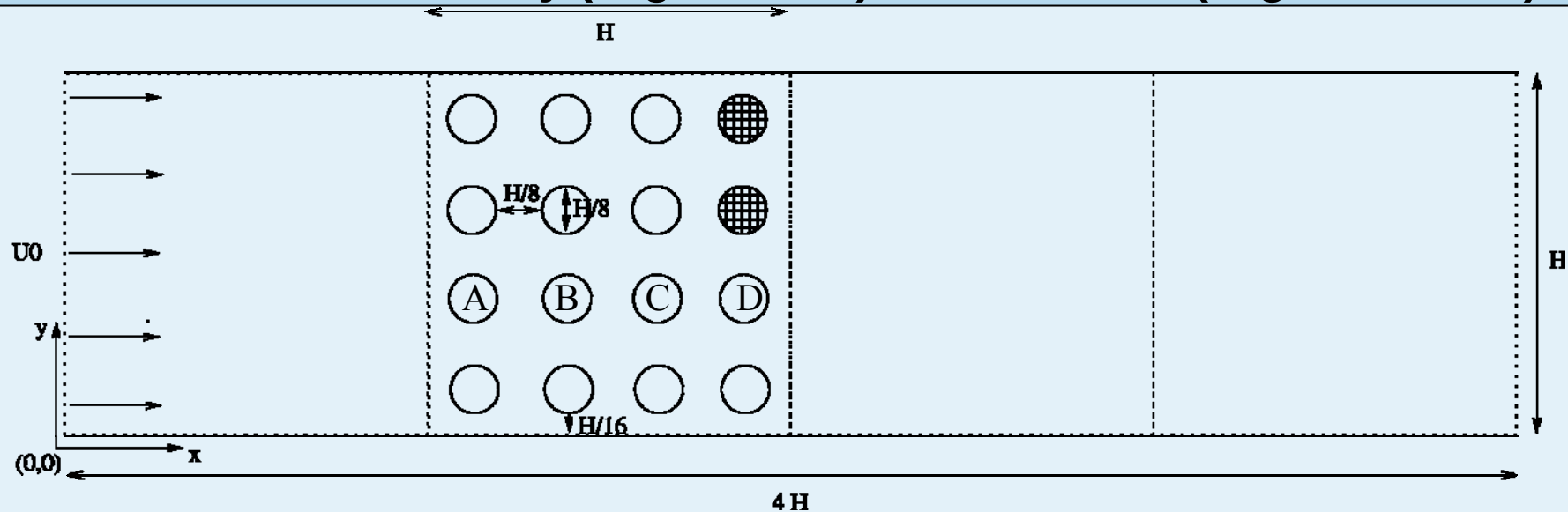
### Ingredients:

- 2nd order BCs
- MRT
- grid refinement (to be discussed)
- efficient data structures

S. Geller, M. Krafczyk, J. Tölke, S. Turek, J. Hron:  
Benchmark computations based on Lattice-Boltzmann,  
Finite Element and Finite Volume Methods for laminar Flows,  
Computers and Fluids 35, pp. 888-897 (2006)



## Benchmark stationary (Ergun $Re=1$ ) and transient (Ergun $Re=200$ )



Re 1: pressure plots for  $y=0.5/0.625H$

drag & lift coefficients for obstacle „A“

Re 200: drag & lift for obstacle „D“

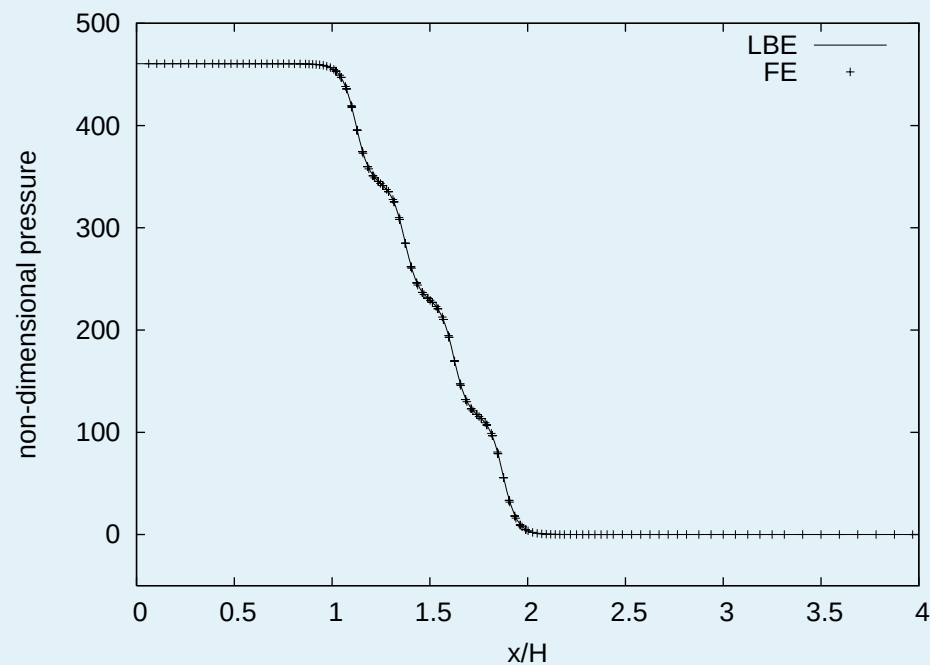
FE-solver: „Featflow“, Prof. Turek, TU Dortmund

[www.featflow.de](http://www.featflow.de)

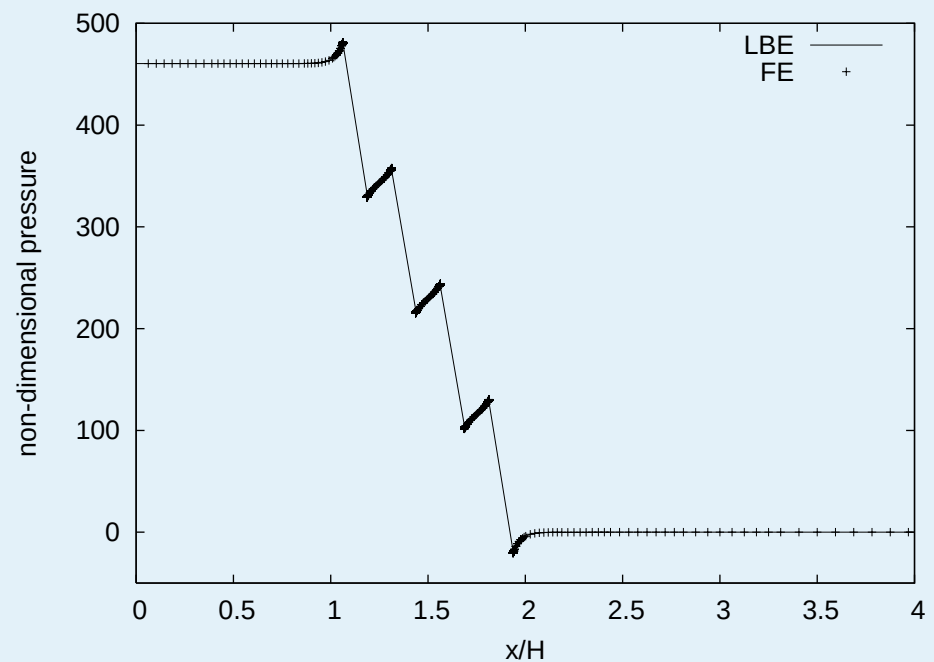


## Pressure (Ergun $Re=1$ )

$y = 0.5 H$



$y = 0.625 H$





**cylinder A,  $Re_E=1$**

**reference: drag = 465.58, lift = 0.958**

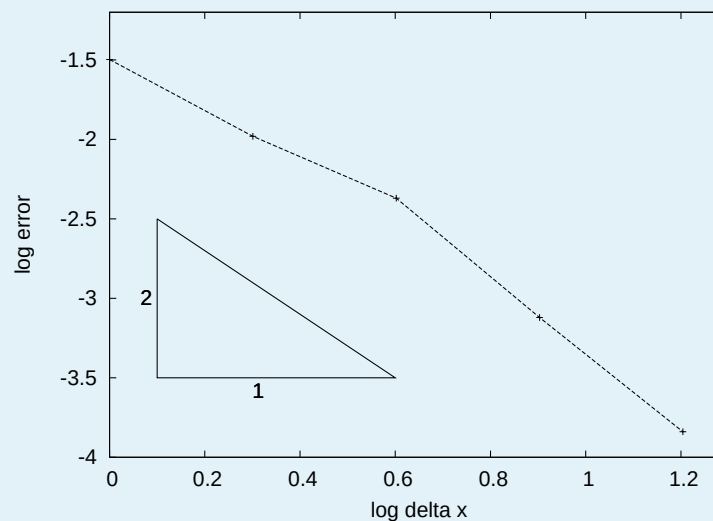
| scheme         | #dof          | rel.error [%] |             | time [s]  |
|----------------|---------------|---------------|-------------|-----------|
|                |               | drag          | lift        |           |
| LB, 4-6        | 48096         | 1.03          | 1.07        | 10        |
| <b>LB, 4-7</b> | <b>141696</b> | <b>0.43</b>   | <b>0.70</b> | <b>93</b> |
| FF, 0+2        | 11774         | 0.77          | 5.50        | 6         |
| <b>FF, 1+2</b> | <b>26922</b>  | <b>0.58</b>   | <b>1.04</b> | <b>53</b> |
| FF, 2+0        | 30642         | 1.34          | 0.19        | 33        |
| FF, 2+1        | 43314         | 0.37          | 0.10        | 38        |



convergence study: LBE,  $Re=1$ , circle A, drag

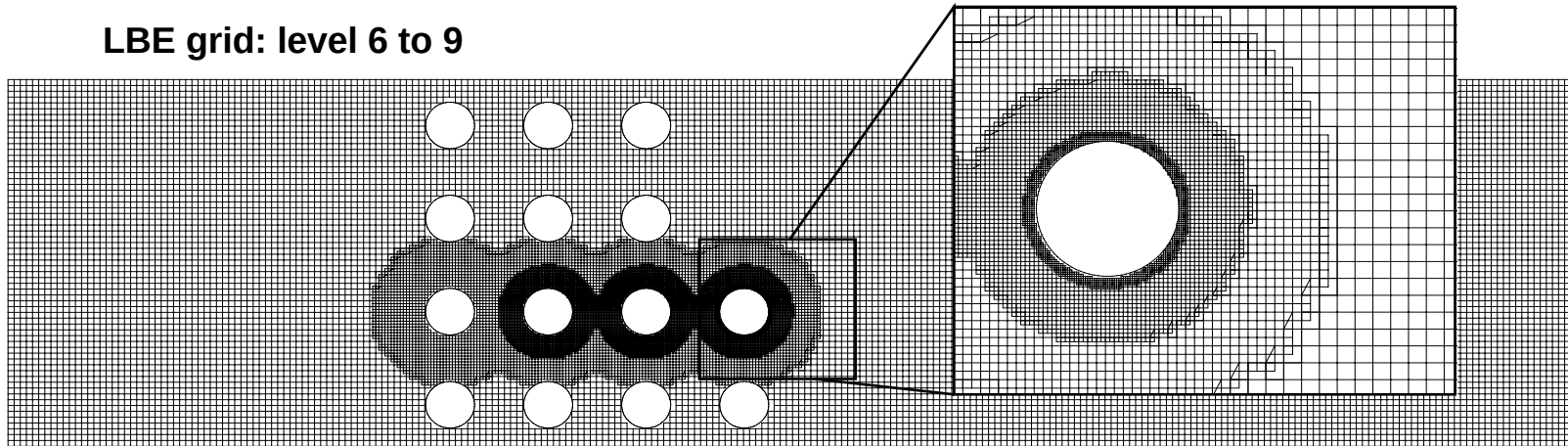
| min | max | Ma        | #DOF    | #drag       | rel. error[%] | #timesteps | time [s] |
|-----|-----|-----------|---------|-------------|---------------|------------|----------|
| 4   | 5   | 0,0173205 | 15264   | 450,7688527 | 3,183         | 3900       | 3        |
| 4   | 6   | 0,0086603 | 40320   | 470,4550817 | 1,045         | 2000       | 9        |
| 4   | 7   | 0,0043301 | 141696  | 467,5764449 | 0,427         | 2900       | 93,2     |
| 4   | 8   | 0,0021651 | 549936  | 465,9428266 | 0,076         | 4900       | 1140     |
| 4   | 9   | 0,0010825 | 2182608 | 465,6574185 | 0,014         | 7900       | 14703    |
| 9   | 9   | 0,0010825 | 8976960 | 465,5861301 | 0,000         | 152300     | 45352    |

reference value: 465,58

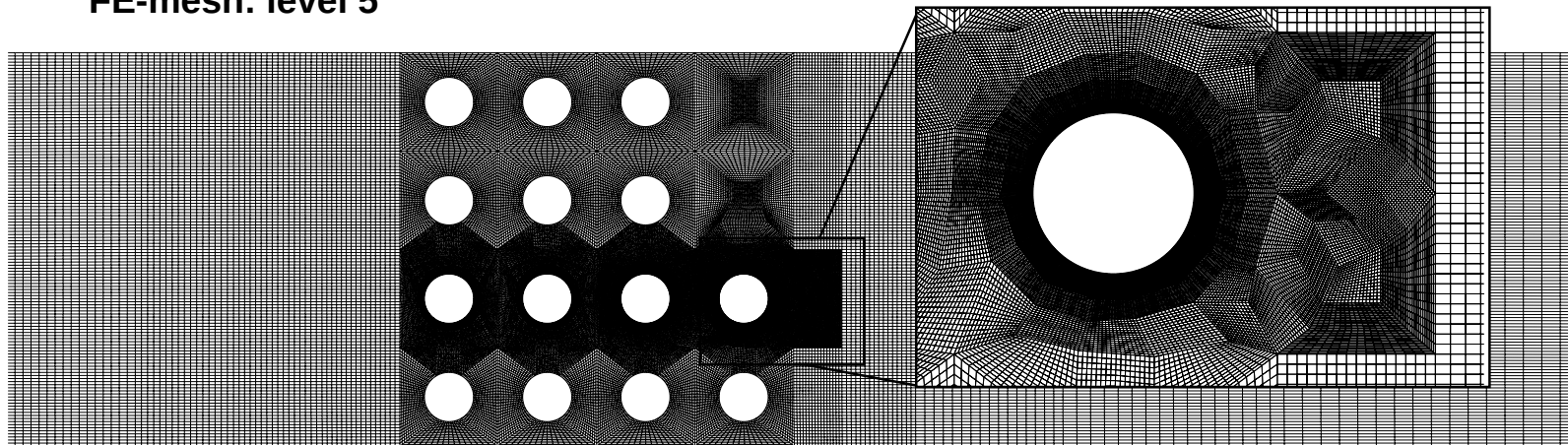




**LBE grid: level 6 to 9**



**FE-mesh: level 5**

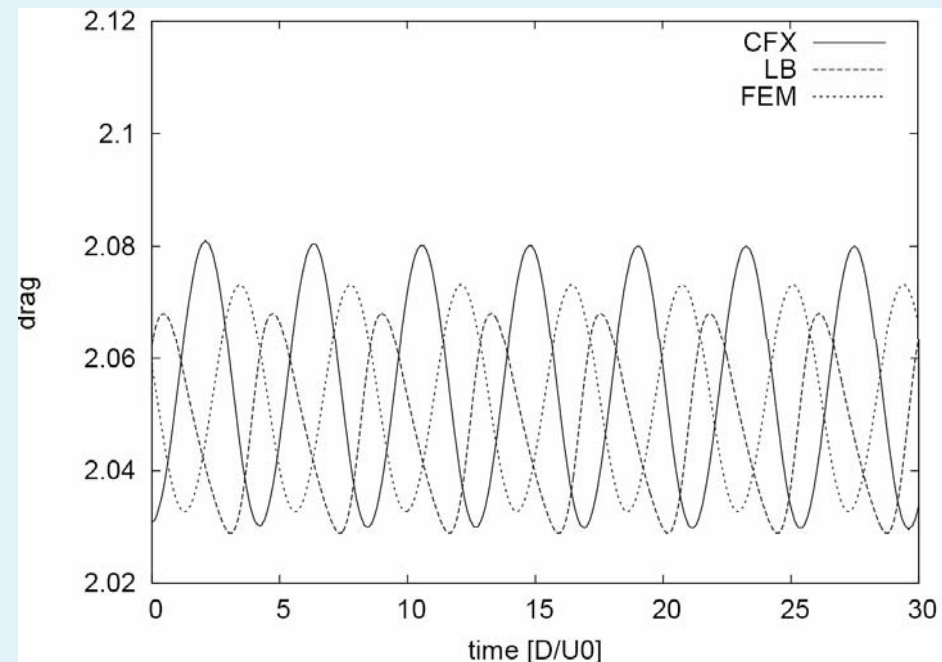


## results for the transient case (Ergun Re = 200, cylinder D):

| scheme   | #dof      | cd[%] | cl[%] | Tref [%] | CPU-time[s] / Tref |
|----------|-----------|-------|-------|----------|--------------------|
| LB (6-8) | 199.656   | 2.4   | 0.4   | 0.5      | 30                 |
| LB (6-9) | 243.774   | 0.3   | 1.6   | 0.5      | 46                 |
| FEM(4)   | 113.264   | 1.3   | 0.3   | 9.2      | 22                 |
| FEM(5)   | 450.528   | 0.1   | 1.5   | 0.1      | 265                |
| CFX      | 385.485   | 1.6   | 2.5   | 0.2      | 2856               |
| CFX      | 917.616   | 0.5   | 1.3   | 0.2      | 6594               |
| CFX      | 1.807.428 | 0     | 0     | 0        | 13440              |

Ma = 0.02

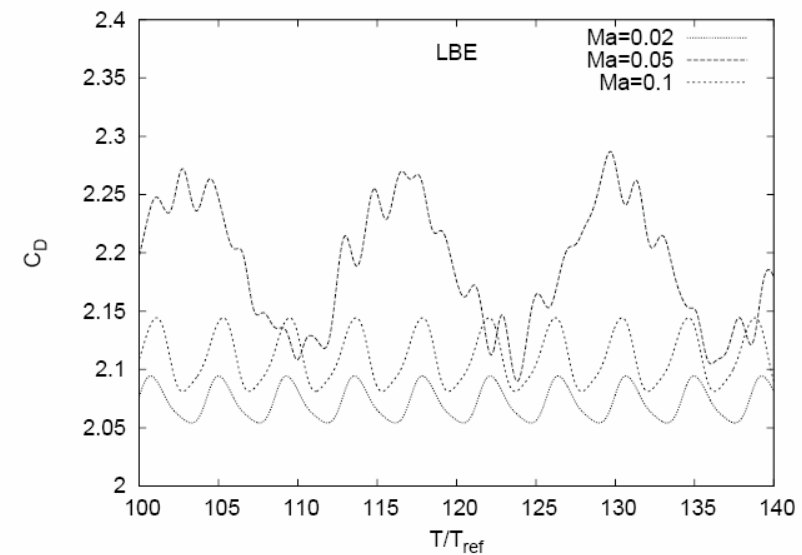
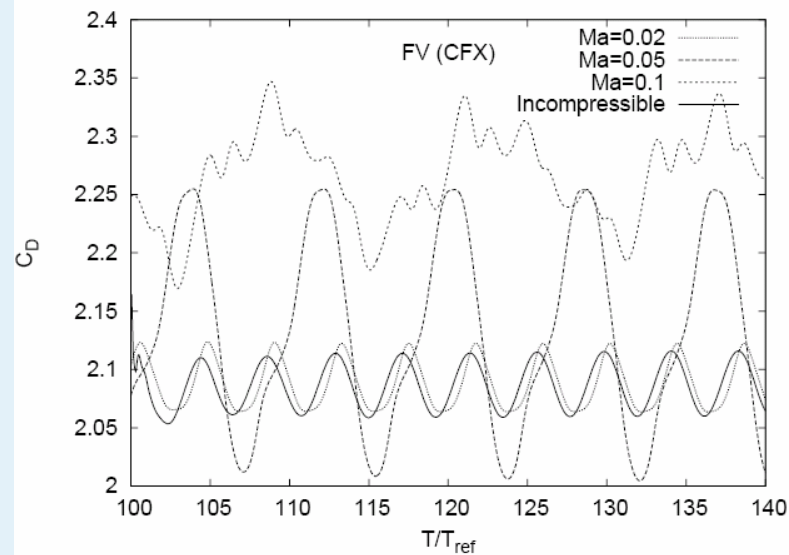
reference: cd = 2.0548  
cl = 0.9150  
Tref = 4.2327



## results for the transient case (Ergun $Re = 200$ , cylinder D):

| scheme   | #dof      | Ma   | CPU-time[s] / Tref |
|----------|-----------|------|--------------------|
| LB (6-8) | 318.123   | 0.1  | 12                 |
| LB (6-8) | 318.123   | 0.05 | 25                 |
| LB (6-8) | 318.123   | 0.02 | 61                 |
| CFX      | 385.485   | 0.1  | 2730               |
| CFX      | 385.485   | 0.05 | 2814               |
| CFX      | 385.485   | 0.02 | 2772               |
| CFX      | 1.807.428 | 0    | 2856               |

compressibility effect  
- Ma number effect

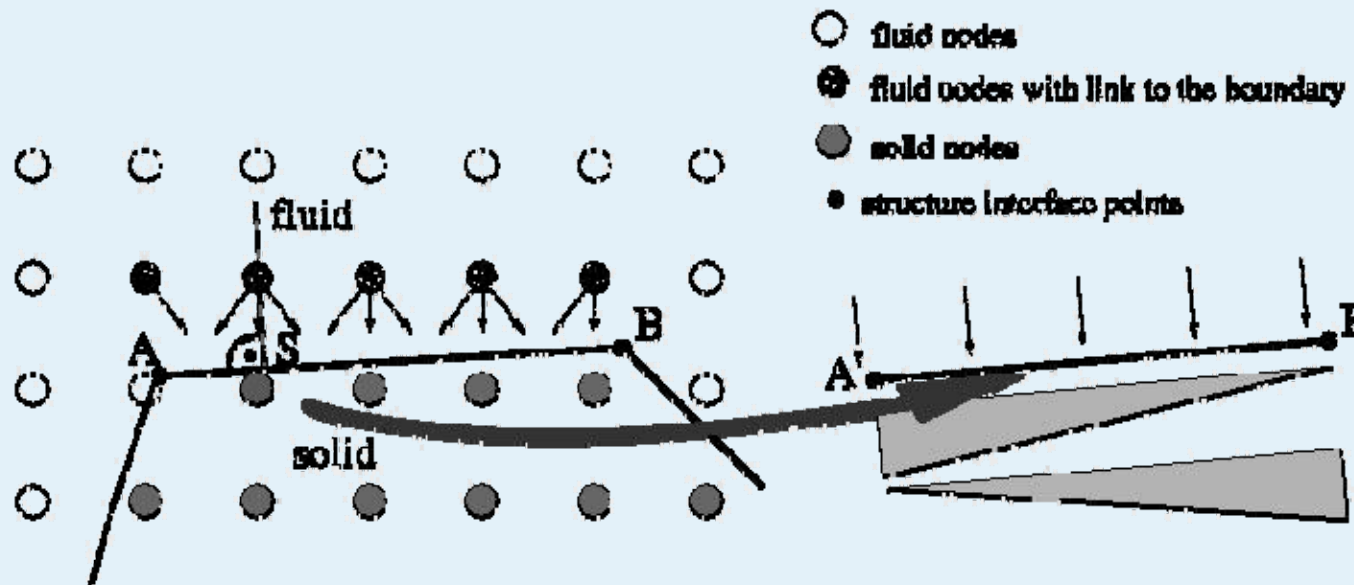


## Force evaluation

- **momentum exchange:**  
(Ladd, 1992, 2002)

$$dI = f_{inversDir}(x, t + \Delta t) + \tilde{f}_{Dir}(x, t)$$

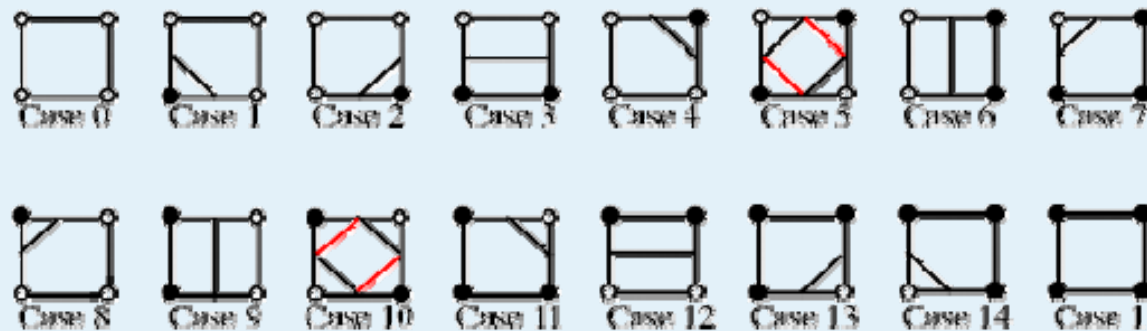
- **forces:** 
$$F_i = \sum_i e_i \cdot [f_{inversDir}(x, t + \Delta t) + \tilde{f}_{Dir}(x, t)] \cdot \frac{\Delta x^2}{\Delta t}$$



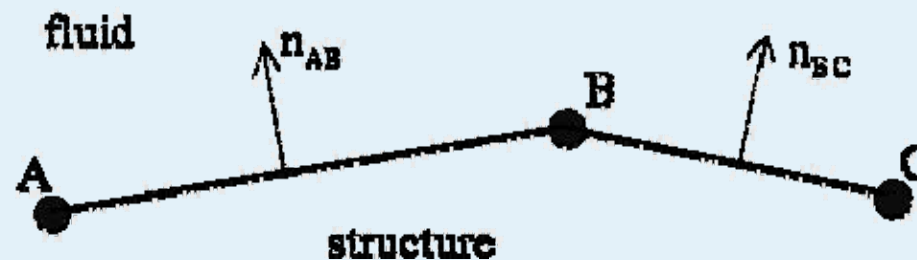


## Force evaluation

- stress integration: 
$$P_{\alpha\beta} = c_s^2 \rho \delta_{\alpha\beta} + (1 - \frac{\Delta t}{2\tau}) \sum_k f_k^{neq} e_{i\alpha} e_{i\beta}$$



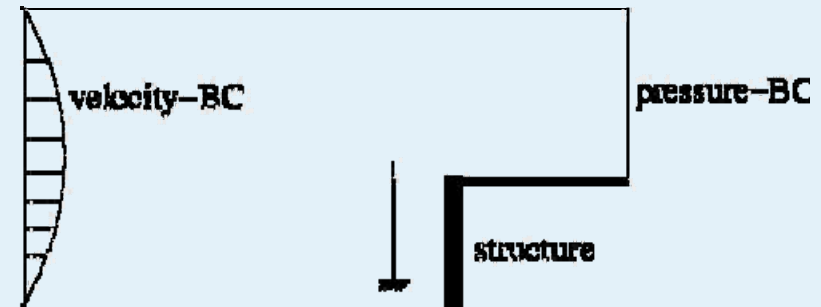
- forces: 
$$F_B = (\frac{1}{4}\sigma_A + \frac{3}{4}\sigma_B)n_{AB} \frac{1}{2}l_{AB} + (\frac{3}{4}\sigma_B + \frac{1}{4}\sigma_C)n_{BC} \frac{1}{2}l_{BC}$$



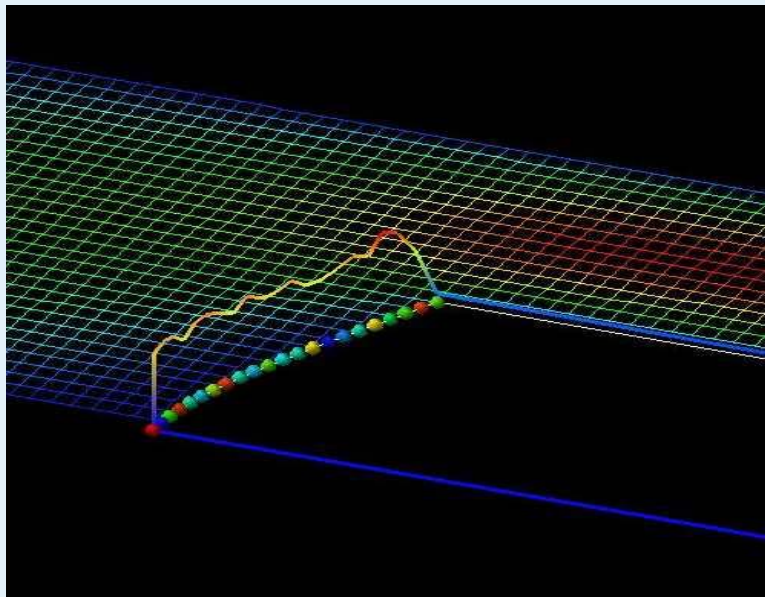


## Force evaluation

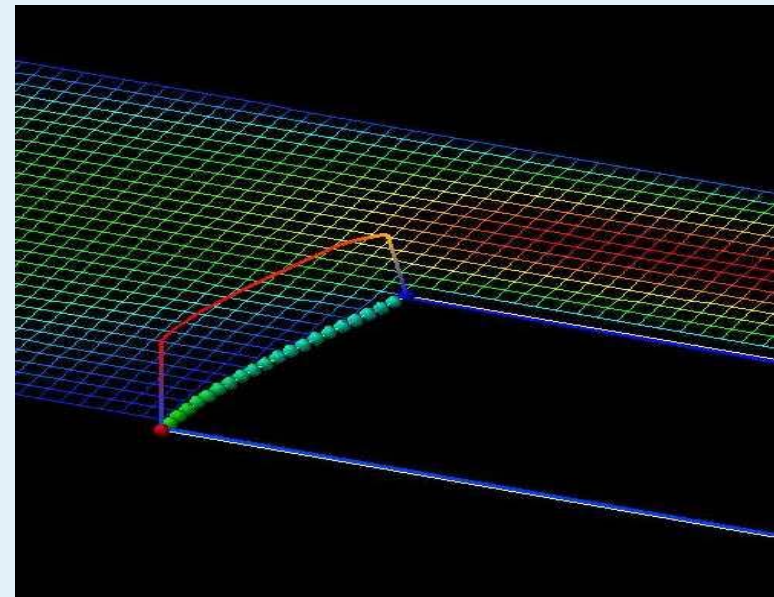
- simple example:



- momentum exchange ☹️

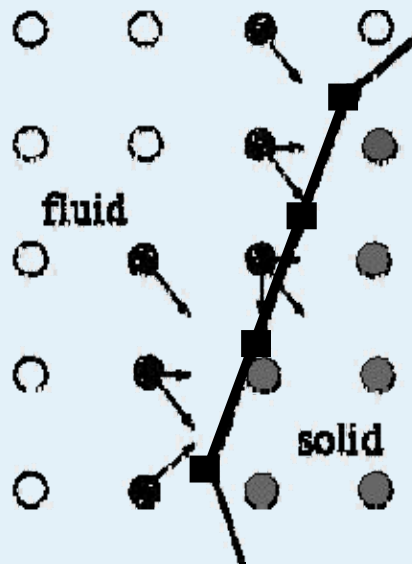


- stress integration 🤔



## Force evaluation

### momentum exchange



- weighted nodal forces
- integration along the whole obstacle
- for lines of subnodal length not appropriate





## Conversion LB-System – ,real world‘

Force:

$$\frac{F_{real}}{H_{real}} = \frac{F_{LB}}{H_{LB}} \frac{\rho_{real} u_{real}^2}{\rho_{LB} u_{LB}^2}$$

Time:

$$T_{real} = T_{LB} \frac{v_{LB} H_{real}^2}{v_{real} H_{LB}^2}$$

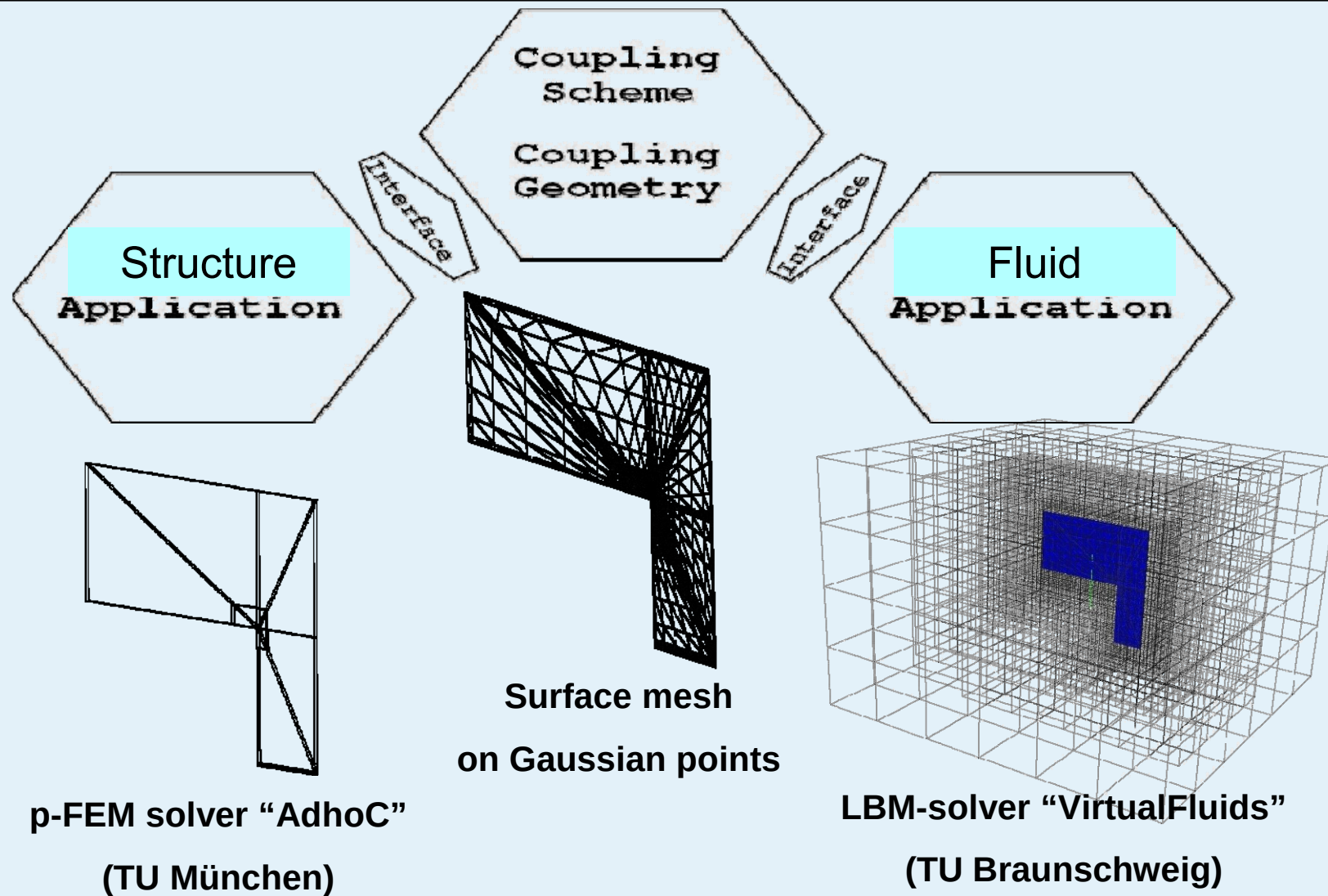
## Fluid-Structure interaction



Ferrybridge, England 1965

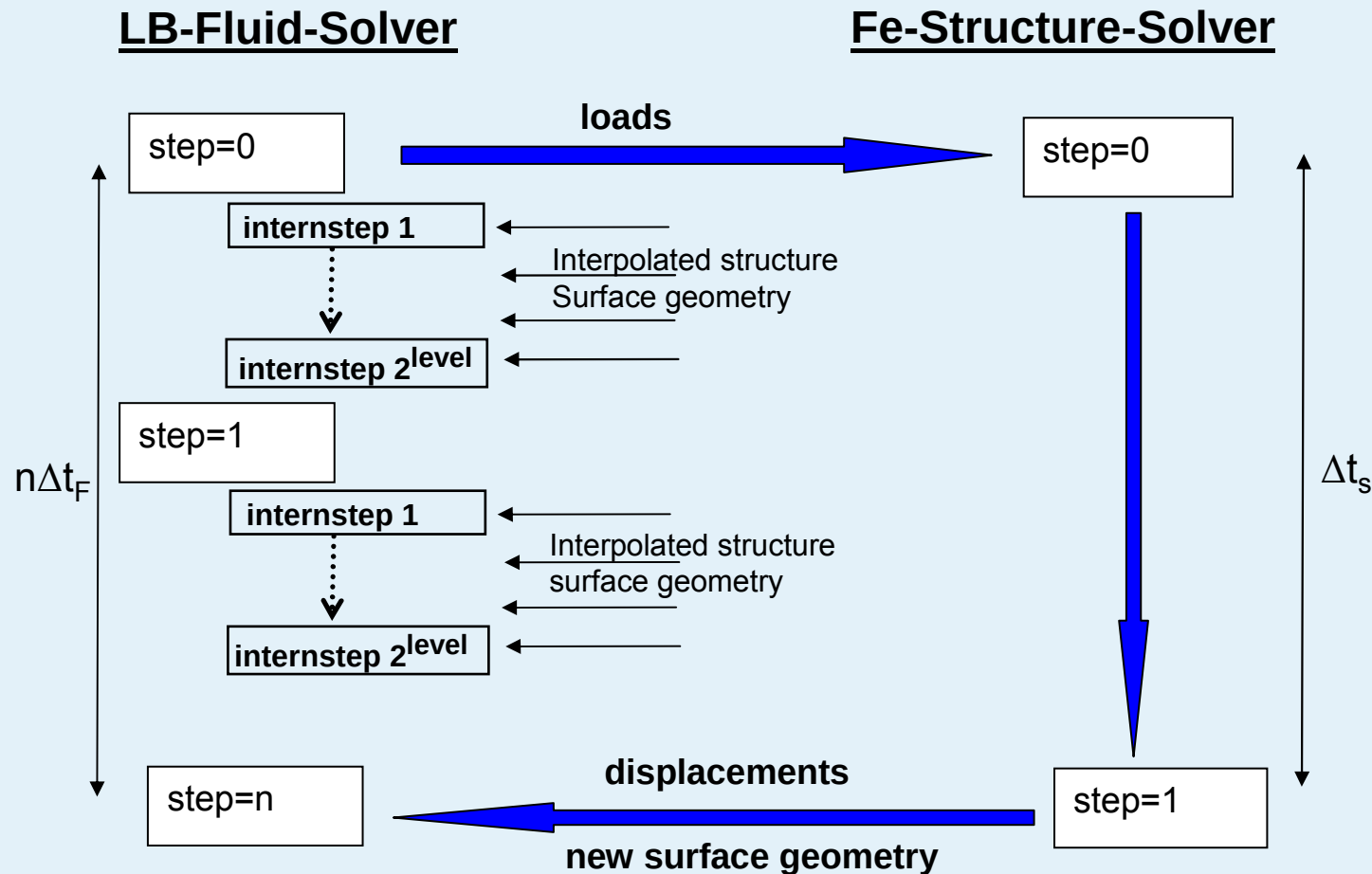


## Fluid-Structure interaction





## Coupling algorithm (explicit)



**Lattice-Boltzmann Method on quadtree type Grids for Fluid-Structure-Interaction**

S. Geller, J. Tölke, M. Krafczyk in H.-J. Bungartz and M. Schäfer, editors, Fluid-Structure Interaction: Modelling, Simulation, Optimisation, Springer Verlag, 2007, preprint available.



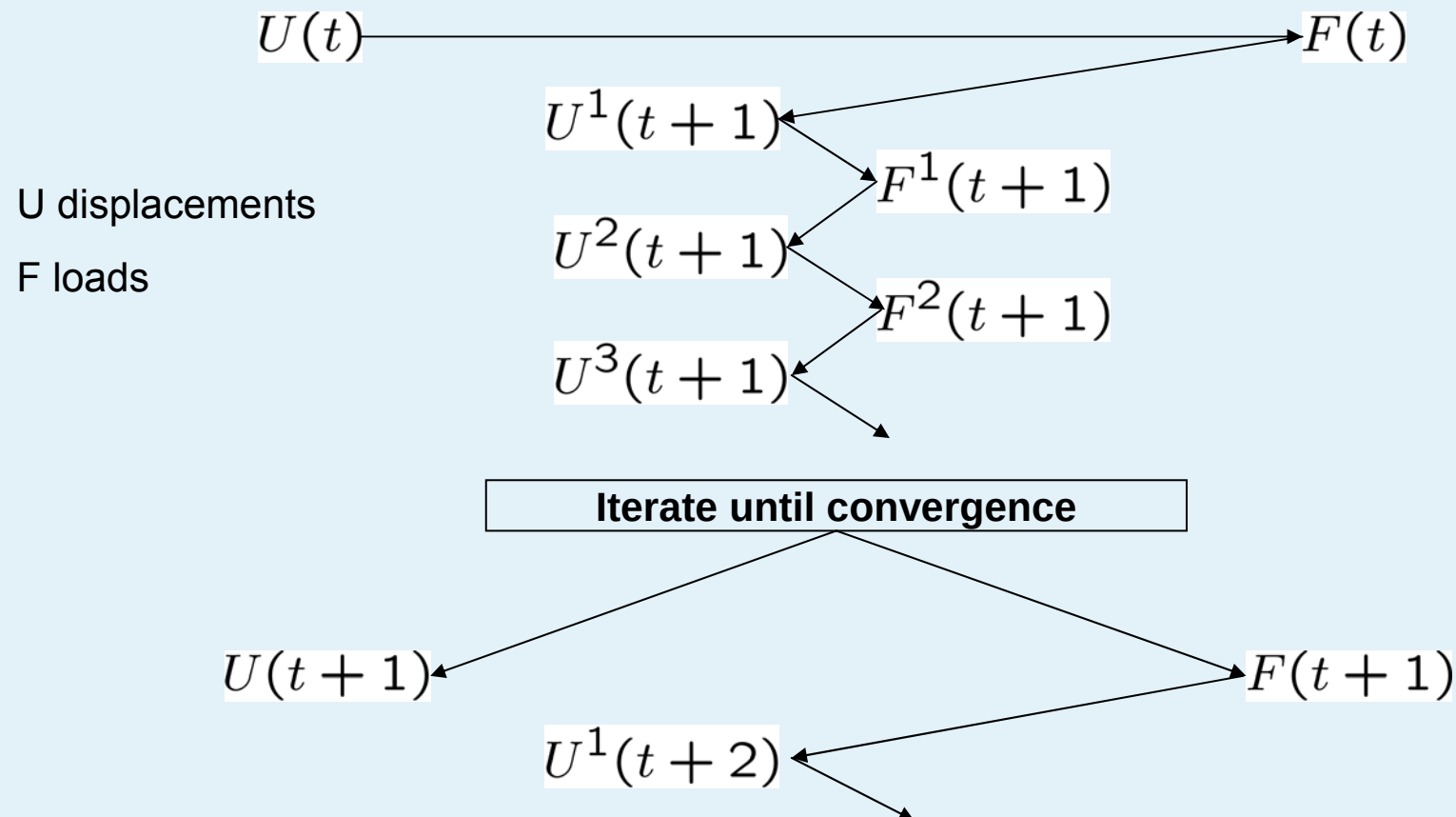
## Coupling algorithm (implicit)

### LB-Fluid-Solver

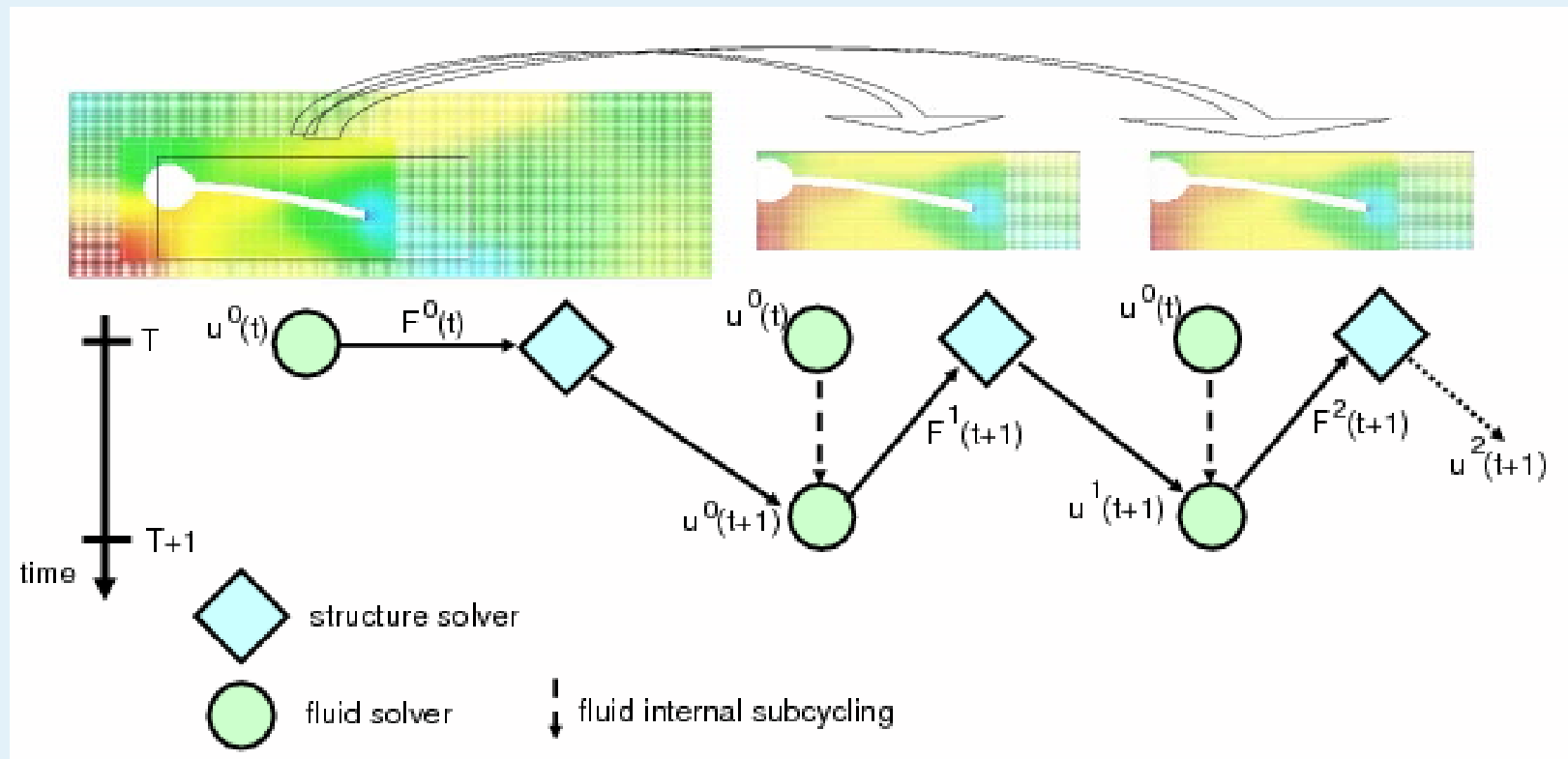
$$F(t+1) = h(U(t), U(t+1))$$

### Fe-Structure-Solver

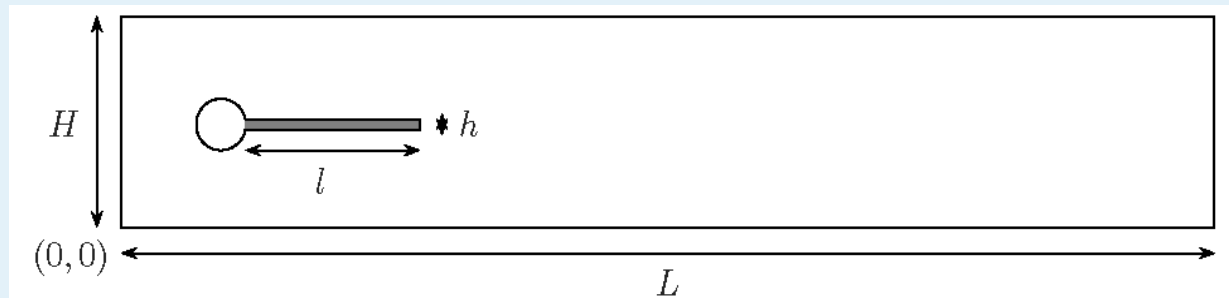
$$U(t+1) = g(F(t), F(t+1))$$



## Coupling algorithm (implicit)



## Benchmark FSI 1/3



$$\begin{aligned}\rho_f &= 1000[\text{kg m}^{-3}] \\ \rho_s &= 1000[\text{kg m}^{-3}] \\ \nu_f &= 1/1000[\text{m}^2\text{s}^{-1}] \\ \nu_s &= 0.4[-]\end{aligned}$$

1D-beam-elements

- ca. 50 DOF
- Newmark

FE-Solver Adhoc

- ca. 1000 DOF
- Newmark

FSI 1 (Re=20):

$$E = 1.4E6[\text{Pa}]$$

$$\bar{U} = 0.2[\text{m s}^{-1}]$$

FSI 3 (Re=200):

$$E = 5.6E6[\text{Pa}]$$

$$\bar{U} = 2.0[\text{m s}^{-1}]$$

Ma=0.1: **1h/Periode**

Ma=0.02: **5h/Periode**

|             | VF+1D-Beam | VF+AdhoC | VF+AdhoC |
|-------------|------------|----------|----------|
| #dof        | 972054     | 972054   | 773334   |
| Ma          | 0.1        | 0.1      | 0.02     |
| Rel. Fehler | 243.9 %    | 7.3 %    | 1.2 %    |

|                 | VF+1D-Beam | VF+AdhoC | VF+AdhoC |
|-----------------|------------|----------|----------|
| #dof            | 2318904    | 1835863  | 1836495  |
| Ma              | 0.1        | 0.1      | 0.02     |
| Rel. F., Mittel | 21.7 %     | 14.0 %   | 3.1 %    |
| Rel. F., Ampl.  | 14.2 %     | 16.0 %   | 1.2 %    |
| Rel. F., Frequ. | 7.8 %      | 0.2 %    | 1.5 %    |





# **Numerical Methods for the discrete Boltzmann equation**

**Manfred Krafczyk**

**contributors:**

**B. Ahrenholz, S. Freudiger, S. Geller, B. Nachtwey, M. Stiebler, J. Tölke**

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**<http://www.cab.bau.tu-bs.de>**



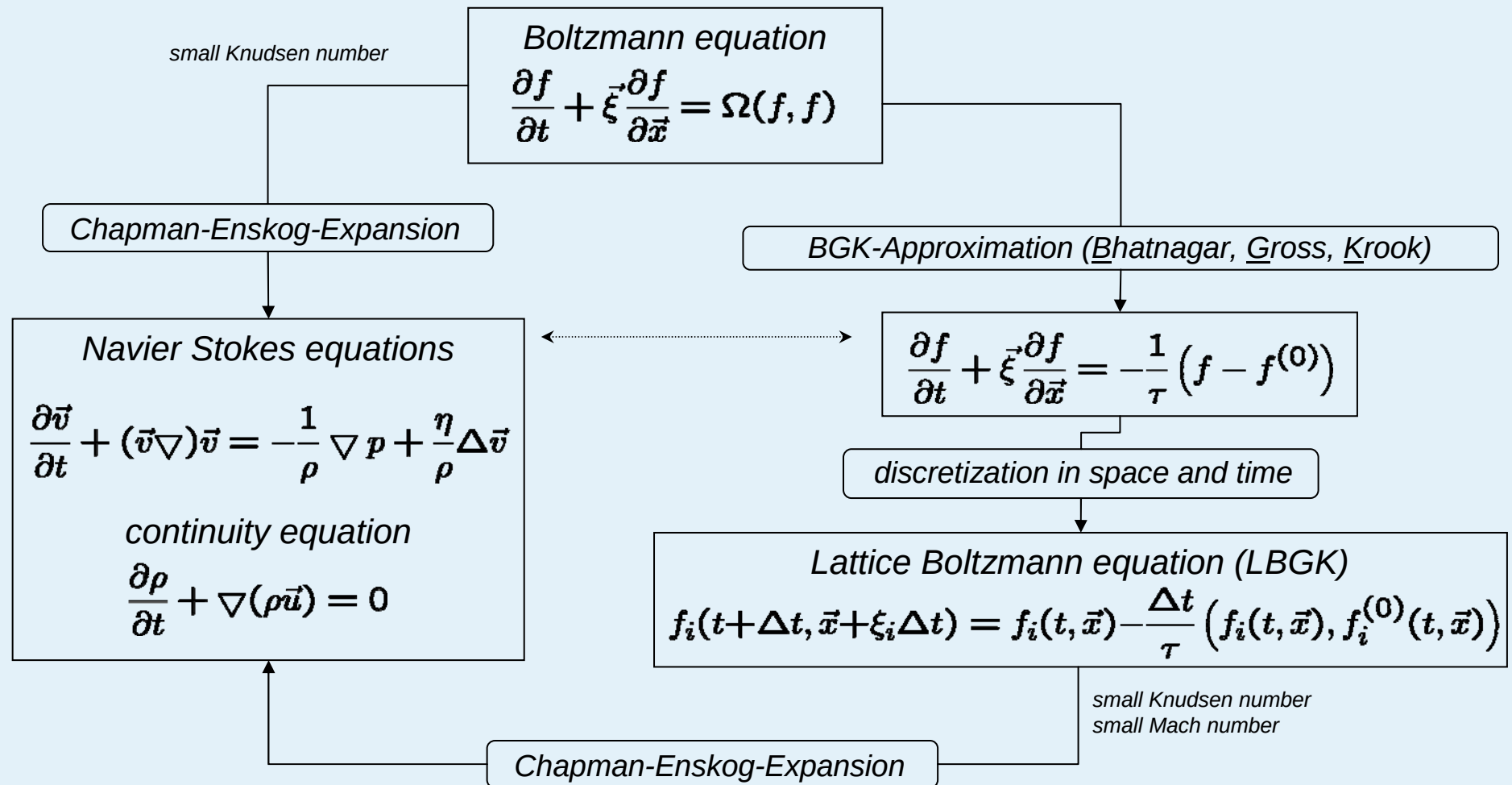


## Overview

- **Reminder: the discrete Boltzmann equation**
- **explicit FD approach**
  - grid refinement
  - adaptivity
- **implicit FD approach**
- **geometric Multigrid for the stationary problem**
- **FV**
- **p-FEM**



# from Boltzmann to Navier Stokes and LBGK





## LB or „conventional“ approach ?

### → direct discretization of the Navier-Stokes equations

- Second-order symmetric Finite Difference in space, explicit first order in time
  - unconditionally unstable for the advection equation
  - max. cell Reynolds number  $< 2$  (Navier-Stokes)
- Finite Volume second order in space, explicit in time
- Finite Differences implicit in space and time
- Spectral methods
- Finite Elements (h-, p-, hp-version, discontinuous Galerkin)
- meshless methods (SPH, X-FEM, ....)
- ...

A general statement concerning the efficiency of LB-methods in comparison to all of the above methods in general is inappropriate and very probably misleading !



## From the discrete BE to LBGK:

## explicit Finite Difference discretization

$$\frac{f_i(\vec{x}, t + \Delta t) - f_i(\vec{x}, t)}{\Delta t} + c \frac{f_i(\vec{x} + \vec{e}_i \Delta t, t + \Delta t) - f_i(\vec{x}, t + \Delta t)}{\Delta x} = -\frac{1}{\tau} (f_i(\vec{x}, t) - f_i^{eq}(\vec{x}, t))$$



$$\Delta t = c \Delta x$$



$$f_i(\vec{x} + \vec{e}_i \Delta t, t + \Delta t) - f_i(\vec{x}, t + \Delta t) = -\frac{\Delta t}{\tau} (f_i(\vec{x}, t) - f_i^{eq}(\vec{x}, t))$$

Taylor expansion + Chapman-Enskog analysis:

viscosity:

$$\mu = c_s^2 \rho \left( \tau - \frac{\Delta t}{2} \right)$$



## grid refinement (Filippova 1998, Krafczyk 1998, Yu, 2002, Crouse, 2002)

LBGK for grid level l:

$$f_{i,l}(\vec{x} + \vec{e}_i \cdot \Delta t_l, t + \Delta t_l) - f_{i,l}(\vec{x}, t) = - \frac{\Delta t_l}{3 \frac{\nu}{c^2} + \frac{1}{2} \Delta t_l} \left( f_{i,l}(\vec{x}, t) - f_{i,l}^{(0)}(\vec{x}, t) \right)$$

continuity of density/pressure and momentum requires for two grids of level  $l = \{c, f\}$ :

$$f_{i,c}^{(0)}(\vec{x}, t) = f_{i,f}^{(0)}(\vec{x}, t) = f_i^{(0)}(\vec{x}, t)$$

Additionally stresses have to be continuous:

$$S_{\alpha\beta} = \left( \frac{\Delta t_l}{2\tau_l} - 1 \right) \Pi_{\alpha\beta}^{(neq)} \propto \sum_i e_{i\alpha} e_{i\beta} f_i^{(neq)}$$



Taylor-expansion delivers equivalent PDE:

$$\frac{\partial f_i(\vec{x}, t)}{\partial t} + \vec{e}_i \nabla f(\vec{x}, t) + O(\Delta t) = \frac{Df_i}{Dt} = - \frac{1}{3\nu + \frac{1}{2} \delta t_l} \left( f_i(\vec{x}, t) - f_i^{(eq)}(\vec{x}, t) \right)$$

Linear approximation:

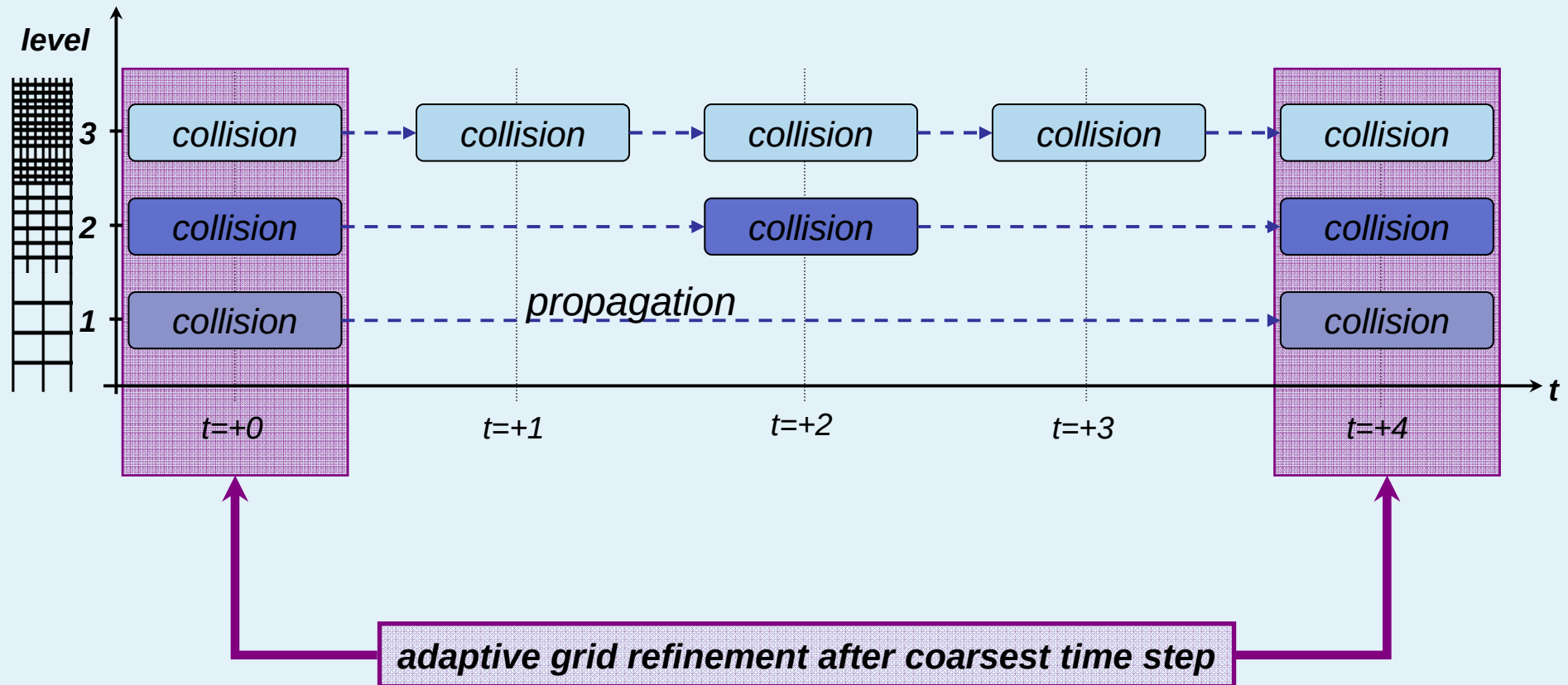
$$\frac{\partial f_i^{(eq)}(\vec{x}, t)}{\partial t} + \vec{e}_i \nabla f_i^{(eq)}(\vec{x}, t) + O(\Delta t) = \frac{Df_i^{(eq)}}{Dt} = - \frac{1}{3\nu + \frac{1}{2} \delta t_l} \left( f_i^{(1)}(\vec{x}, t) \right)$$

Identity of total derivatives  
implies for non-equilibrium  
distributions:

$$\frac{f_{i,c}^{(1)}}{f_{i,f}^{(1)}} = - \frac{3\nu + \frac{1}{2} \delta t_c}{3\nu + \frac{1}{2} \delta t_f}$$



## nested timestepping on non uniform grids





**adaptivity** (Crouse et al. 2002, Tölke et al. 2006)

motivation:

1. less expert knowledge required
2. much more flexible in terms of complicated geometries
3. maximum efficiency for given resources

requirements:

1. unstructured grids for local refining / coarsening
2. error indicator / estimator
3. semi-automatic generation of interface configurations  
e.g. with respect to interpolation
4. implementation optimization to maximize data locality





## error indicator / estimator

*estimator*: residual measure for upper and lower error bound,  
for LBE not yet available !



*indicator*: heuristic measure without guaranteed lower/upper error limit  
(often based on physical properties instead of residua)

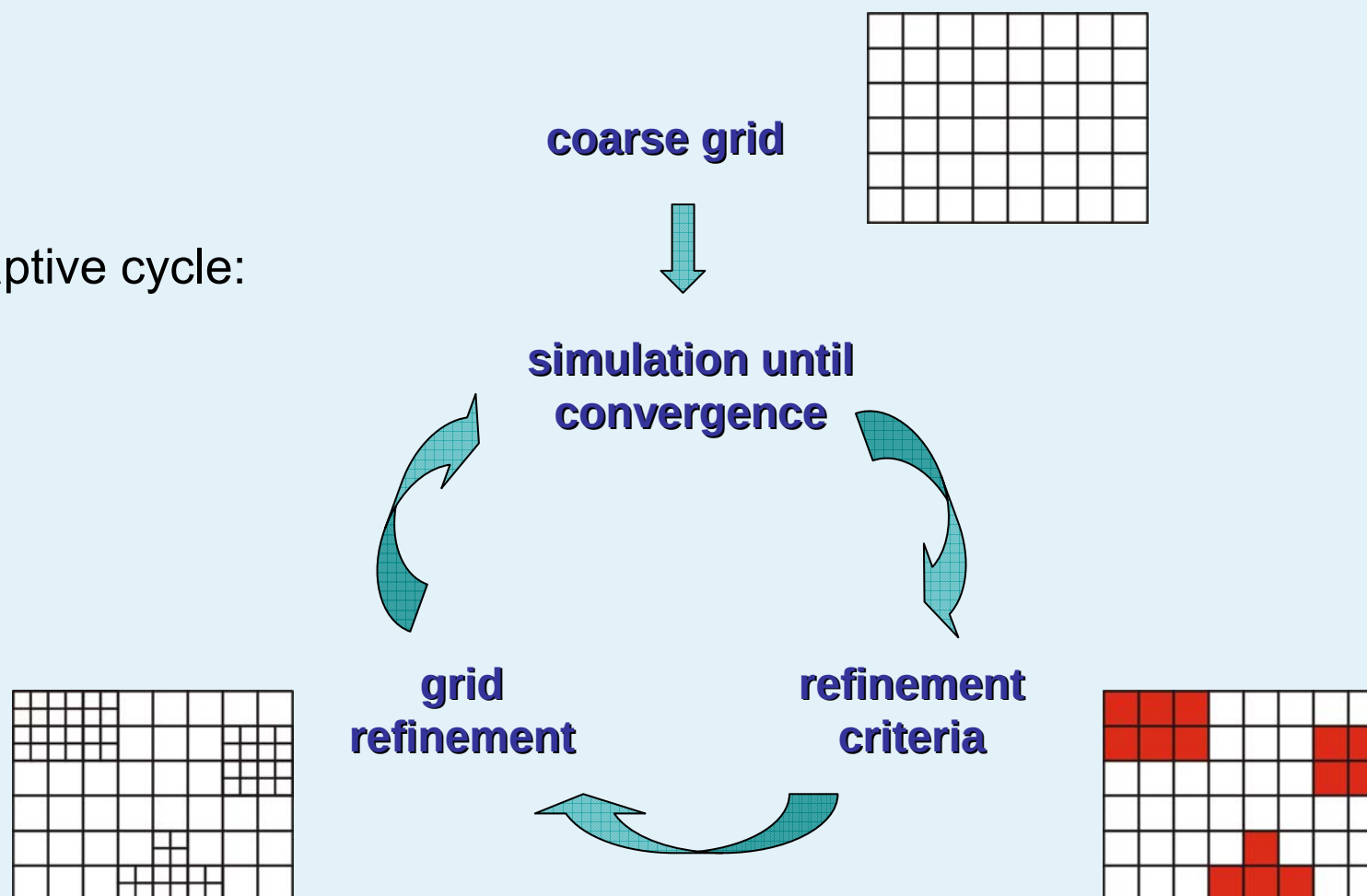
Indicator examples:

- curl magnitude
- divergence magnitude
- velocity difference between nodes
- magnitude of mixed derivatives, e.g.
- .....

$$\sqrt{\left(\frac{\partial u_1}{\partial x_2}\right)^2 + \left(\frac{\partial u_2}{\partial x_1}\right)^2}$$

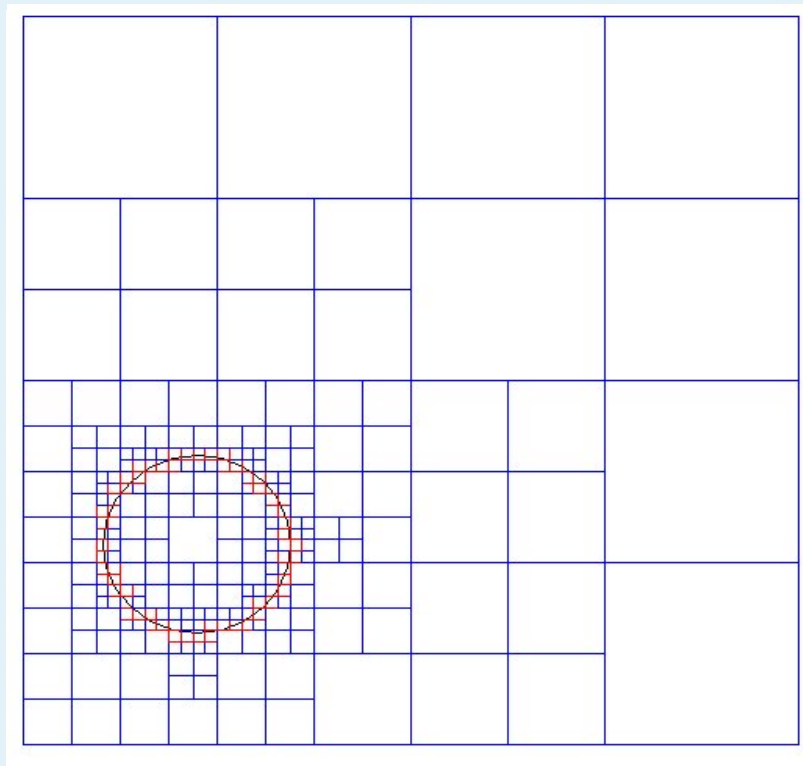


adaptive cycle:





## LOCAL refinement: recursive space tiling using tree data structures



level 0 (root level)

level 1

level 2

level 3

level 4

level 5

level 6

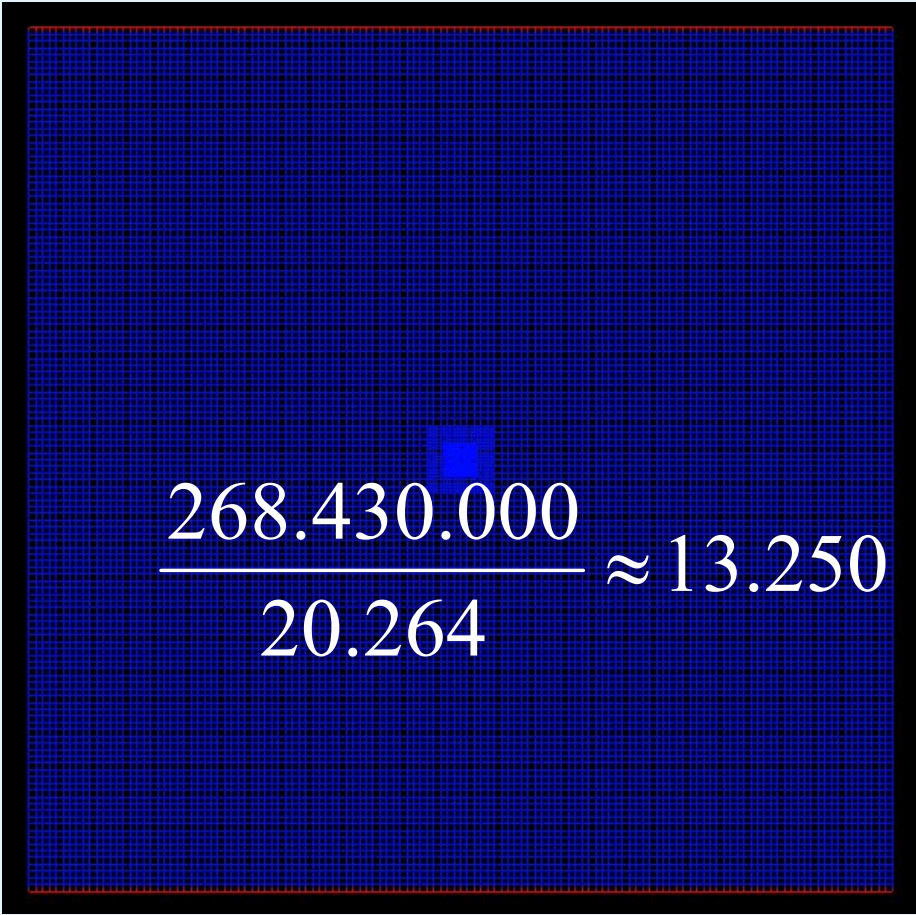
level 6 (smoothed)



(Crouse, Rank, Krafczyk, Tölke, 2002)

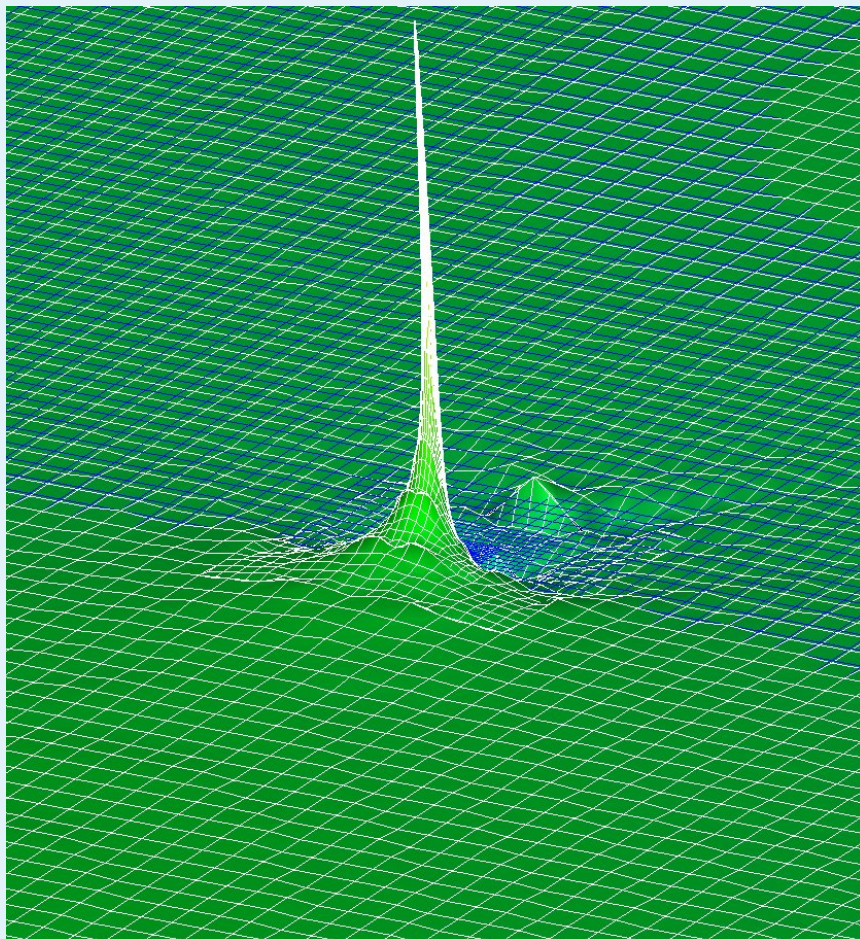
Stokes flow  
(Re = 1):

nonuniform:  
20.264  
grid points

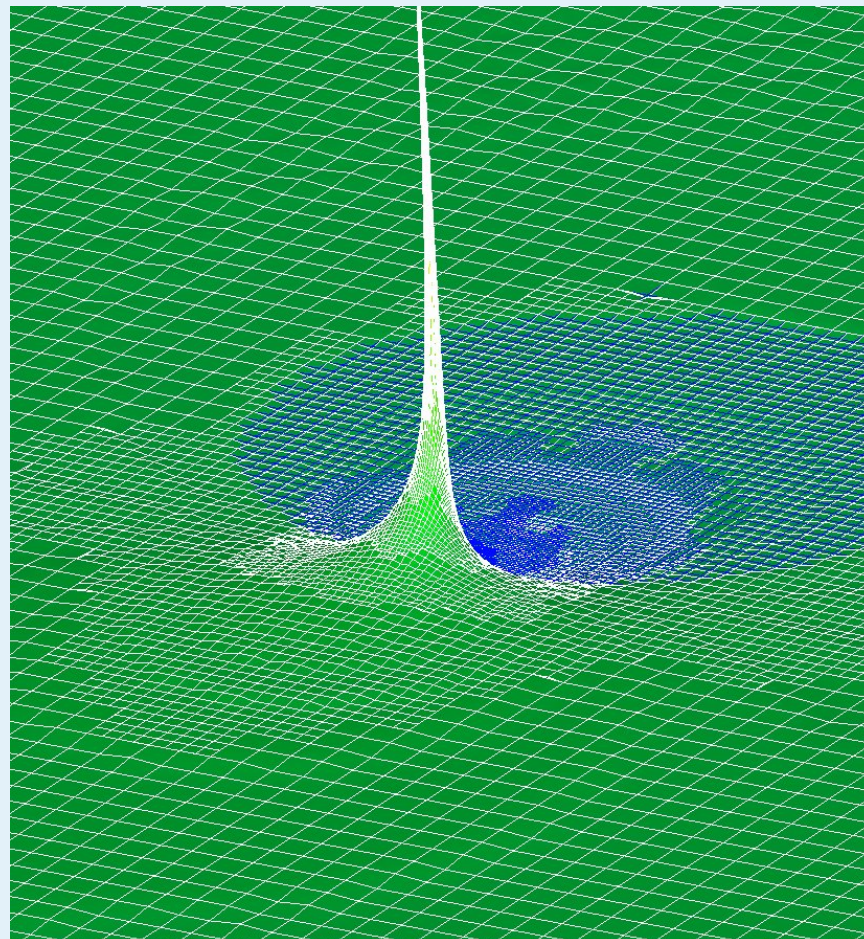

$$\frac{268.430.000}{20.264} \approx 13.250$$

uniform:  
~ 268.430.000  
grid points





'a priori' refinement:



adaptive refinement:



- refinement criterion:  
*divergence magnitude*
- 'a priori refinement':
  - 20135 grid nodes
  - $C_D = 10,01$  (error: 3,8%)
- adaptive simulation:
  - 25658 grid nodes (+ 27,4 %)
  - $C_D = 10,42$   
(error: 0,115%, i.e. reduction by a factor of 33)



## Multi-Grid-acceleration for the stationary discrete BE:

**PDE:**

$$\vec{e}_i \nabla f_i(\vec{x}, t) = -\frac{1}{\tau} (f_i(\vec{x}, t) - f_i^{eq}(\vec{x}, t))$$

**Discretization of the spatial derivatives with 2nd order upwind results in a non-linear system of equations**

$$\vec{G}_l(\vec{f}_1, \vec{f}_2, \vec{f}_3, \dots, \vec{f}_n) = 0 \quad l = 1, \dots, n$$

**smoothing: collective Gauss-Seidel leads to local Newton-Raphson for  $\vec{f}_k$**

$$L_k(\vec{f}_1, \vec{f}_2, \dots, \vec{f}_k, \dots, \vec{f}_n) = 0$$

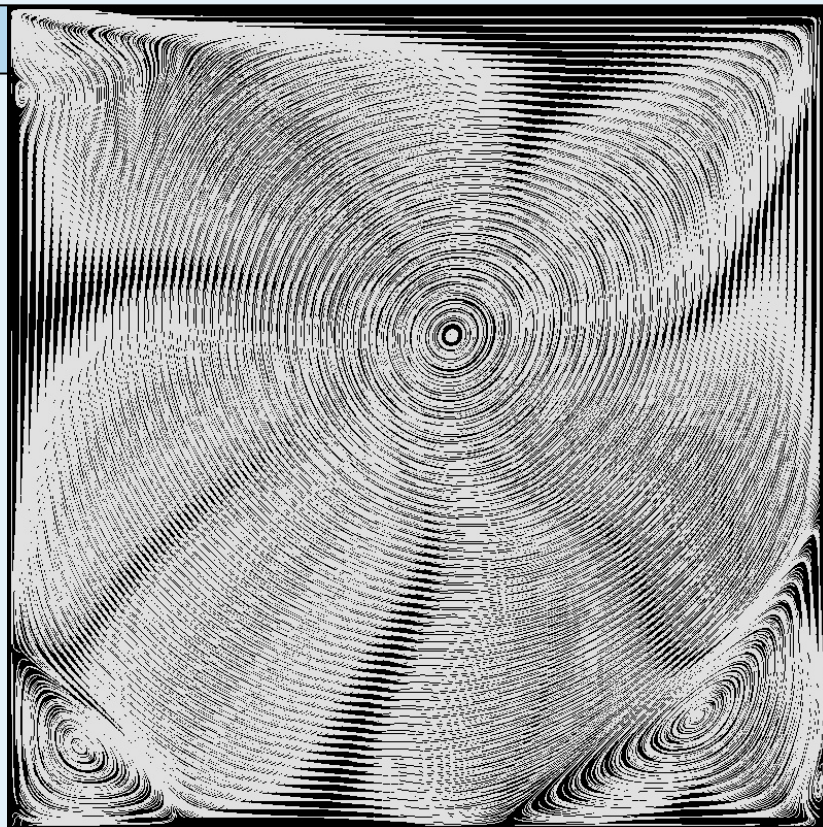
**prolongation and restriction:**

$$\frac{1}{16} \begin{bmatrix} 1 & 2 & 1 \\ 2 & 4 & 2 \\ 1 & 2 & 1 \end{bmatrix}$$

$$\frac{1}{8} \begin{bmatrix} 0 & 1 & 0 \\ 1 & 4 & 1 \\ 0 & 1 & 0 \end{bmatrix}$$

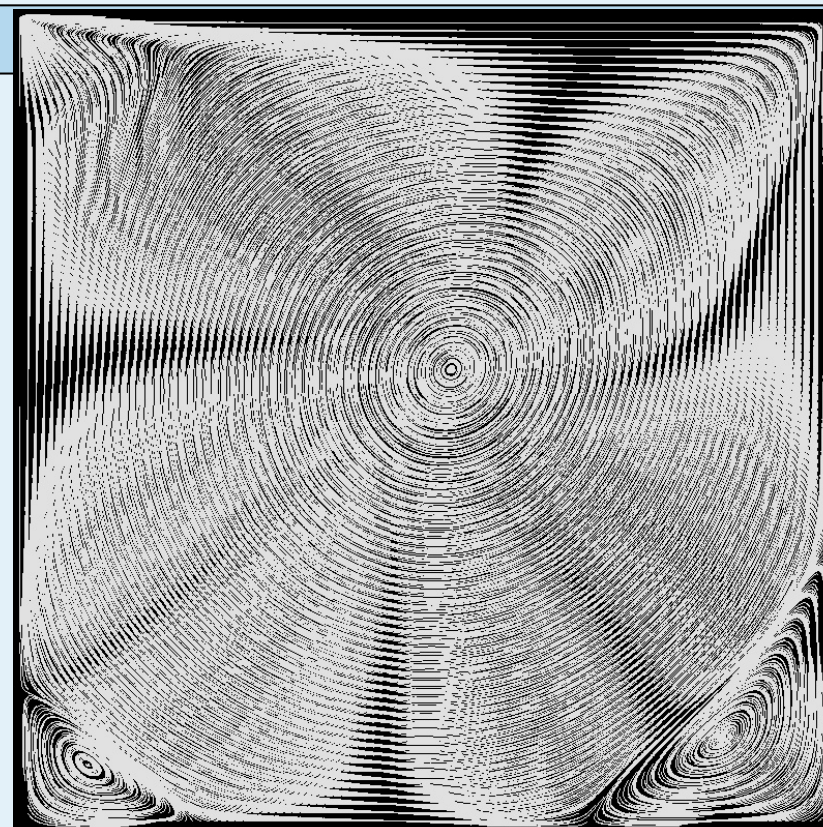
**+bilinear interpolation**





LBGK

FLASH MG prototype



LBGK Code

FLASH



Driven Cavity

 $Re = 1000$ 

512 x 512 nodes

CPU-ratio  $\sim 1:100$





## FV-discretization of the discrete BE

$$\frac{\partial f_a(t, \mathbf{x})}{\partial t} + \xi_a \cdot \frac{\partial f_a(t, \mathbf{x})}{\partial \mathbf{x}} = -\frac{1}{\tau} (f_a(t, \mathbf{x}) - f_a^{(0)}(\rho(t, \mathbf{x}), \mathbf{u}(t, \mathbf{x})))$$

$$a = 0, \dots, 8$$

$$\rho = \sum_{a=0}^8 f_a \quad \rho \mathbf{u} = \sum_{a=0}^8 \xi_a f_a$$

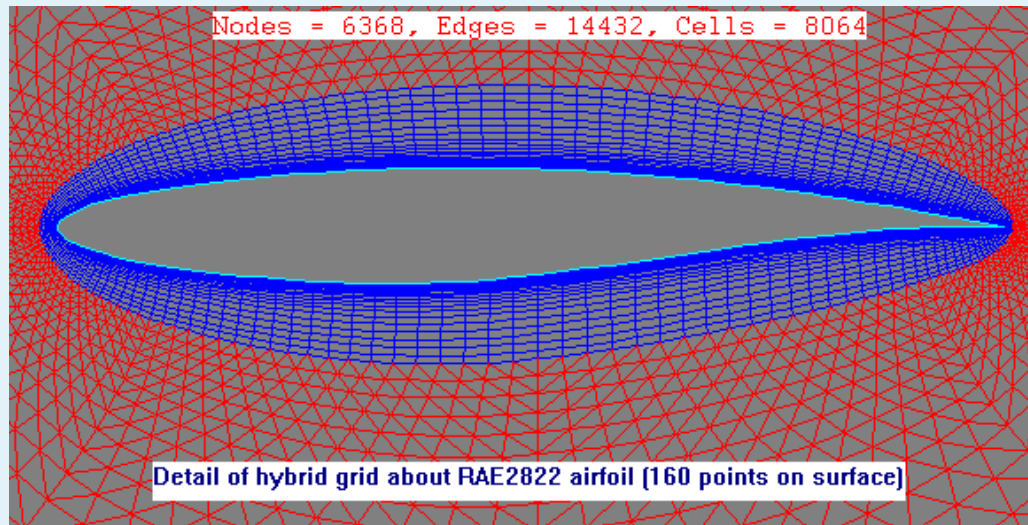
$$f_a^{(0)} = w_a \rho \left[ 1 + 3(\xi_a \cdot \mathbf{u}) + \frac{9}{2} (\xi_a \cdot \mathbf{u})^2 - \frac{3}{2} \mathbf{u} \cdot \mathbf{u} \right]$$

$$w_a = \frac{1}{36} \begin{cases} 16, a = 0 \\ 4, a = 1..4 \\ 1, a = 5..8 \end{cases}$$

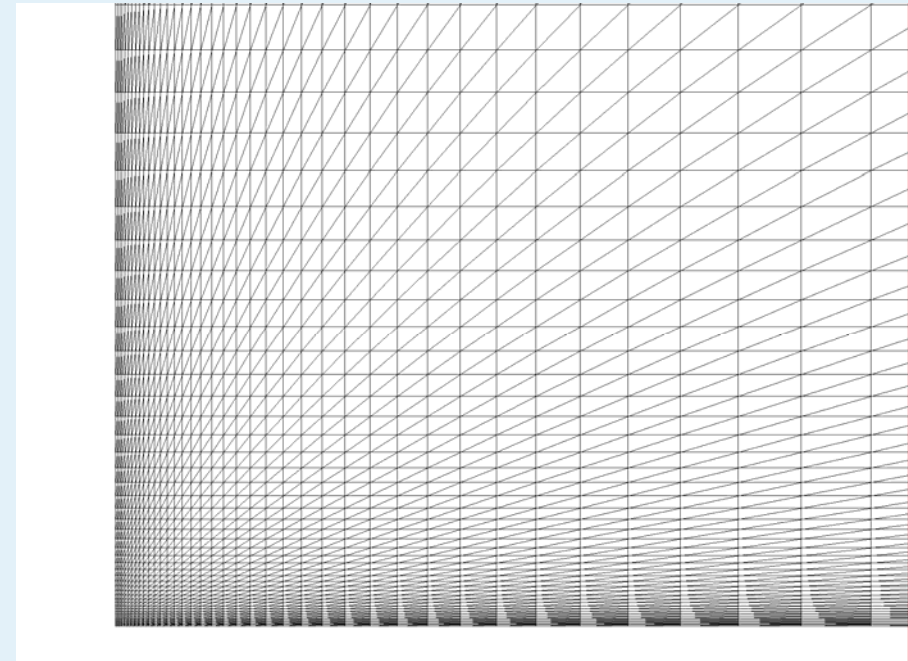
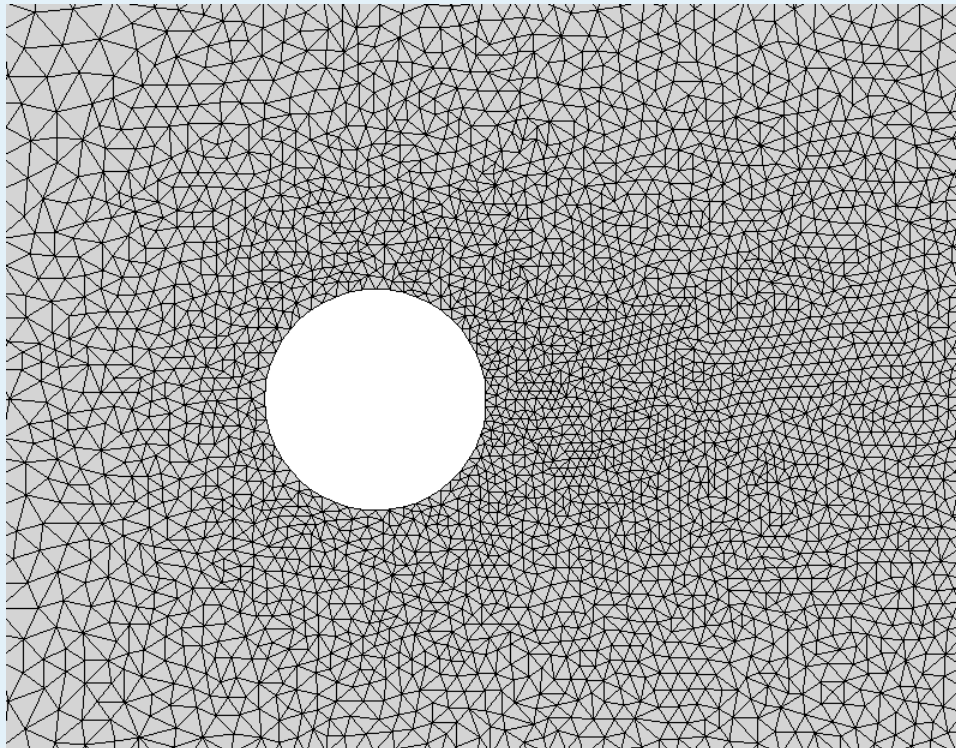
(resting partikel)

## motivation for FV Discretization:

engineering flows are often anisotropic, thus anisotropic elements may be advantageous



## unstructured / anisotropic FV meshes

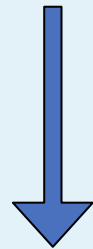




## Finite-Volume-approach (Xi et al. 1999)

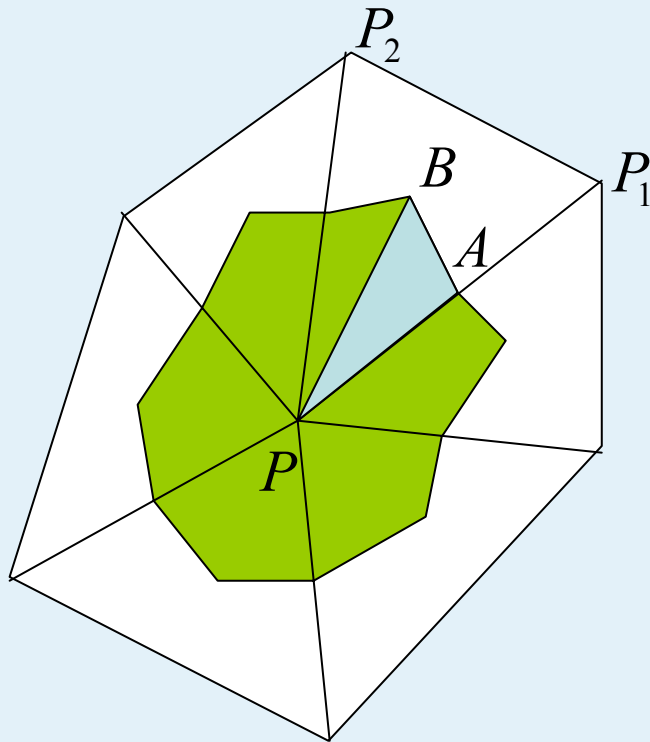
discrete Boltzmann equation:

$$\frac{\partial f_a(t, \mathbf{x})}{\partial t} + \xi_a \cdot \frac{\partial f_a(t, \mathbf{x})}{\partial \mathbf{x}} = -\frac{1}{\tau} (f_a(t, \mathbf{x}) - f_a^{(0)}(t, \mathbf{x}))$$



Integration over control volume  
containing node P

$$A_{CV} \frac{\partial f_a(t, P)}{\partial t} + \xi_a \cdot \oint_{\Gamma_{CV}} \mathbf{n}_{\Gamma} f_a(t, \mathbf{x}) d\Gamma = -\frac{1}{\tau} \int_{\Omega_{CV}} f_a(t, \mathbf{x}) - f_a^{(0)}(t, \mathbf{x}) d\Omega$$



$$\vec{A} = \frac{1}{2}(\vec{P} + \vec{P}_1)$$

$$\vec{B} = \frac{1}{3}(\vec{P} + \vec{P}_1 + \vec{P}_2)$$

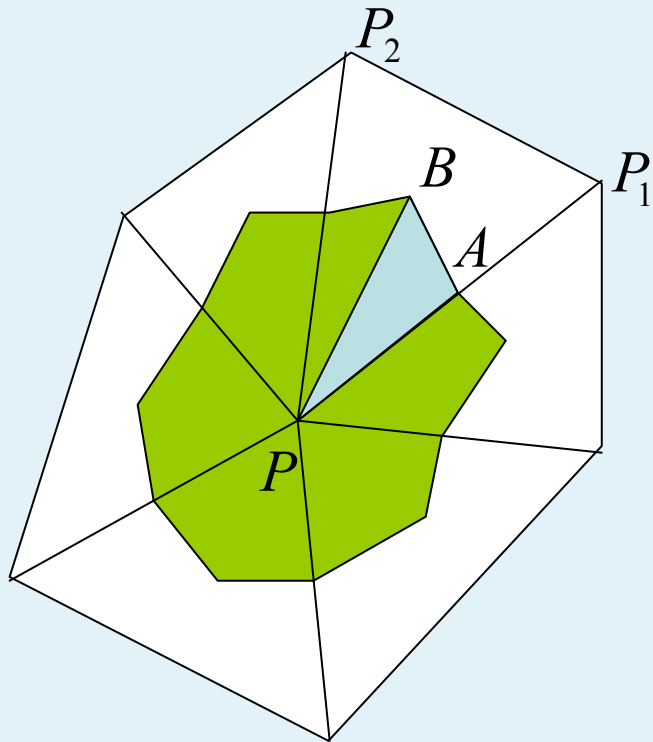
Discrete form of the collision operator:

$$\frac{1}{\tau_{PAB}} \int (f(t, \mathbf{x}) - f^{(0)}(t, \mathbf{x})) d\Omega = A_{PAB} \frac{\sum_{\mathbf{x}=\vec{P}, \vec{A}, \vec{B}} [f(t, \mathbf{x}) - f^{(0)}(t, \mathbf{x})]}{3}$$

where

$$f(A) = \frac{1}{2}[f(P) + f(P_1)]$$

$$f(B) = \frac{1}{3}[f(P) + f(P_1) + f(P_2)]$$

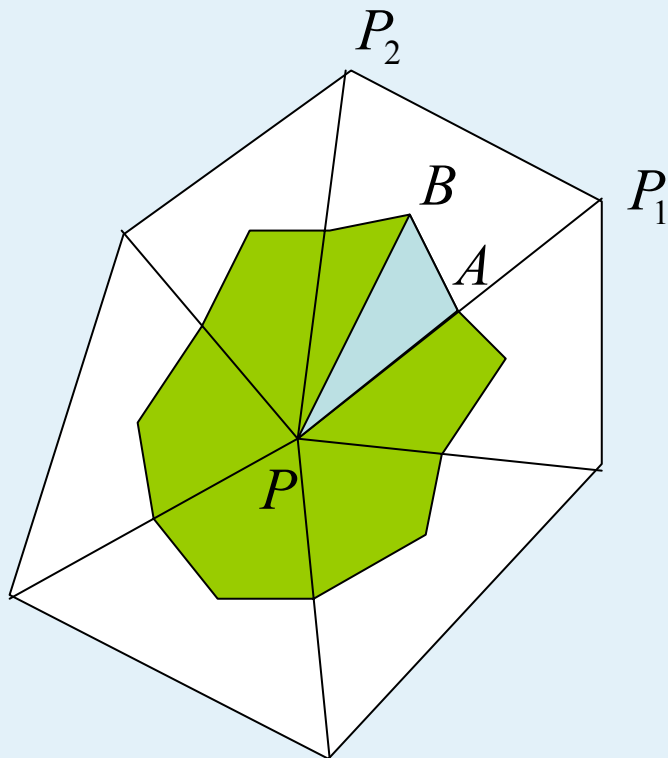


Discrete form of the propagation operator:

$$\xi \cdot \oint_{AB} \mathbf{n}_{AB} f(t, \mathbf{x}) d\Gamma = (\xi \cdot \mathbf{n}_{AB}) l_{AB} f_{flux}$$

$$\vec{A} = \frac{1}{2}(\vec{P} + \vec{P}_1)$$

$$\vec{B} = \frac{1}{3}(\vec{P} + \vec{P}_1 + \vec{P}_2)$$



computation of flux density:

- central scheme:

$$f_{flux} = \frac{f(t, A) + f(t, B)}{2}$$

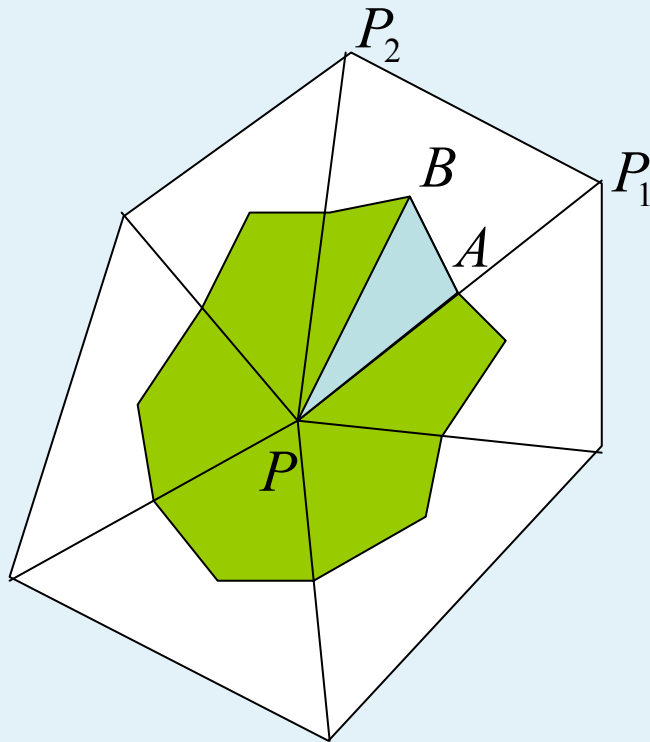
$$f(A) = \frac{1}{2}[f(P) + f(P_1)]$$

$$f(B) = \frac{1}{3}[f(P) + f(P_1) + f(P_2)]$$

$$\vec{A} = \frac{1}{2}(\vec{P} + \vec{P}_1)$$

$$\vec{B} = \frac{1}{3}(\vec{P} + \vec{P}_1 + \vec{P}_2)$$

## Finite-Volume-Method



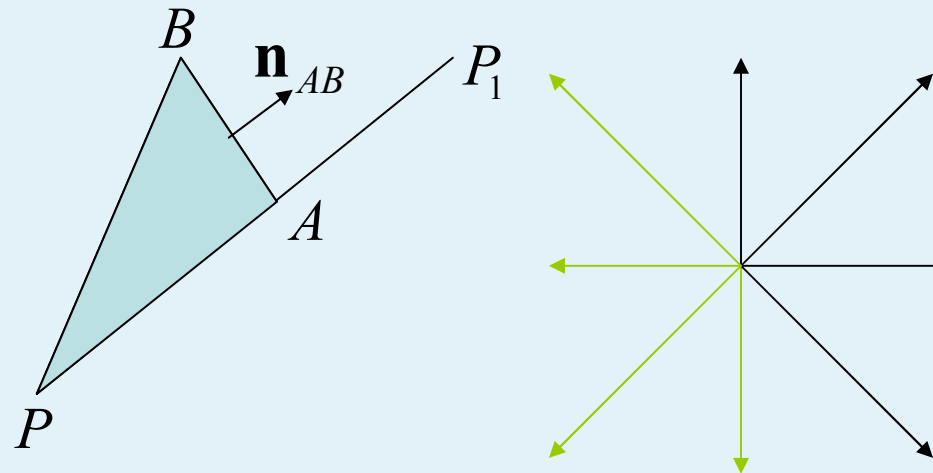
$$\vec{A} = \frac{1}{2}(\vec{P} + \vec{P}_1)$$

$$\vec{B} = \frac{1}{3}(\vec{P} + \vec{P}_1 + \vec{P}_2)$$

computation of flux density:

- first order upwind:

$$f_{a,AB,flux} = \begin{cases} f_{a,P}; \xi_a \cdot \mathbf{n}_{AB} > 0 \\ f_{a,P_1}; \xi_a \cdot \mathbf{n}_{AB} \leq 0 \end{cases}$$







## first order upwind

problem: introduces substantial numerical dissipation

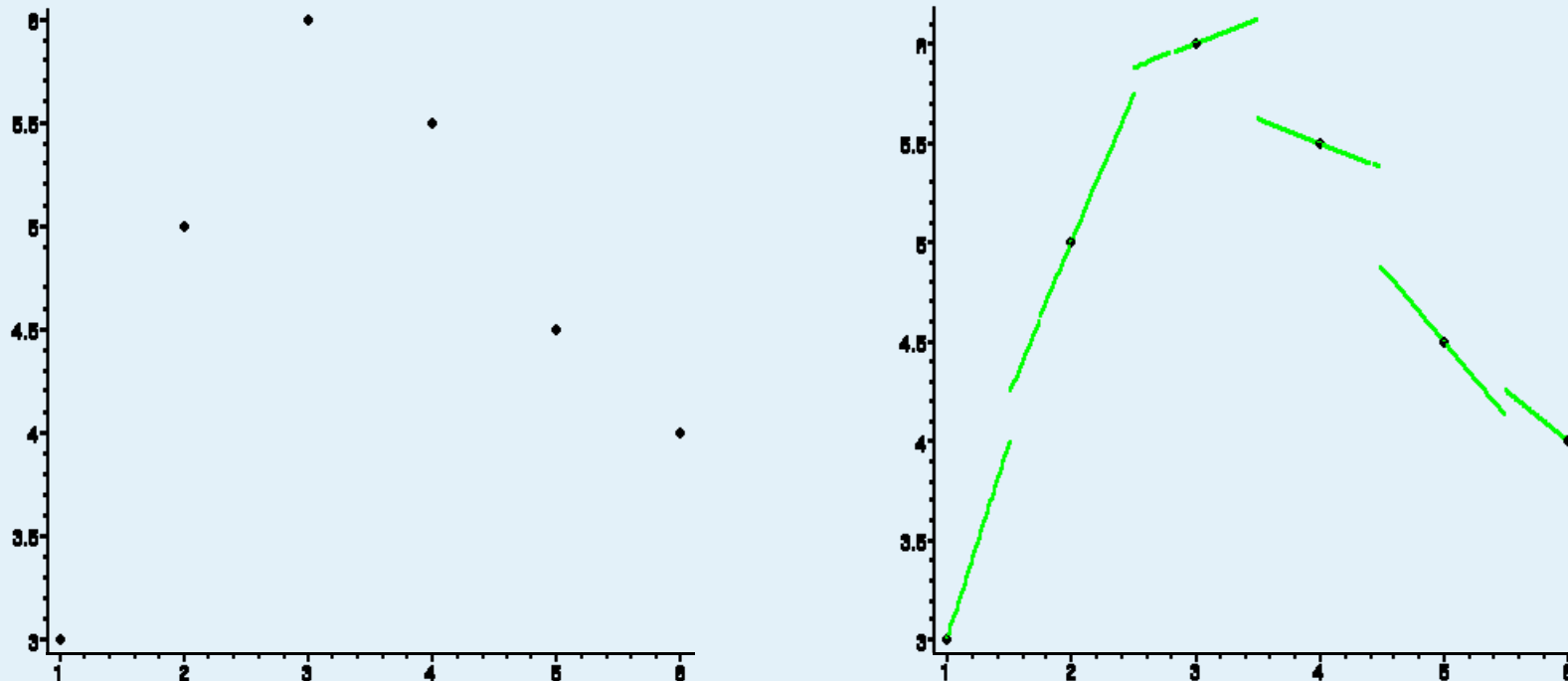
➡ may work as a simple limiter in areas with large gradients

shear rate criterion: 
$$\|S_{ij}\| = \left\| \sum_a \xi_{ai} \xi_{aj} f_a^{(neq)} \right\| > S_{thresh}$$

cell Re-criterion: 
$$Re_{cell} = \frac{|\mathbf{u}| \Delta x}{\nu} > Re_{thresh}$$



## alternative: Least-Squares-Linear-Reconstruction



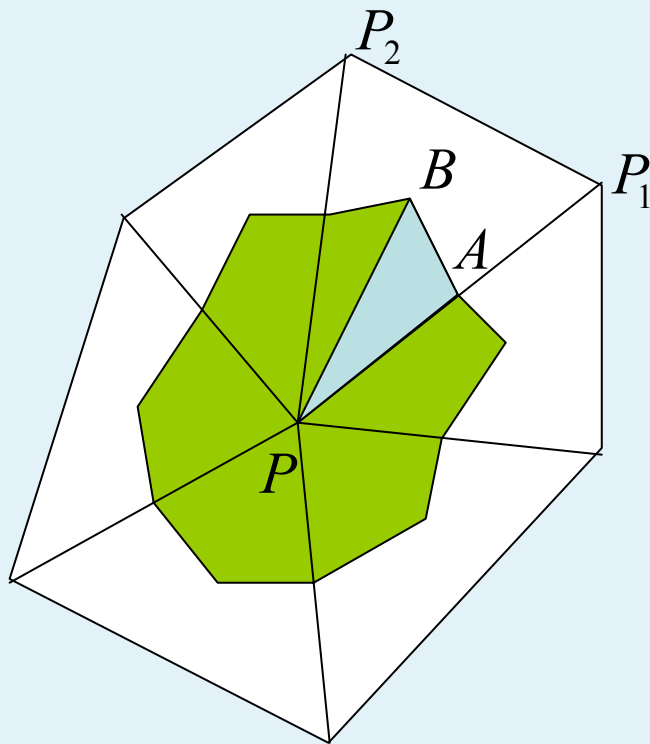
Idea: The assumed distribution gradients in each cell are chosen such that the resulting linear functions optimally extrapolate to the values of  $f$  at the neighboring nodes in a least squares sense.



Stiebler et al., Comp. & Fluids, 2006  
computation of flux density:

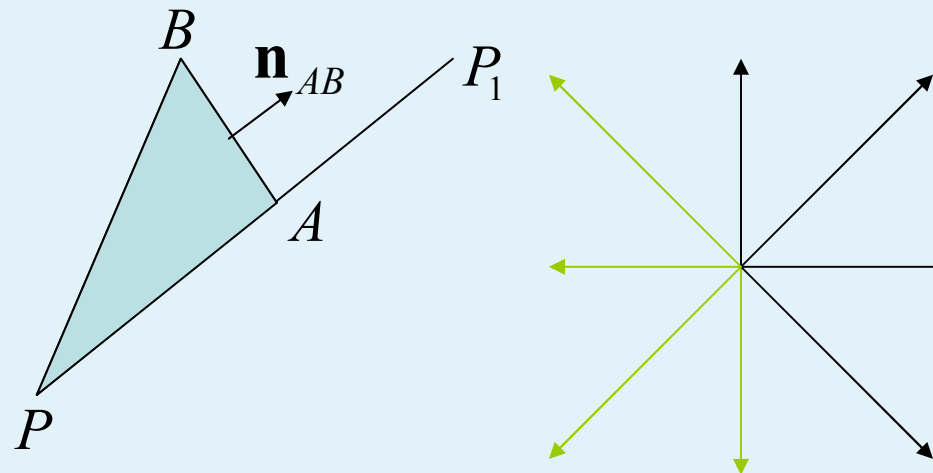
- upwind based on LSLR:

$$f_{a,AB,\text{flux}} = \begin{cases} f_{a,P} + \tilde{\nabla} f_{a,P} \cdot [\{\mathbf{x}_A + \mathbf{x}_B\}/2 - \mathbf{x}_P(P)]; & \xi_a \cdot \mathbf{n}_{AB} > 0 \\ f_{a,P_1} + \tilde{\nabla} f_{a,P_1} \cdot [\{\mathbf{x}_A + \mathbf{x}_B\}/2 - \mathbf{x}_{P_1}(P_1)]; & \xi_a \cdot \mathbf{n}_{AB} \leq 0 \end{cases}$$



$$\vec{A} = \frac{1}{2}(\vec{P} + \vec{P}_1)$$

$$\vec{B} = \frac{1}{3}(\vec{P} + \vec{P}_1 + \vec{P}_2)$$





## least squares – linear reconstruction (LSLR)-scheme

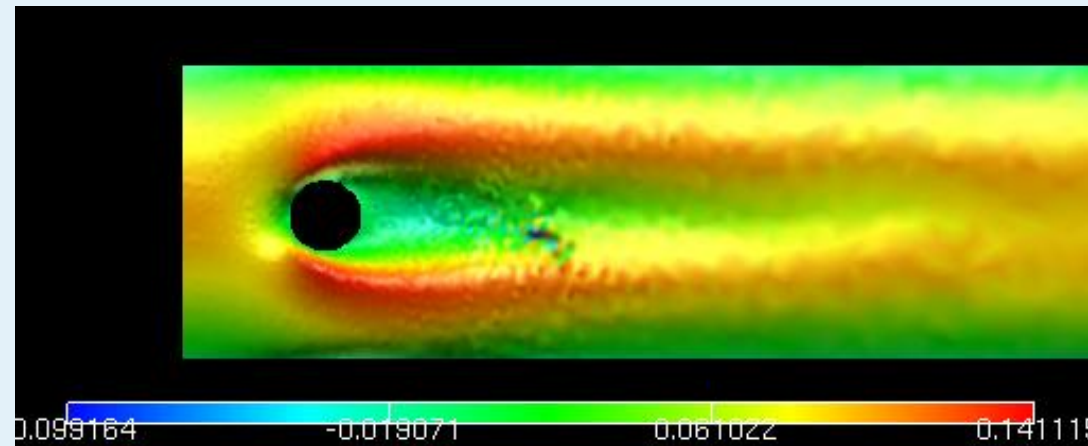
- increase in stability compared to central scheme
- comparable accuracy to central scheme
- additional computational cost to determine the gradient ~50 %



## testcase: flow around cylinder

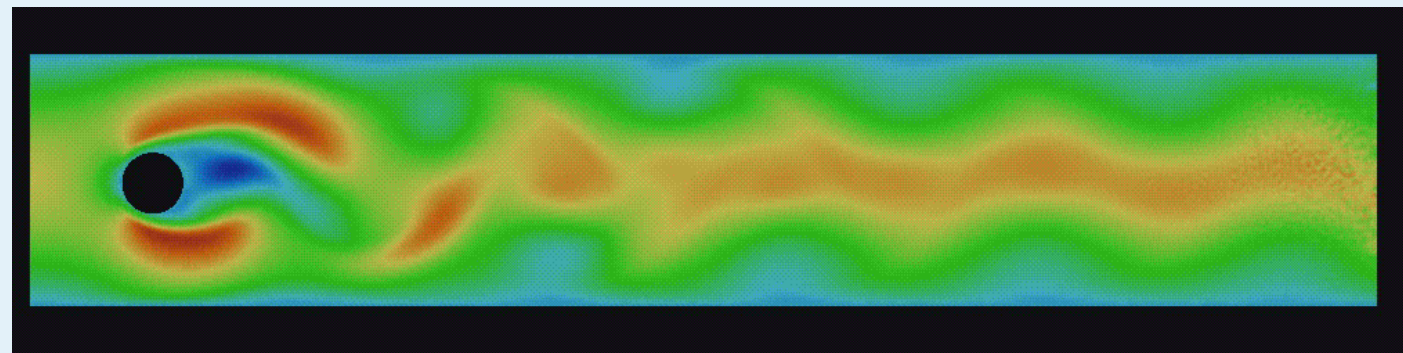


central scheme:



first order upwind-scheme:

$$S_{thresh} = 0.5$$



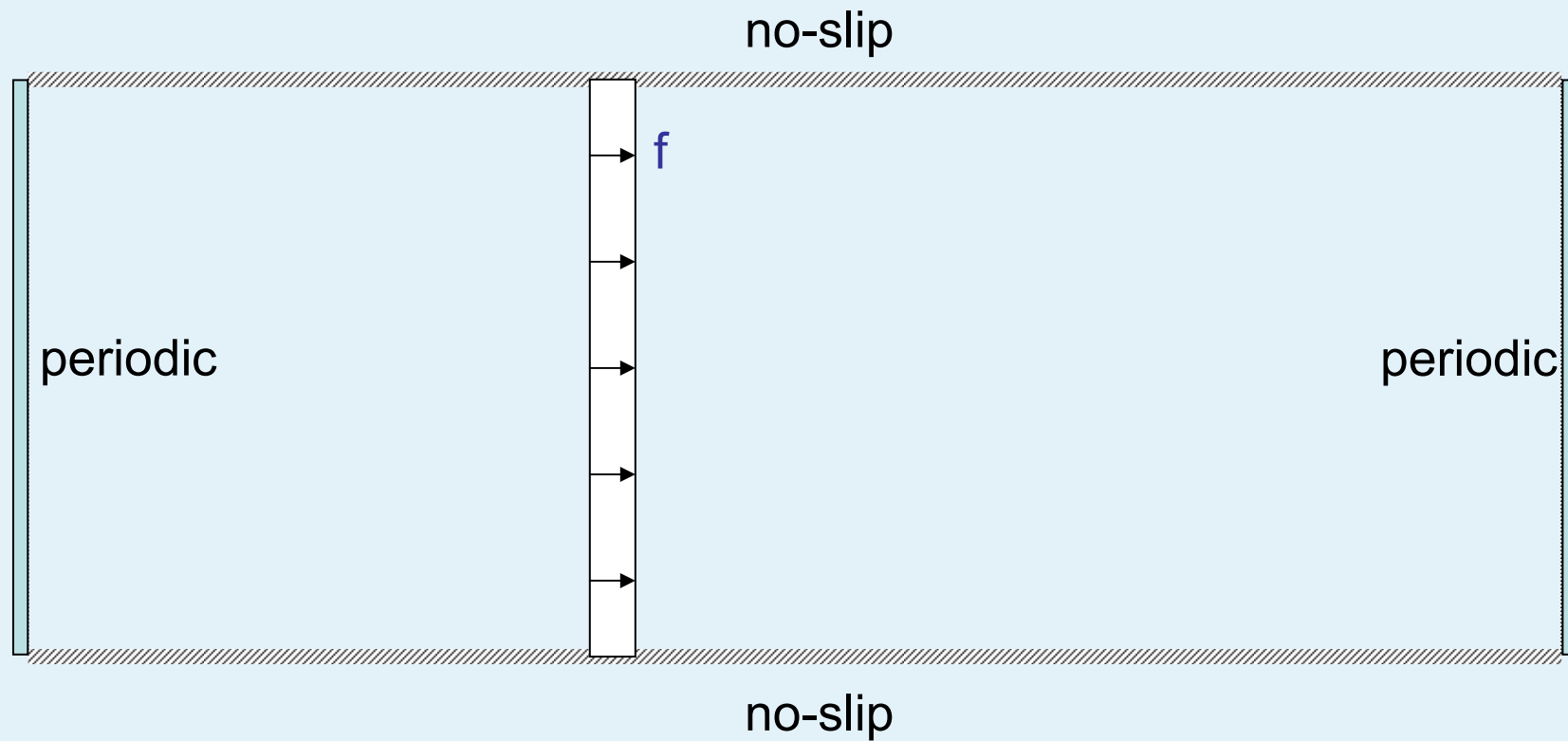


## drag coefficient

| $S_{Thresh}$ | $c_D$ |
|--------------|-------|
| 0,8          | 3,92  |
| 1,0          | 3,67  |
| 1,2          | 3,26  |
| LSLR:        | 3,17  |
| reference:   | 3,23  |



## testcase: Poiseuille flow





## numerical viscosity in channel flow

| $\tau$ | $V_{centr}$ | $V_{upw}$ | $V_{upw} - V_{centr}$ | rel. err. | Re-# |
|--------|-------------|-----------|-----------------------|-----------|------|
| 0.075  | 0,025       | 0,544     | 0,520                 | 20,960    | 320  |
| 0.150  | 0,049       | 0,560     | 0,511                 | 10,484    | 160  |
| 0.300  | 0,096       | 0,602     | 0,505                 | 5,239     | 80   |
| 0.600  | 0,201       | 0,729     | 0,528                 | 2,629     | 40   |

$$\Delta x \approx 1.00 = \frac{H}{80}$$

| $\tau$ | $V_{centr}$ | $V_{upw}$ | $V_{upw} - V_{centr}$ | rel. err. | Re-# |
|--------|-------------|-----------|-----------------------|-----------|------|
| 0.075  | 0,026       | 0,719     | 0,694                 | 27,182    | 320  |
| 0.150  | 0,051       | 0,746     | 0,695                 | 13,573    | 160  |
| 0.300  | 0,104       | 0,797     | 0,693                 | 6,664     | 80   |
| 0.600  | 0,203       | 0,904     | 0,701                 | 3,449     | 40   |

$$\Delta x \approx 1.33 = \frac{H}{60}$$

| $\tau$ | $V_{centr}$ | $V_{upw}$ | $V_{upw} - V_{centr}$ | rel. err. | Re-# |
|--------|-------------|-----------|-----------------------|-----------|------|
| 0.075  | 0,027       | 1,072     | 1,046                 | 39,279    | 320  |
| 0.150  | 0,054       | 1,099     | 1,046                 | 19,504    | 160  |
| 0.300  | 0,118       | 1,261     | 1,143                 | 9,698     | 80   |
| 0.600  | 0,228       | 1,323     | 1,096                 | 4,814     | 40   |

$$\Delta x \approx 2.00 = \frac{H}{40}$$



## drag coefficient for $Re=20$

|                    | # Nodes | cD        | CPU-time |
|--------------------|---------|-----------|----------|
| Ma=0.173:          |         |           |          |
| LBM Grid #1        | 10200   | 5,63      | 16       |
| LBM Grid #2        | 40800   | 5,595     | 120      |
| LBM Grid #3        | 163000  | 5,580     | 900      |
| FVM central #1     | 7564    | 5,51      | 240      |
| FVM central #2     | 11736   | 5,48      | 360      |
| FVM central #3     | 17293   | 5,48      | 480      |
| FVM LSLR #1        | 7564    | 5,62      | 300      |
| FVM LSLR #2        | 11736   | 5,6       | 400      |
| FVM LSLR #3        | 17293   | 5,6       | 690      |
| Ma=0.086:          |         |           |          |
| LBM Grid #1        | 10200   | 5,67      | 30       |
| LBM Grid #2        | 40800   | 5,61      | 200      |
| LBM Grid #3        | 163000  | 5,596     | 1850     |
| FVM central #1     | 7564    | 5,4       | 830      |
| FVM LSLR #1        | 7564    | 6,0       | 16500    |
| reference solution |         | 5.57-5.59 |          |



## Poiseuille flow

|            |         | Re=230  | Re=450 | Re=900 | Re=2300 |
|------------|---------|---------|--------|--------|---------|
| grid #1    | central | ---     | ---    | ---    | ---     |
| (7 nodes)  | LSLR    | 0,248   | 0,377  | 0,537  | 0,739   |
| grid #2    | central | ---     | ---    | ---    | ---     |
| (11 nodes) | LSLR    | 0,123   | 0,201  | 0,323  | 0,538   |
| grid #3    | central | ---     | ---    | ---    | ---     |
| (21 nodes) | LSLR    | 0,0608  | 0,124  | 0,253  | 0,387   |
| grid #4    | central | 0,00627 | ---    | ---    | ---     |
| (41 nodes) | LSLR    | 0,01028 | 0,0318 | 0,05   | 0,203   |

numbers represent

$$e_{L_2} = \left[ \frac{\sum (u_{x,theory} - u_{x,sim})^2}{\sum u_{x,theory}^2} \right]^{\frac{1}{2}}$$



## unstructured FVM vs. hierarchical LBM

Leading error  $O(\Delta x^2)$

Meshing Flexibility

Only Cartesian grids (but  
subgrid corrections possible)

Anisotropic elements for e.g.  
boundary layers

Local refinement / coarsening  
only in powers of two

Computational effort substantially  
higher

Automatic and fast grid generation  
in 3D



## conclusion for present FV Lattice-Boltzmann approaches

- upwind scheme can be used to stabilize a computation in critical regions of the flow
- to reduce the amount of numerical viscosity, higher order upwind schemes will have to be introduced
- a locally implicit time stepping scheme can improve the stability of the method at a considerable computational cost
- least square variants improve stability while maintaining accuracy
- present FV LB implementations are not competitive CFD solvers



## Finite Element Discretization of the discrete Boltzmann equation

### *motivation:*

- weak formulation facilitates development of *a posteriori* error estimators
- allows anisotropic elements
- allows unstructured meshes
- allows curved element boundaries (blending method)
- allows anisotropic ansatz spaces (p-version)



The following slides describing a high-order FEM discretization of the discrete Boltzmann equation are a summary of work recently published by Dr. Alexander Düster in IJNME 2006 ([www.inf.bv.tum.de/~duester](http://www.inf.bv.tum.de/~duester)).

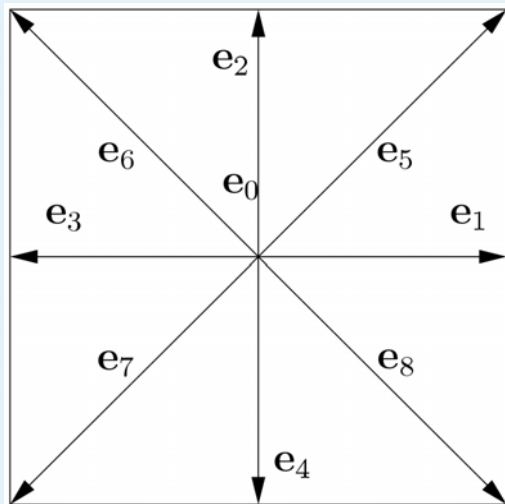


## Discontinuous Galerkin method

$$\frac{\partial f_i}{\partial t} + \mathbf{e}_i \cdot \nabla f_i = C_i \quad \text{in } \Omega \subset \mathbb{R}^2, \quad i = 0, 1, 2, \dots, 8$$

$$\int_{\Omega_e} \phi \frac{\partial f_i}{\partial t} d\Omega = - \int_{\Omega_e} \phi \mathbf{e}_i \cdot \nabla f_i d\Omega + \int_{\Gamma_{in}(\Omega_e)} \phi [f_i] \mathbf{e}_i \cdot \mathbf{n} d\Gamma + \int_{\Omega_e} \phi C_i d\Omega$$

$$i = 0, 1, 2, \dots, 8, \quad \forall \phi$$



$$[f_i] = f_i^+ - f_i^-$$

$$f_i^\pm = \lim_{\varepsilon \rightarrow 0} f_i(\mathbf{x} \pm \varepsilon \mathbf{e}_i)$$

$$f_i^-(\mathbf{x}) = f_i^*(\mathbf{x}) \quad \text{if } \mathbf{x} \in \Gamma_{in}(\Omega)$$

$$\mathbf{e}_i \cdot \mathbf{n} \geq 0 \quad \text{on } \Gamma_{out}(\Omega_e)$$

$$\mathbf{e}_i \cdot \mathbf{n} < 0 \quad \text{on } \Gamma_{in}(\Omega_e)$$





## Spatial discretization:

$$\hat{\phi} = \sum_{k=1}^{k_{modes}} N_k \hat{\phi}_k = \mathbf{N} \hat{\phi} \quad \hat{f}_i = \sum_{k=1}^{k_{modes}} N_k \hat{f}_{i,k} = \mathbf{N} \hat{\mathbf{f}}_i$$

$$\nabla \hat{\phi} = \sum_{k=1}^{k_{modes}} \nabla N_k \hat{\phi}_k = \mathbf{B} \hat{\phi} \quad \nabla \hat{f}_i = \sum_{k=1}^{k_{modes}} \nabla N_k \hat{f}_{i,k} = \mathbf{B} \hat{\mathbf{f}}_i$$

$$\mathbf{N} = \begin{bmatrix} N_1 & N_2 & N_3 & \dots & N_{k_{modes}} \end{bmatrix} \quad \mathbf{B} = \begin{bmatrix} \frac{\partial N_1}{\partial x} & \frac{\partial N_2}{\partial x} & \frac{\partial N_3}{\partial x} & \dots & \frac{\partial N_{k_{modes}}}{\partial x} \\ \frac{\partial N_1}{\partial y} & \frac{\partial N_2}{\partial y} & \frac{\partial N_3}{\partial y} & \dots & \frac{\partial N_{k_{modes}}}{\partial y} \end{bmatrix}$$



$$\int_{\Omega_e} \phi \frac{\partial f_i}{\partial t} d\Omega = - \int_{\Omega_e} \phi \mathbf{e}_i \cdot \nabla f_i d\Omega + \int_{\Gamma_{in}(\Omega_e)} \phi [f_i] \mathbf{e}_i \cdot \mathbf{n} d\Gamma + \int_{\Omega_e} \phi C_i d\Omega$$

$$i = 0, 1, 2, \dots, 8, \forall \phi$$



$$\int_{\Omega_e} \mathbf{N}^T \mathbf{N} d\Omega \frac{d\hat{\mathbf{f}}_i}{dt} = - \int_{\Omega_e} \mathbf{N}^T \mathbf{e}_i \cdot \nabla \hat{f}_i d\Omega +$$

$$+ \int_{\Gamma_{in}(\Omega_e)} \mathbf{N}^T \mathbf{n} \cdot \mathbf{e}_i [\hat{f}_i] d\Gamma + \int_{\Omega_e} \mathbf{N}^T C_i d\Omega$$



$$\mathbf{M} \frac{d\hat{\mathbf{f}}_i}{dt} = \mathbf{L}(\hat{\mathbf{f}}_i)$$



## Temporal discretization: forward Euler:

$$M \frac{d\hat{\mathbf{f}}_i}{dt} = \mathbf{L}(\hat{\mathbf{f}}_i)$$

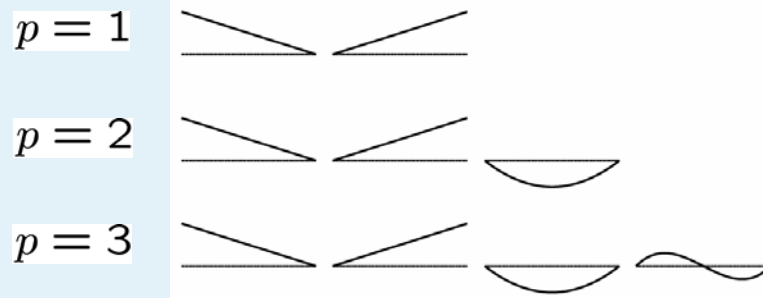
$$M \frac{\hat{\mathbf{f}}_i^{n+1} - \hat{\mathbf{f}}_i^n}{\Delta t} = \mathbf{L}(\hat{\mathbf{f}}_i^n)$$



$$\begin{aligned} M \Delta \hat{\mathbf{f}}_i^{n+1} &= \Delta t \mathbf{L}(\hat{\mathbf{f}}_i^n), \quad i = 0, 1, 2, \dots, 8 \\ \hat{\mathbf{f}}_i^{n+1} &= \hat{\mathbf{f}}_i^n + \Delta \hat{\mathbf{f}}_i^{n+1} \end{aligned}$$



## Hierarchic shape functions of high order finite elements in 1D (Szabó, Babuška 1991)



$$\left. \begin{aligned} N_1(\xi) &= \frac{1}{2}(1 - \xi) \\ N_2(\xi) &= \frac{1}{2}(1 + \xi) \end{aligned} \right\} p = 1$$

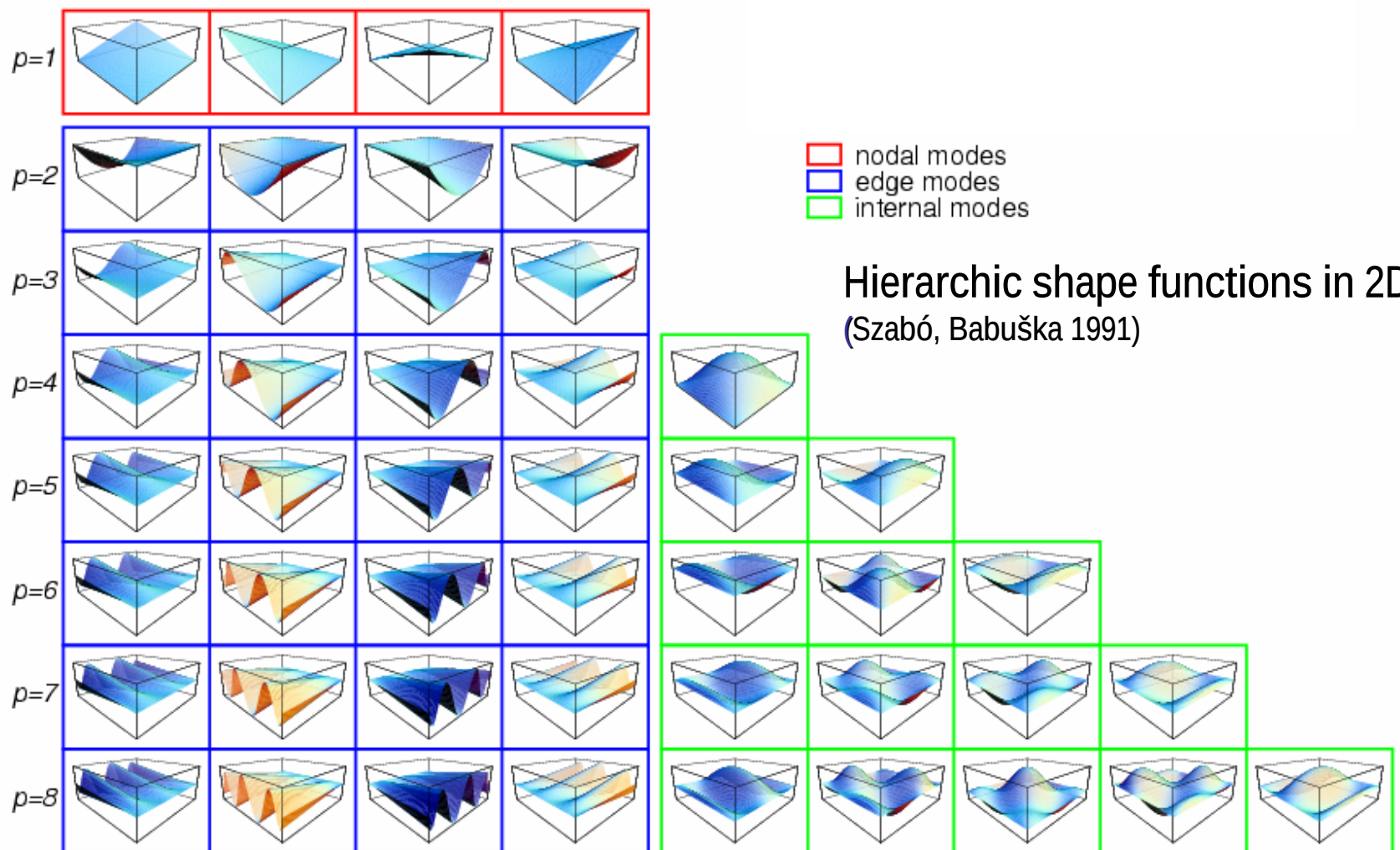
$$N_i(\xi) = \phi_{i-1}(\xi), \quad i = 3, 4, \dots, p + 1$$

## Integrated Legendre Polynomials

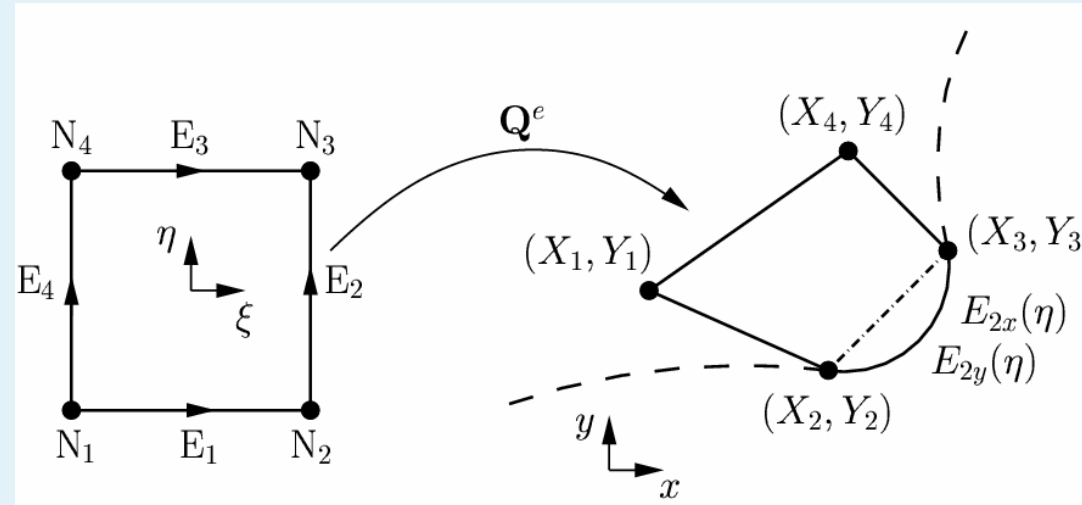
$$\phi_j(\xi) = \sqrt{\frac{2j-1}{2}} \int_{-1}^{\xi} L_{j-1}(x) dx = \frac{1}{\sqrt{4j-2}} (L_j(\xi) - L_{j-2}(\xi)), \quad j = 2, 3, \dots$$

## Orthogonality property

$$\int_{-1}^1 \frac{dN_i}{d\xi} \frac{dN_j}{d\xi} d\xi = \delta_{ij}, \quad i \geq 3 \text{ and } j \geq 1 \text{ or } i \geq 1 \text{ and } j \geq 3$$



## Blending function method (Gordon, Hall 1973)



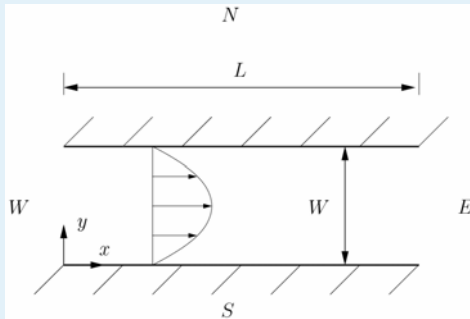
$$x = Q_x^e(\xi, \eta) = \sum_{i=1}^4 N_{1,1}^{N_i}(\xi, \eta) X_i + \left[ E_{2x}(\eta) - \left( \frac{1-\eta}{2} X_2 + \frac{1+\eta}{2} X_3 \right) \right] \frac{1+\xi}{2}$$

$$y = Q_y^e(\xi, \eta) = \sum_{i=1}^4 N_{1,1}^{N_i}(\xi, \eta) Y_i + \left[ E_{2y}(\eta) - \left( \frac{1-\eta}{2} Y_2 + \frac{1+\eta}{2} Y_3 \right) \right] \frac{1+\xi}{2}$$

$$N_{1,1}^{N_i}(\xi, \eta) = \frac{1}{4}(1 + \xi_i \xi)(1 + \eta_i \eta), i = 1, 2, 3, 4$$



## Poiseuille flow



### Navier-Stokes solution

$$u_x = \frac{F_x W^2}{8\rho\nu} \left(1 - \left(\frac{2y}{W} - 1\right)^2\right)$$

$$u_y = 0$$

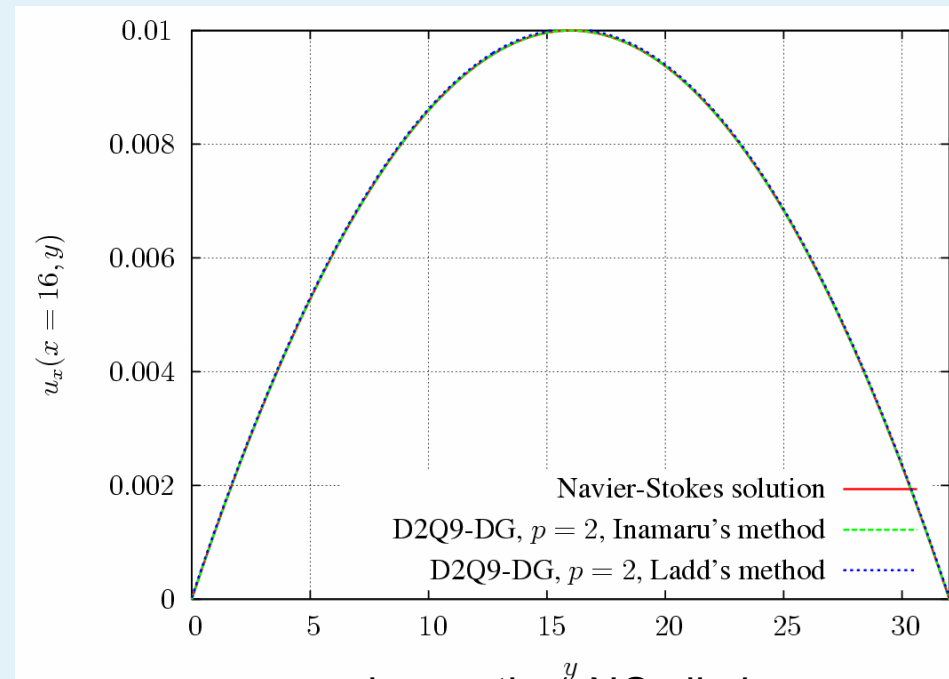
convergence to stationary solution with  $p = 2$ :

Inamaru's method: after 9000 time steps:

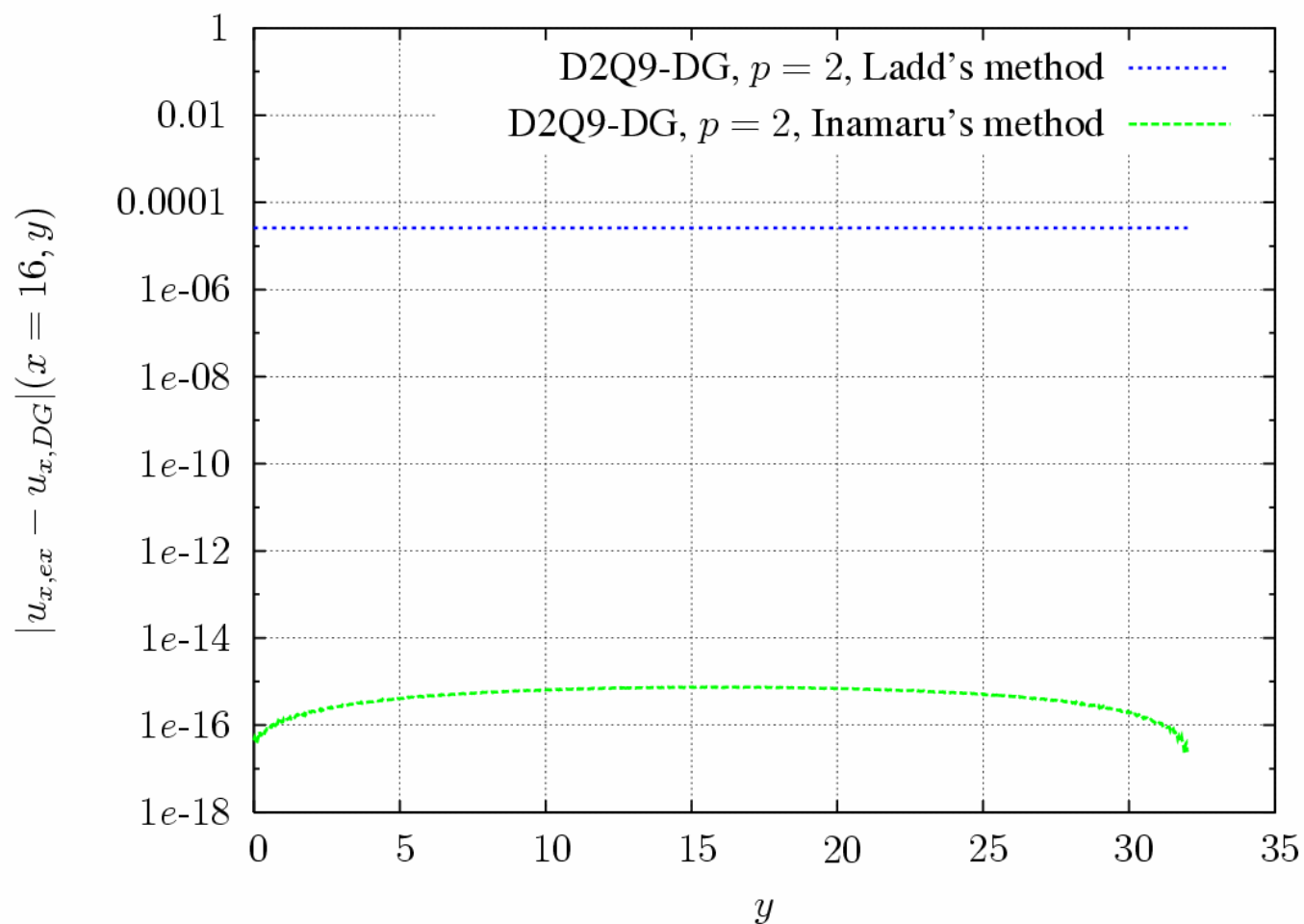
error in  $L_2$  norm  $\approx 1.1 \times 10^{-13}$

Ladd's method: after 11000 time steps:

error in  $L_2$  norm  $\approx 8.3 \times 10^{-4}$



observation: NO slip layer !

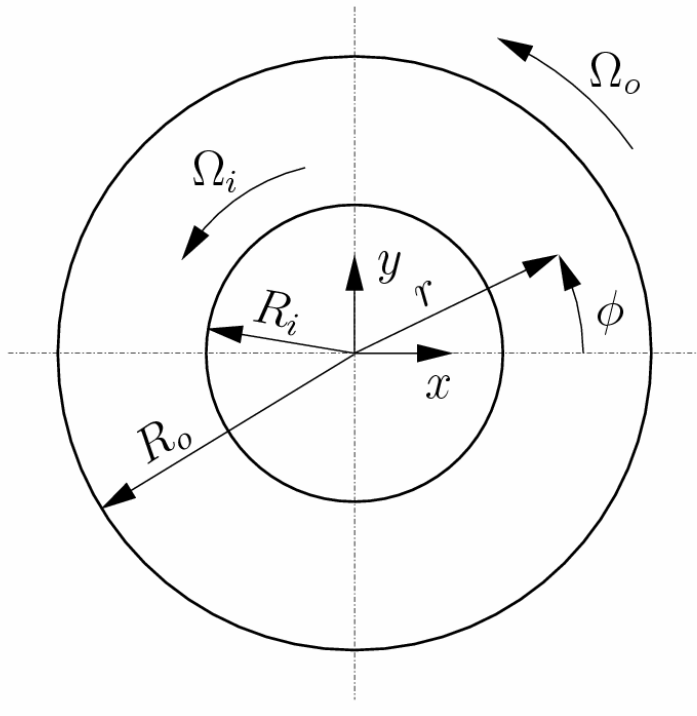




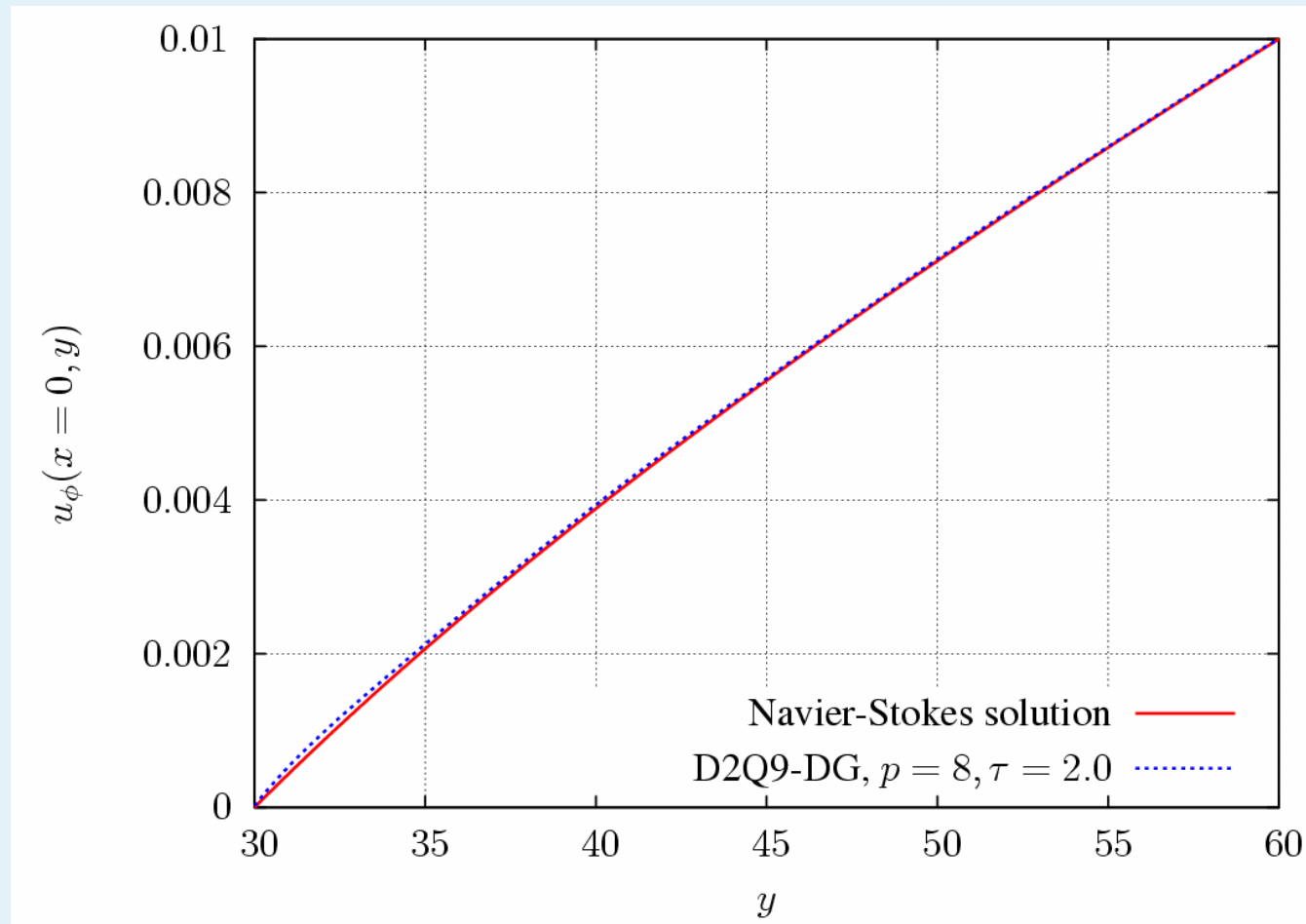


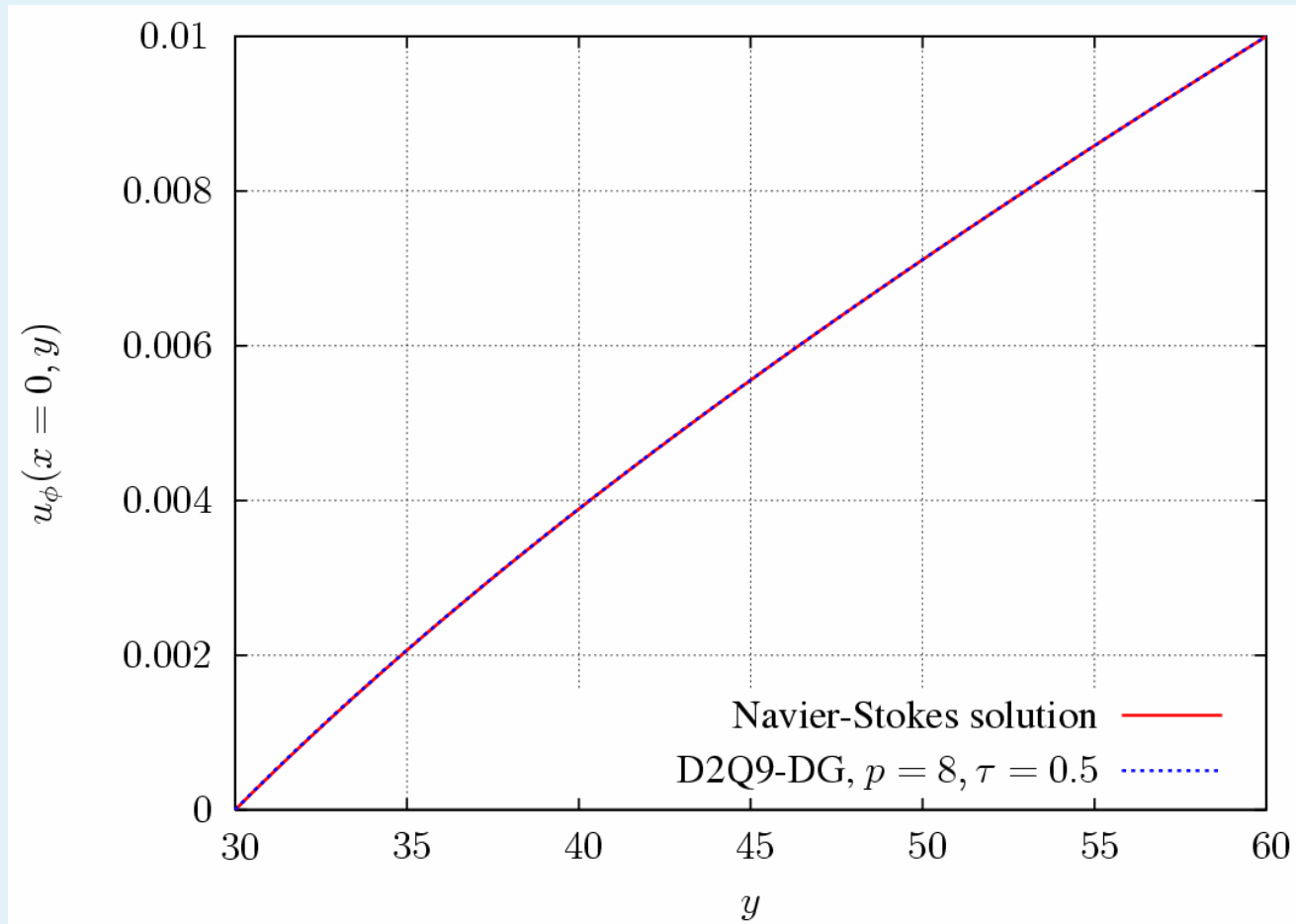
## Rotating Couette flow

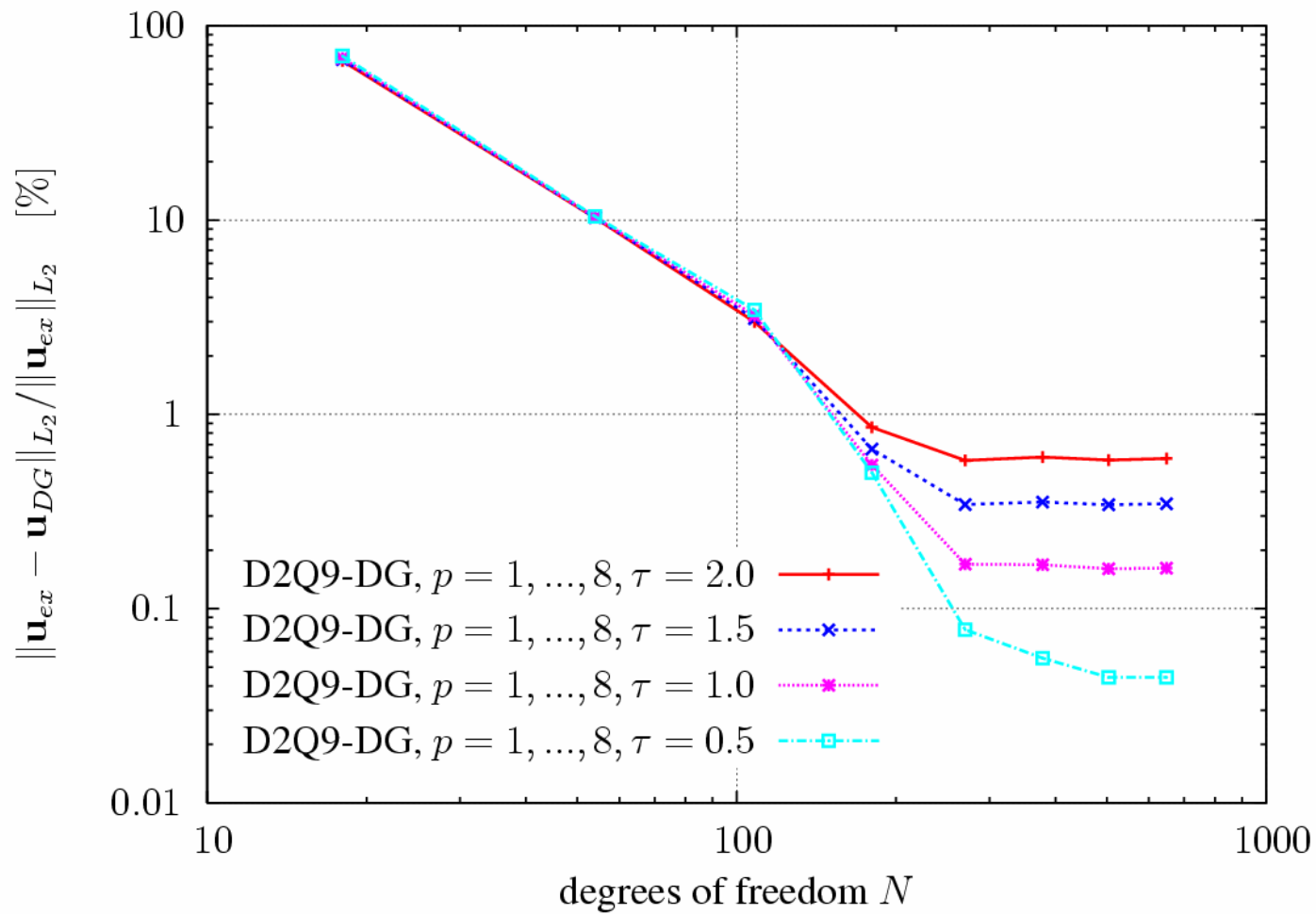
### Navier-Stokes solution



$$u_{\phi}(r) = \frac{1}{R_o^2 - R_i^2} \left( (\Omega_o R_o^2 - \Omega_i R_i^2) r + (\Omega_i - \Omega_o) \frac{R_i^2 R_o^2}{r} \right)$$

Comparison Navier-Stokes / D2Q9-DG,  $p=8$ ,  $\tau=2.0$ 

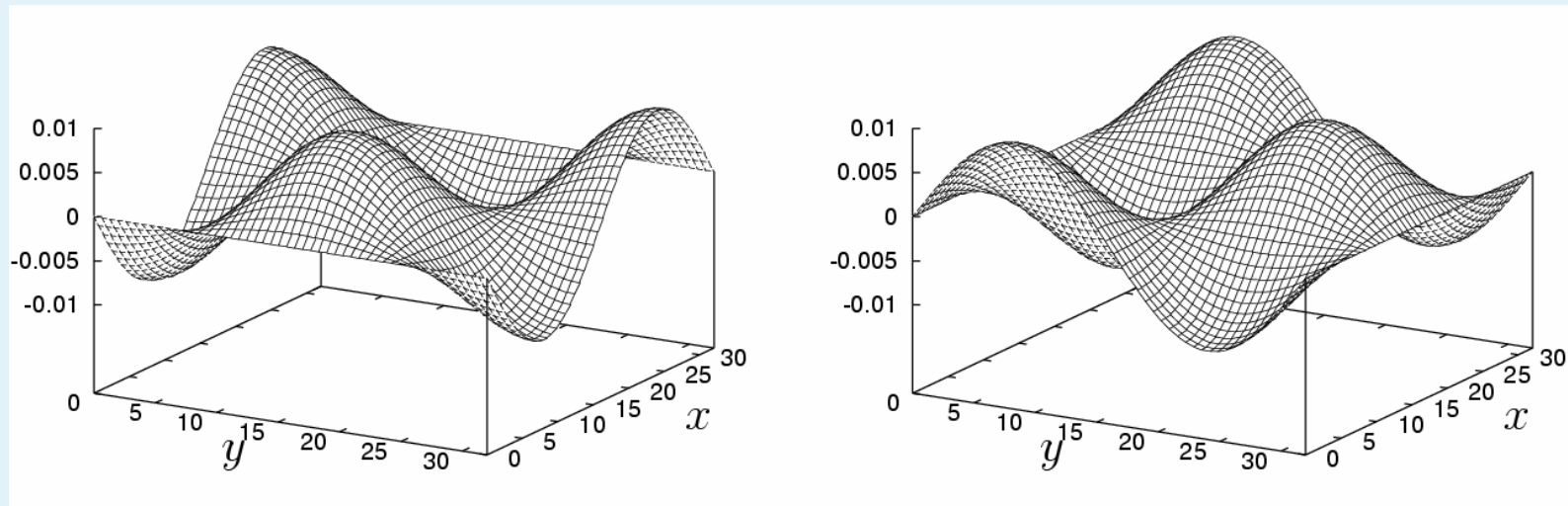
Comparison Navier-Stokes / D2Q9-DG,  $p=8$ ,  $\tau=0.5$ 



observation:  
model deviation  
with respect to  
Navier-Stokes  
dynamics due  
to finite Kn number

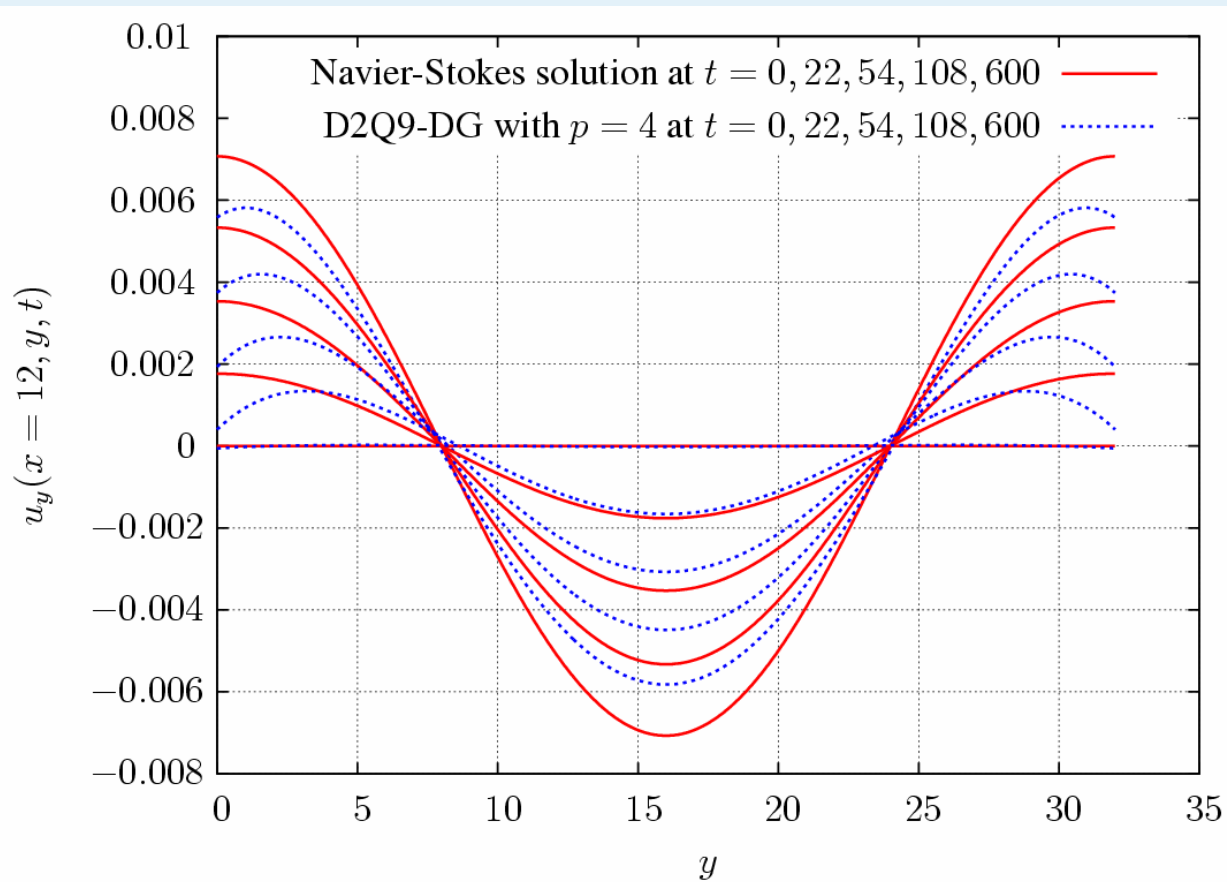


## Taylor vortex flow



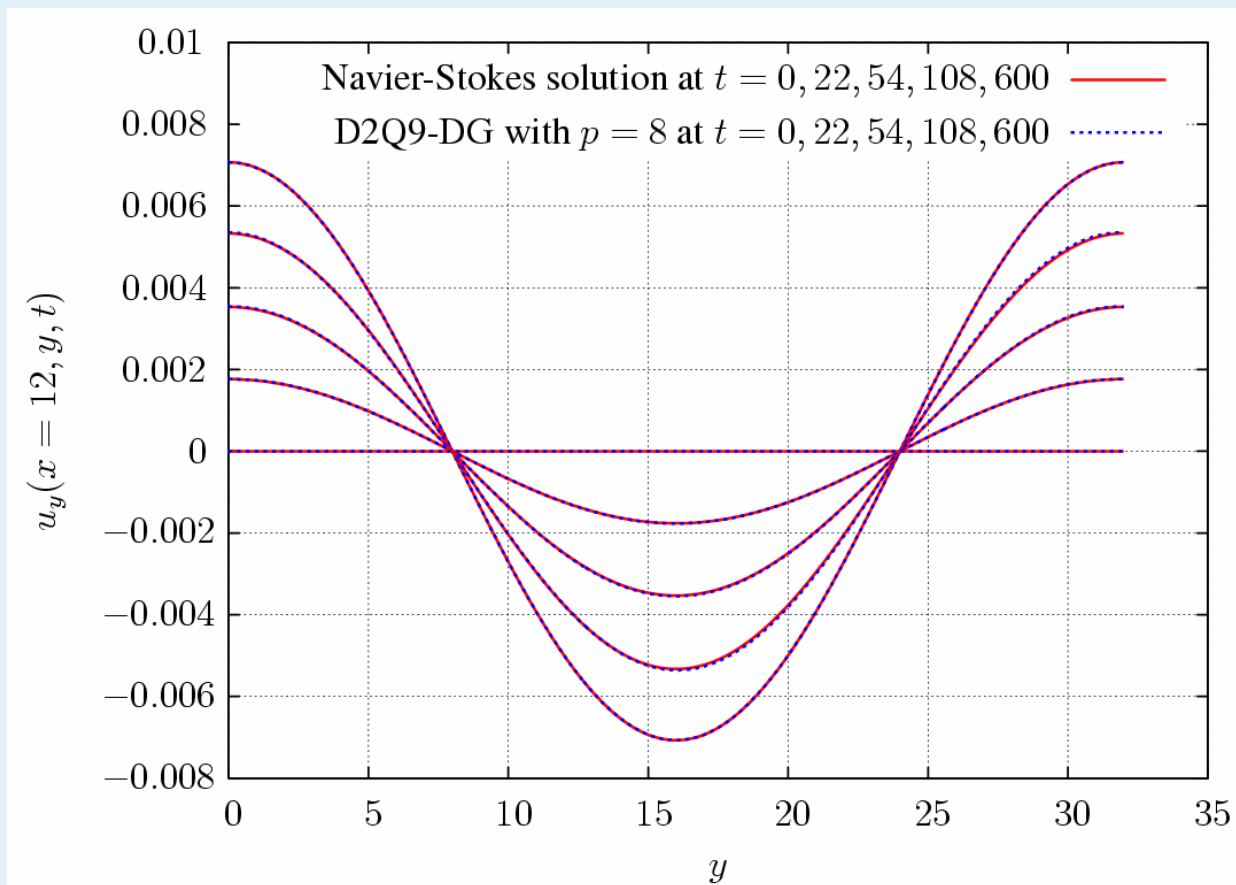
### Navier-Stokes solution

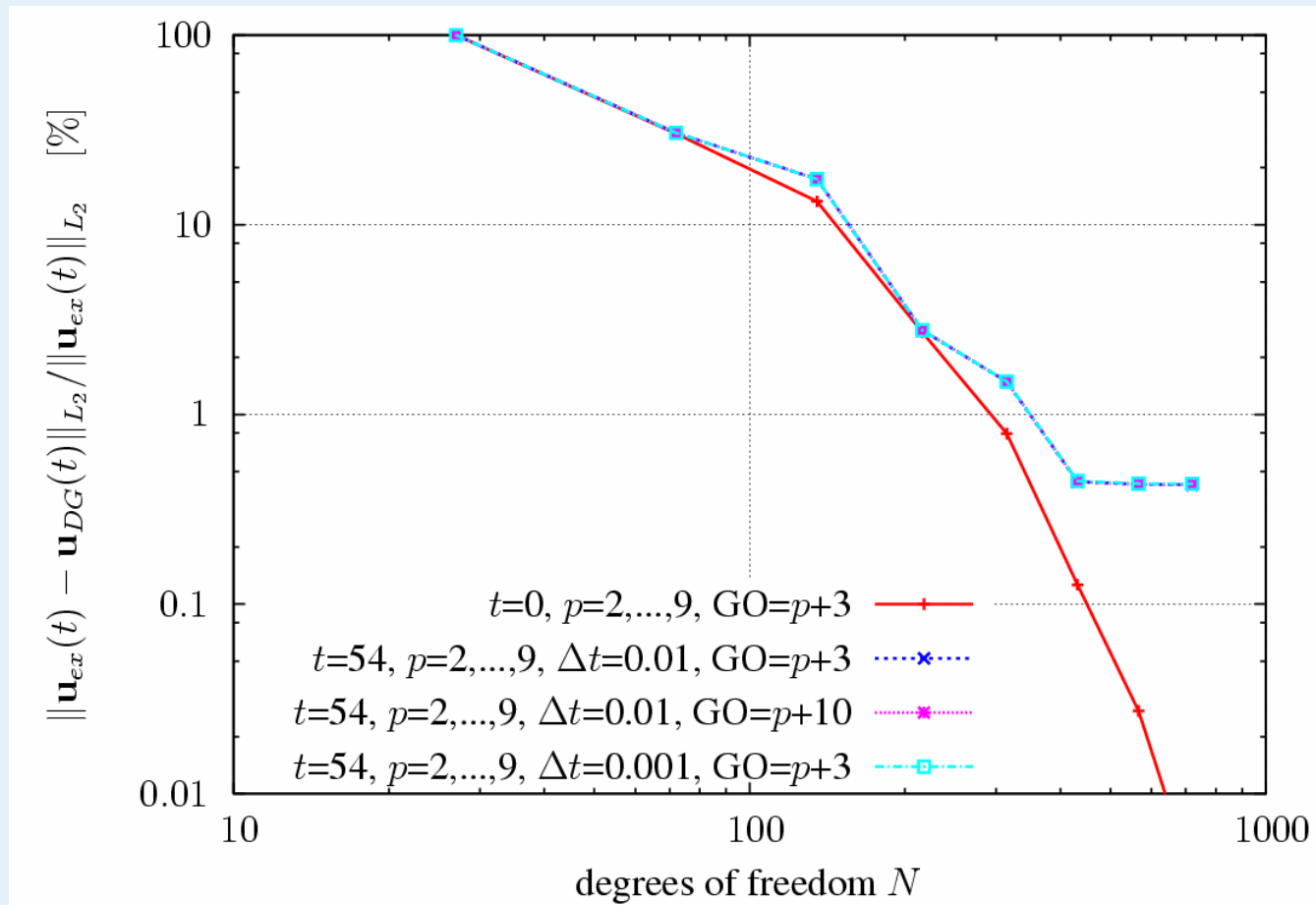
$$\begin{aligned}u_x(x, y, t) &= -u_0 \exp(-\nu t(k_1^2 + k_2^2)) \cos(k_1 x) \sin(k_2 y) \\u_y(x, y, t) &= u_0 k_1/k_2 \exp(-\nu t(k_1^2 + k_2^2)) \sin(k_1 x) \cos(k_2 y)\end{aligned}$$

Comparison Navier-Stokes / D2Q9-DG,  $p=4$ 



## Comparison Navier-Stokes / D2Q9-DG, $p=8$









## conclusions and outlook p-FEM for LB

- exact / accurate representation of curved boundaries
- boundary conditions are defined *on* the boundary
- exponential convergence
- model error (discrete Boltzmann vs Navier-Stokes) can be analyzed (asymptotic behaviour)
- suitable for unstructured grids
  
- to do: higher order time stepping schemes (Runge-Kutta)



# **LB-Methods for multicomponent / multiphase, thermal and turbulent flows**

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## Overview

- **advection-diffusion problems**
  - **grid refinement**
  - **thermal flows**
- **multiphase models**
  - **grid refinement**
- **turbulent flows**
  - **LES**
  - **RANS**
  - **entropic and cascaded LB models**



## A LB extension for advection-diffusion on hierarchical grids

$$\frac{\partial C}{\partial t} + u_j \frac{\partial C}{\partial x_j} = \alpha \frac{\partial^2 C}{\partial x_i \partial x_i}$$

Goal: To develop a numerical scheme for advection-diffusion that works on the same grid as the flow field simulation

⇒ LB methods for advection-diffusion

(e.g. Flekkoy 1993, van der Smaan 1999, Ginzburg 2004)

-efficient (cell Peclet number up to 100)

-inherently mass conservative

-can naturally be extended to hierarchical grids (Stiebler et al. 2006)



## advection-diffusion LB method (Ginzburg 2004)

$$\frac{\partial C}{\partial t} + u_j \frac{\partial C}{\partial x_j} = \alpha \frac{\partial^2 C}{\partial x_i \partial x_i}$$

$$C = \sum_i g_i = \sum_i g_i^{(eq)}, \quad i = 0, \dots, 4$$

LB equation:  $g_i(t + \Delta t, \mathbf{x} + \boldsymbol{\xi}_i \Delta t) = g_i(t, \mathbf{x}) + \lambda (g_i(t, \mathbf{x}) - g_i^{(eq)}(t, \mathbf{x}))$

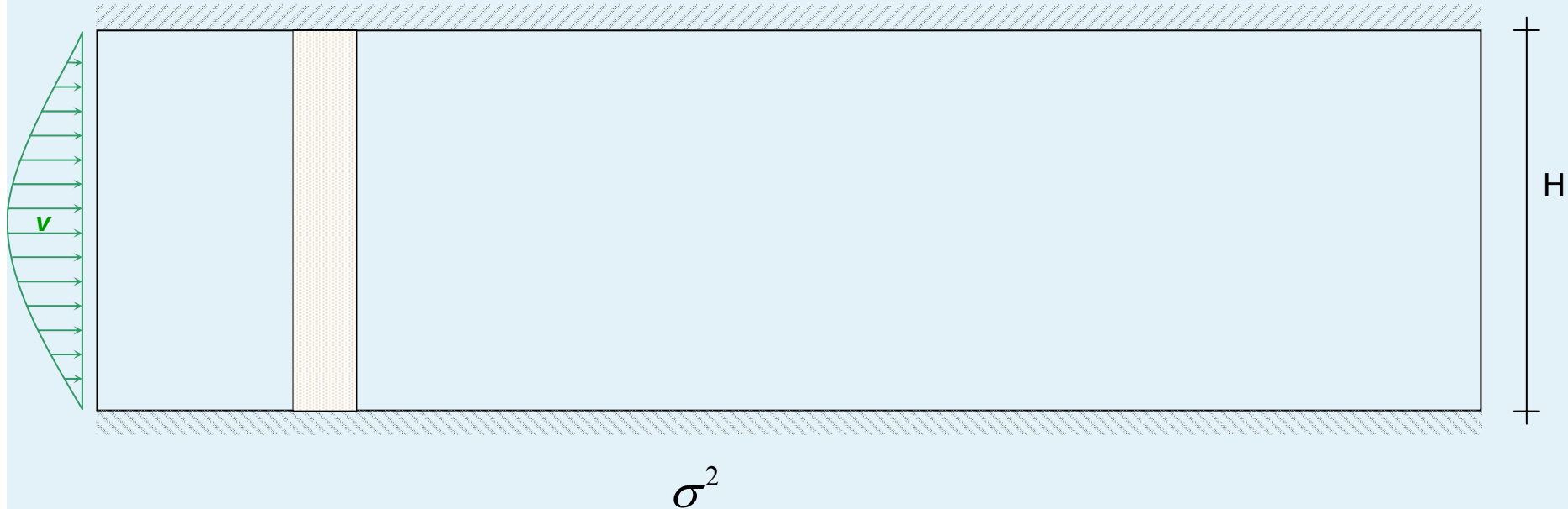
with  $\lambda = -3 + \sqrt{3}$  and equilibrium distributions

$$g_0^{(eq)}(C(\mathbf{x}, t), u(\mathbf{x}, t), a_e(\mathbf{x}, t)) = \frac{C}{3} \left( 1 - 2a_e - 3 \frac{\mathbf{u}^2}{c^2} \right), \quad a_e = \frac{6\sqrt{3}\alpha}{c^2 \Delta t} - 1$$

$$i \neq 0: \quad g_i^{(eq)}(C(\mathbf{x}, t), u(\mathbf{x}, t), a_e(\mathbf{x}, t)) = \frac{C}{6} \left( 1 + a_e + 3 \frac{(\mathbf{u} \cdot \boldsymbol{\xi}_i)^2}{c^4} + 3 \frac{\mathbf{u} \cdot \boldsymbol{\xi}_i}{c^2} \right)$$



## Taylor-Aris-dispersion



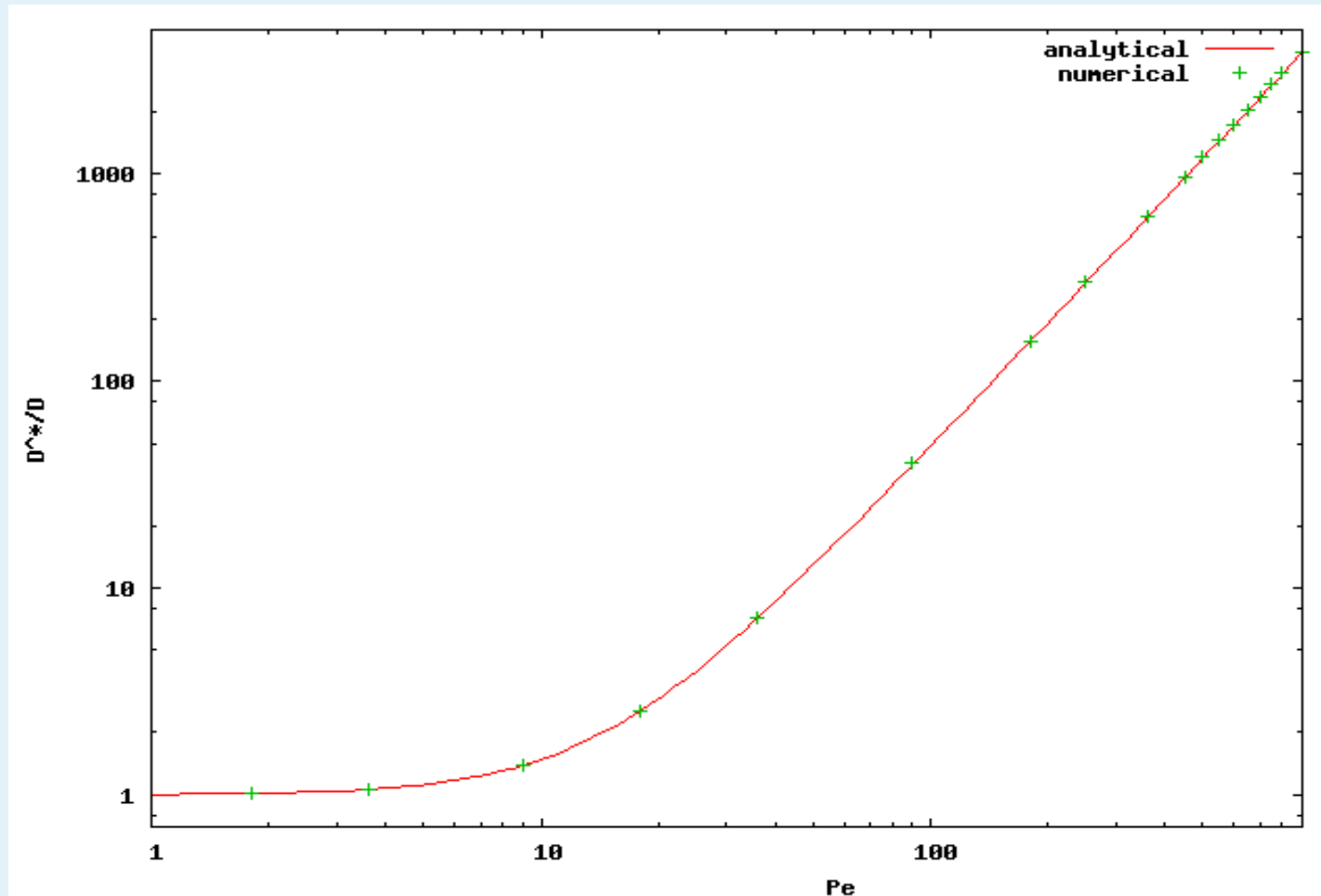
concentration averaged over channel height goes towards a Gaussian density distribution with variance

$$\alpha^* = \frac{1}{2} \frac{d(\sigma^2)}{dt} = \alpha(1 + \text{Pe}^2 / 210), \quad \text{Pe} = \bar{v}H / \alpha$$



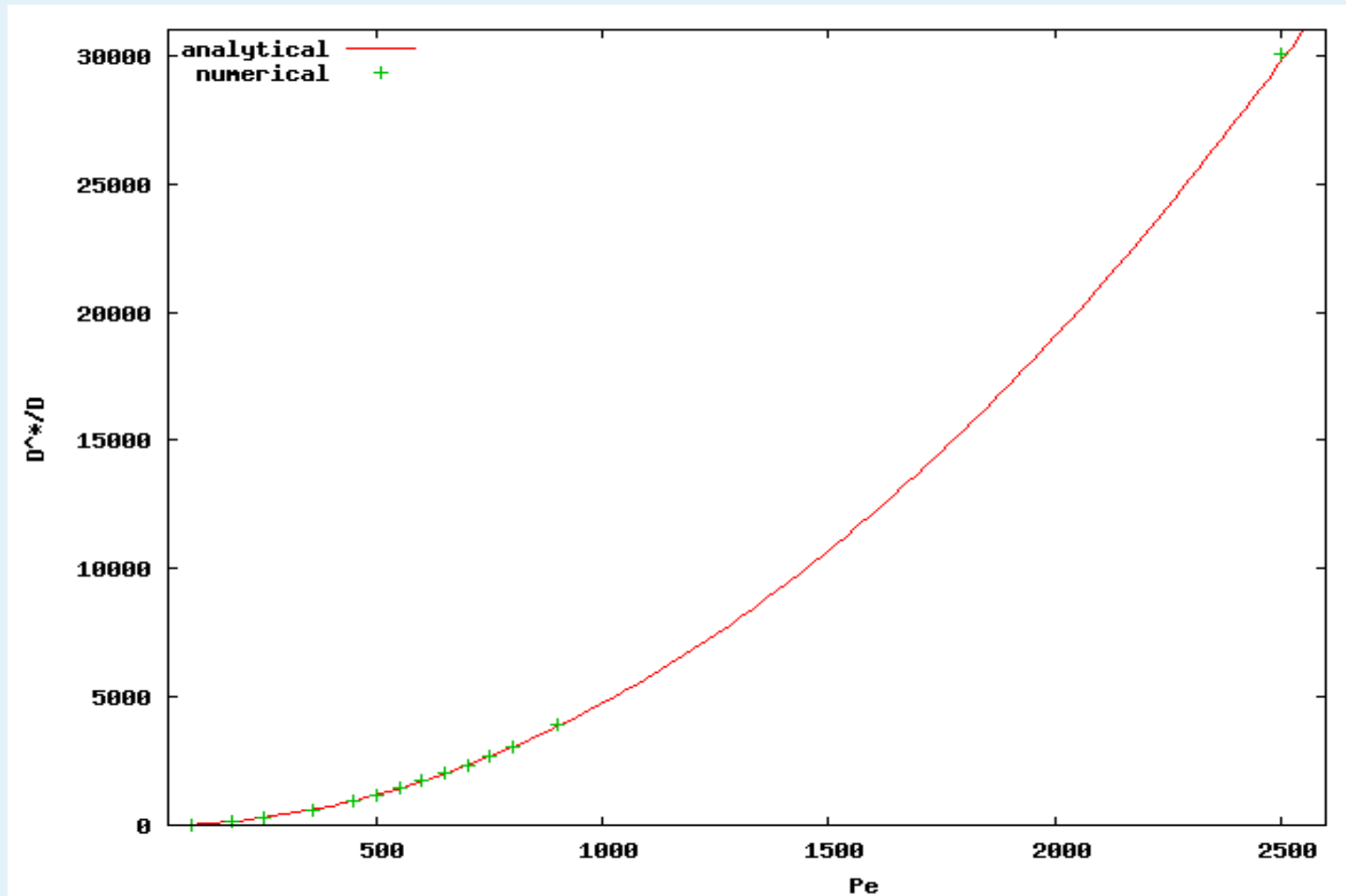


# Taylor-Aris-Dispersion





## Taylor-Aris-Dispersion







## advection diffusion LB method on hierarchical grids

$$g_i(t + \Delta t, \mathbf{x} + \xi_i \Delta t) - g_i(t, \mathbf{x}) = \lambda (g_i(t, \mathbf{x}) - g_i^{(eq)}(t, \mathbf{x}))$$

Taylor series and summation  $\sum_i : \quad \frac{DC}{Dt} = -\left(\frac{\lambda}{2} + 1\right) \sum_i \left( \xi_i \cdot \frac{\partial g_i^{(neq)}}{\partial \mathbf{x}} \right) + O(\Delta t)$

grid invariance of total derivative of transported scalar

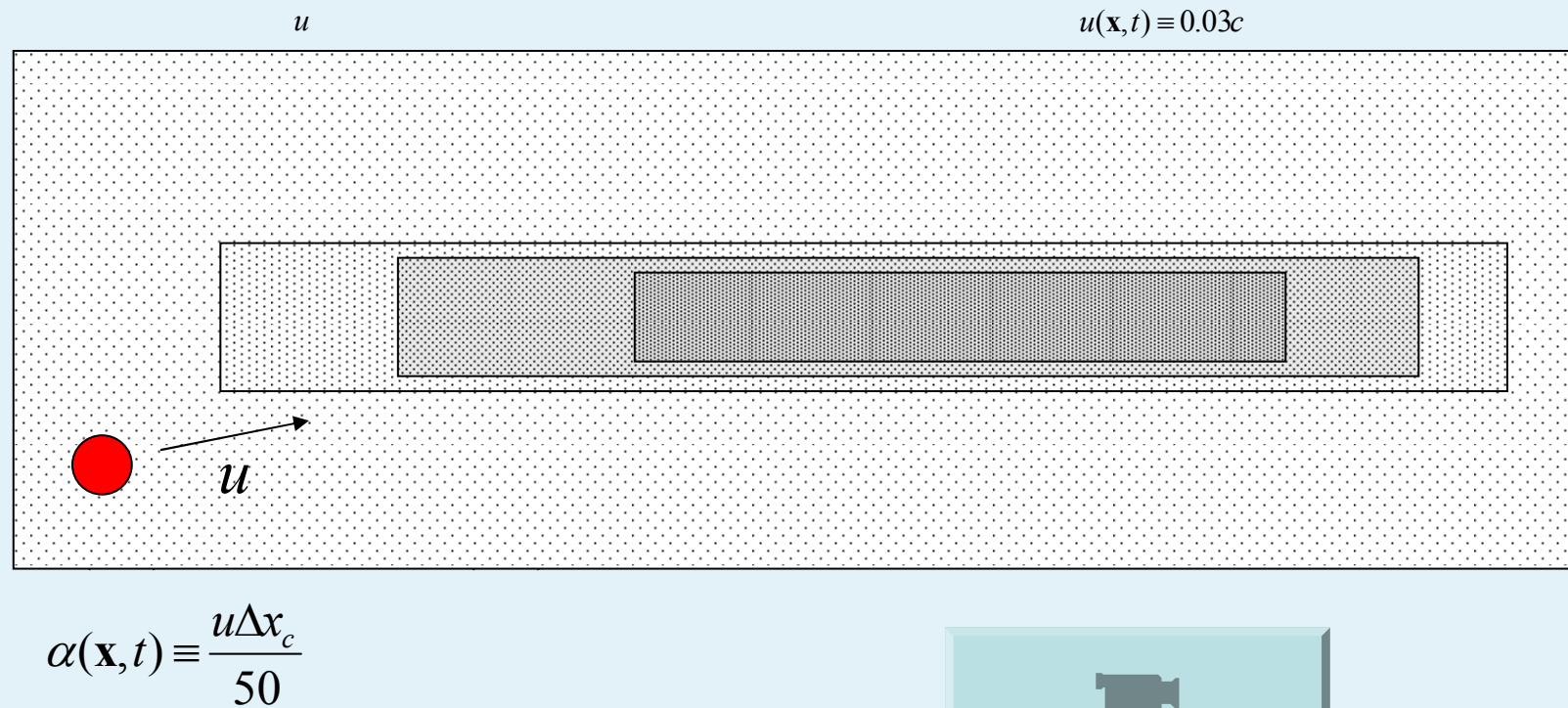


**no** scaling of non-equilibrium parts of distributions

Scaling from fine grid to coarse:  $g_{c,i} = g_i^{(eq)}(C, \mathbf{u}, a_{e,c}) + [g_{f,i} - g_i^{(eq)}(C, \mathbf{u}, a_{e,f})]$

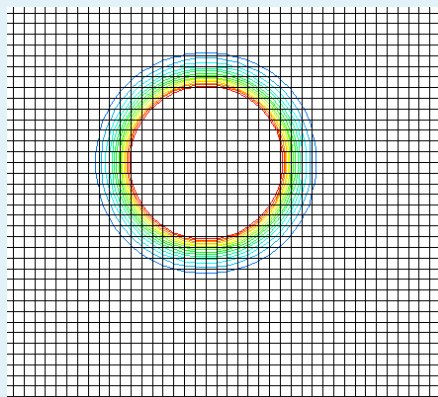
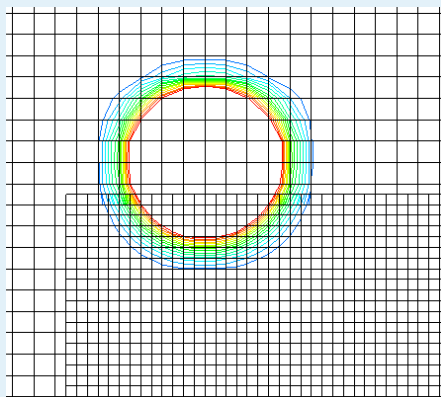


# Test case

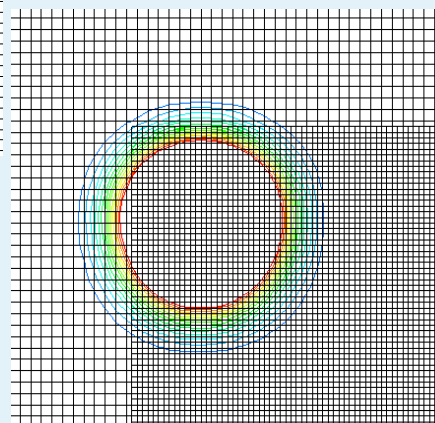




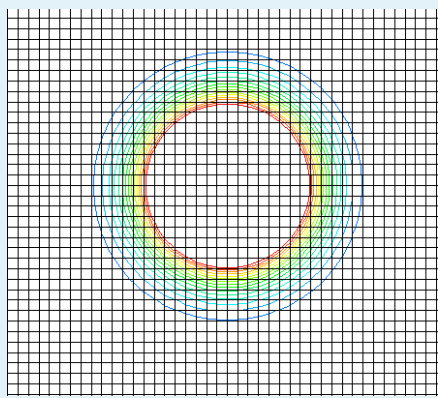
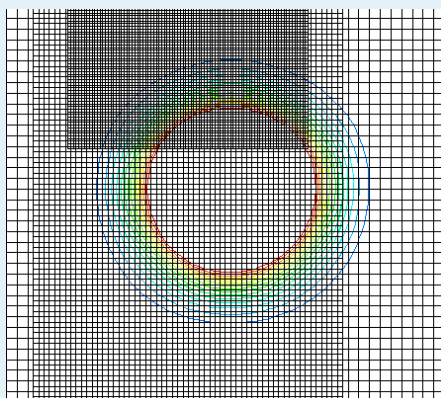
# Test case



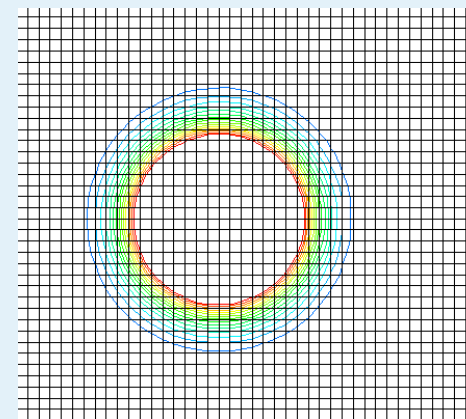
after 30000 time steps



after 60000 time steps

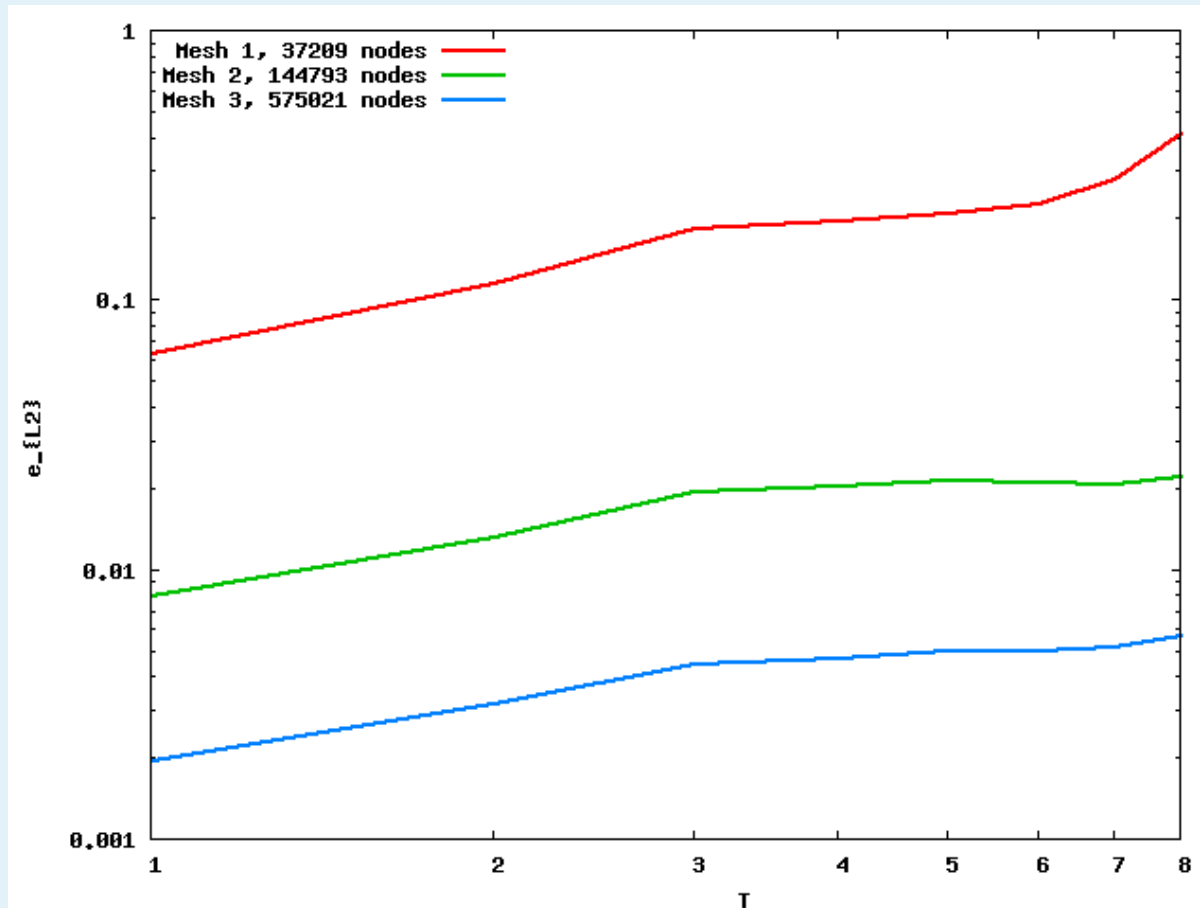


after 90000 time steps





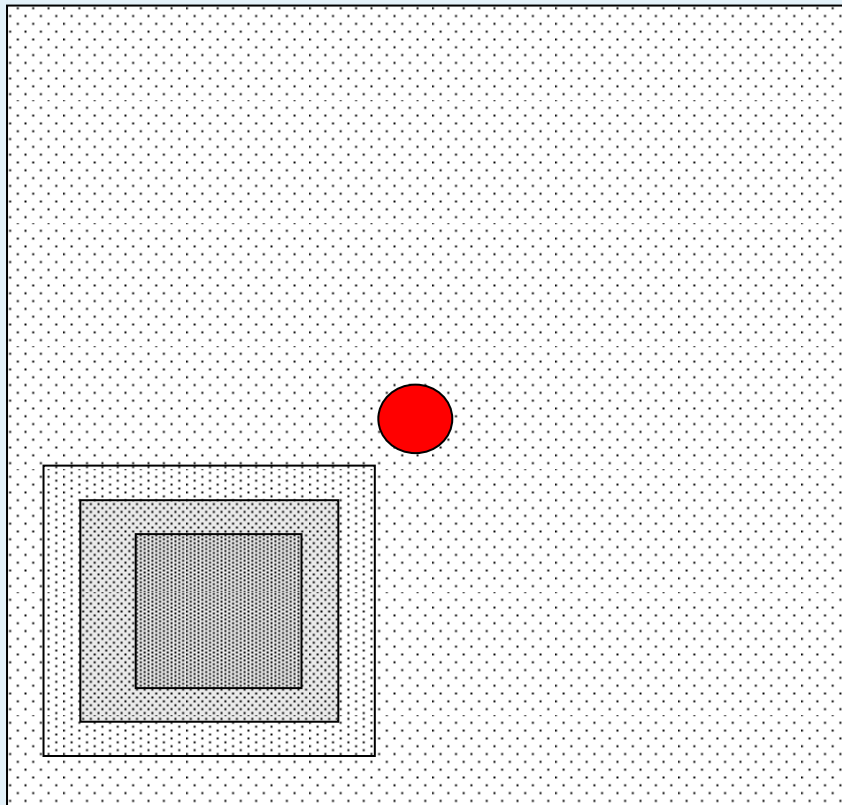
# Test case



L2 error over time for  
non-uniform meshes of  
different resolutions



## Test case: Diffusion without advection

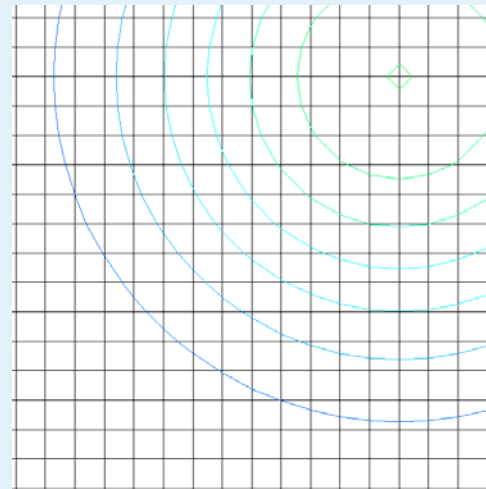
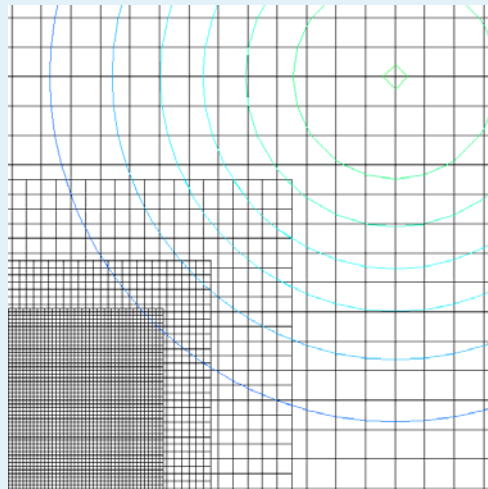


$$\alpha(\mathbf{x}, t) \equiv 0.0064c\Delta x_c$$



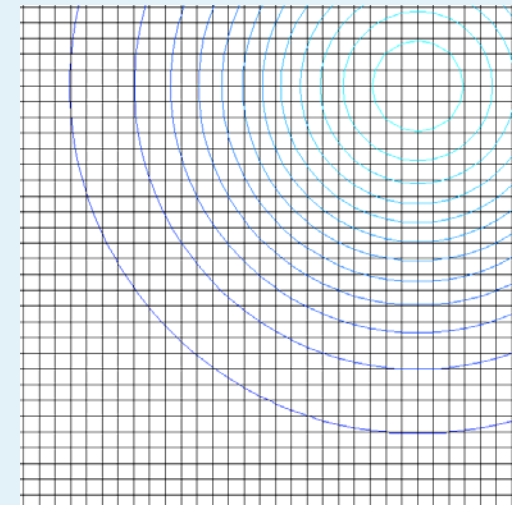
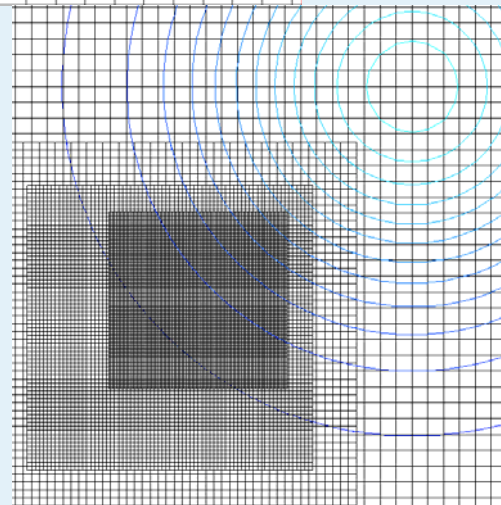


# Test case diffusion without advection



after 6000 time steps

after 12000 time steps





## Thermal flows

One can find four distinct classes of thermal models in the literature:

1. fully compressible models with extended sets of lattice vectors resulting in non-local propagation and difficult boundary conditions (ray tracing, interpolation), e.g. C. Sun, Phys. Rev. E, 61, 2645, 2000
2. Low Ma number models with a large set of discrete velocities
3. Energy dependent discrete velocities
4. hybrid models which solve an additional energy transport equation which is coupled to LB equations in different ways resulting in low Ma number Boussinesq type models usually only valid for small temperature ratios.

$$\frac{c_{\min}^2}{D} < T < \frac{c_{\max}^2}{D}$$



## a compressible thermal low Ma model

Hybrid model

(Tölke 2006)

- Couple speed of sound and temperature
- Correct wrong stresses by additional terms in equilibrium moments (MRT)
- Finite Difference scheme for advection diffusion equation
- non-local collision (next neighbour)

basic idea:

$$c_s^2(\vec{x}, t) \rho(\vec{x}, t) = \frac{\partial P}{\partial \rho} RT(\vec{x}, t) \rho(\vec{x}, t) = T^*(\vec{x}, t) \rho(\vec{x}, t)$$

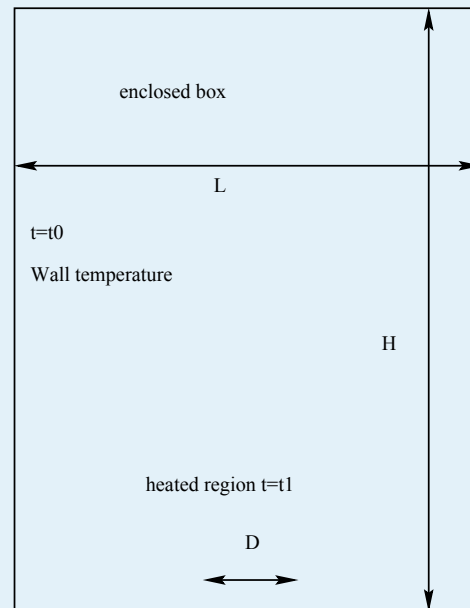
$$p = p_{therm} + p_{hydro} = \underbrace{\rho_1(\vec{x}, t) T^*(\vec{x}, t)}_{\cong const.} + \underbrace{\Delta \rho(\vec{x}, t) T^*(\vec{x}, t)}_{\text{fluctuation}}$$





- Validation for several analytical compressible low Ma problems successful
- density ratios up to 50 achievable
- stability comparable to athermal MRT when energy equation FD stability is provided

numerical example (301x201 nodes):



$$Re \cong 2000$$

$$Ra = \frac{gD^3 \Delta t}{\alpha_0 \nu t_0} \cong 300.000$$

$$Pr = \frac{\nu}{\alpha_0} = 1$$

$$\frac{t_1}{t_0} = 4$$



## Low-Mach number Approximation (LMNA):

energy transport equation

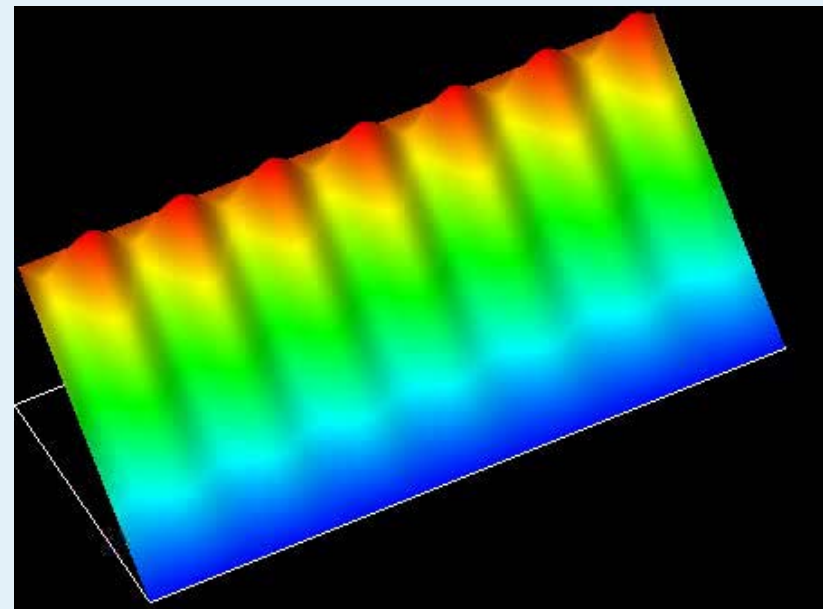
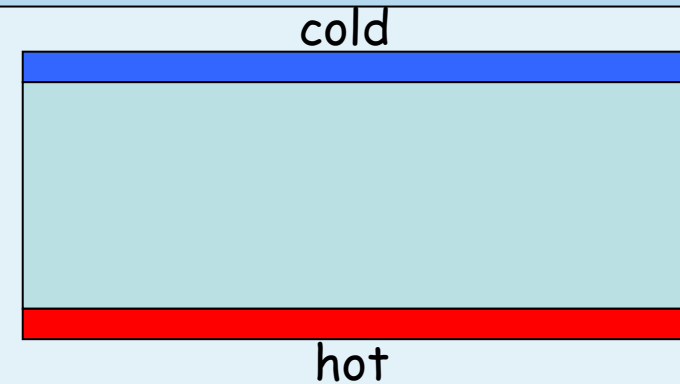
$$\frac{\partial T}{\partial t} + \frac{T \rho \vec{u}}{T_0 \rho_0} \vec{\nabla} T = \frac{T}{T_0 \rho_0} \vec{\nabla} \chi \rho \vec{\nabla} T$$

extension of LBGK-equilibrium distributions

$f = f(p, u, T)$  (Filippova 2000)

allows to simulate thermal flows.

Rayleigh-Benard instability  
( $Ra=1.000.000$ ,  $400 \times 200$  nodes)





## Multi-phase LB models

Numerical simulations of multiphase flows are either based on the surface tracking method, where the interface is modeled explicitly or on a surface capturing method, where the interface is handled implicitly by using a phase field or an index function.

Surface capturing methods are very convenient for handling topological changes. Two examples are the volume of fluid method [10,29] and the level set method. In addition, a coupled version of the volume of fluid and level set method have been developed.

All published LB multiphase models belong to the class of interface capturing schemes. The most prominent models are the Shan-Chen model (1994), Swift's free energy model (1995/96) and the Rothman-Keller LG-approach (1988) and its LB-variant (Gunstensen 1991).

## Extension to multiphase flows (Gunstensen '92)

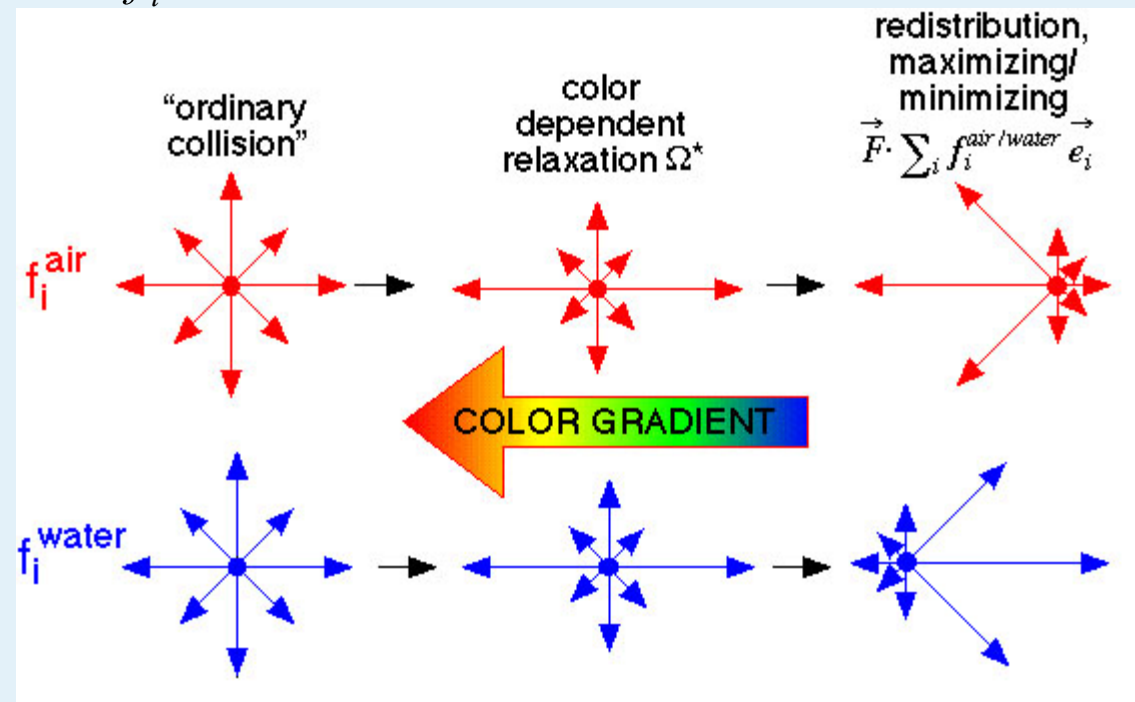
- use two sets of distributions  $f_i^{air}$  and  $f_i^{water}$
- The collision operator of each phase consists of two parts

$$\Omega = \Omega^{(1)} + \Omega^{(2)}$$

$$\Omega^{(2)} = \frac{A_k}{2} |\vec{F}| \left[ \frac{(\vec{e}_i \vec{F})^2}{|\vec{F}|^2} - \frac{1}{2} \right]$$

and a 'color' gradient

$$\vec{F}(\vec{x}) = \sum_i \vec{e}_i \left[ \rho^{air}(\vec{x} + \vec{e}_i) - \rho^{water}(\vec{x} + \vec{e}_i) \right]$$





## Model validation:

- Laplace law (surface tension)
- contact angle (wetting)
- capillary tube (wetting)
- bubble flows (dynamics)



Surface tension can be approximately computed (D3Q19):

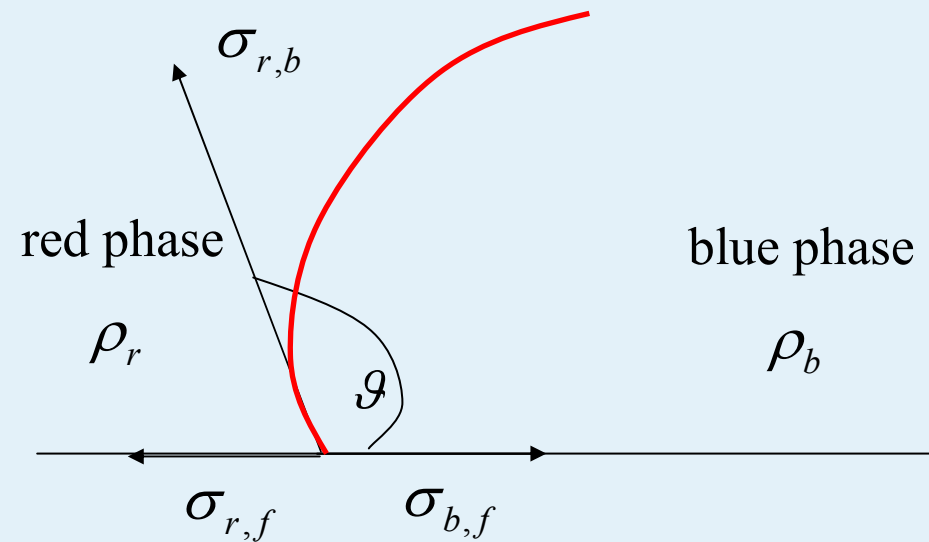
$$\sigma_{a,b} \cong 120A\tau(\rho_a + \rho_b)$$

Laplace law:  $\sigma = \frac{\Delta p}{\kappa} = \frac{\Delta p R}{2}$  for a sphere

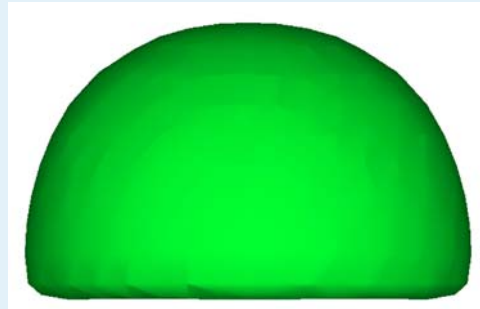
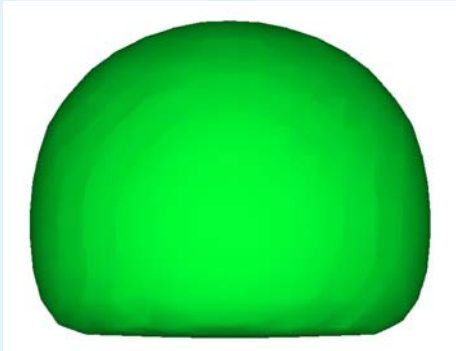
sphere resolution:  
18 nodes

| $\rho_a$ | $\rho_b$ | A    | $\sigma_{theory}$ | $\sigma_{test}$ | rel. error |
|----------|----------|------|-------------------|-----------------|------------|
| 1.0      | 1.0      | 1E-4 | 0.024             | 0.024           | 0.00       |
| 1.0      | 1.0      | 4E-4 | 0.096             | 0.097           | 0.01       |
| 1.0      | 1.0      | 1E-3 | 0.240             | 0.277           | 0.15       |
| 10.0     | 1.0      | 1E-4 | 0.132             | 0.131           | 0.01       |
| 0.125    | 8.0      | 1E-5 | 0.01              | 0.009           | 0.1        |

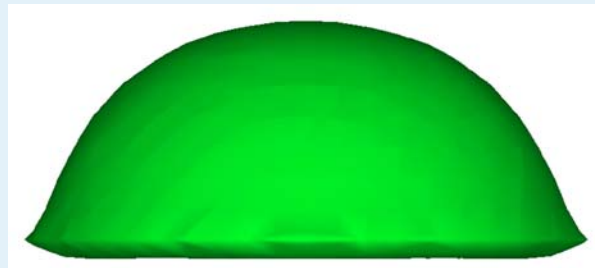
## Contact angle:



Youngs equation:  $\sigma_{r,f} - \sigma_{b,f} - \sigma_{r,b} \cos \vartheta = 0$



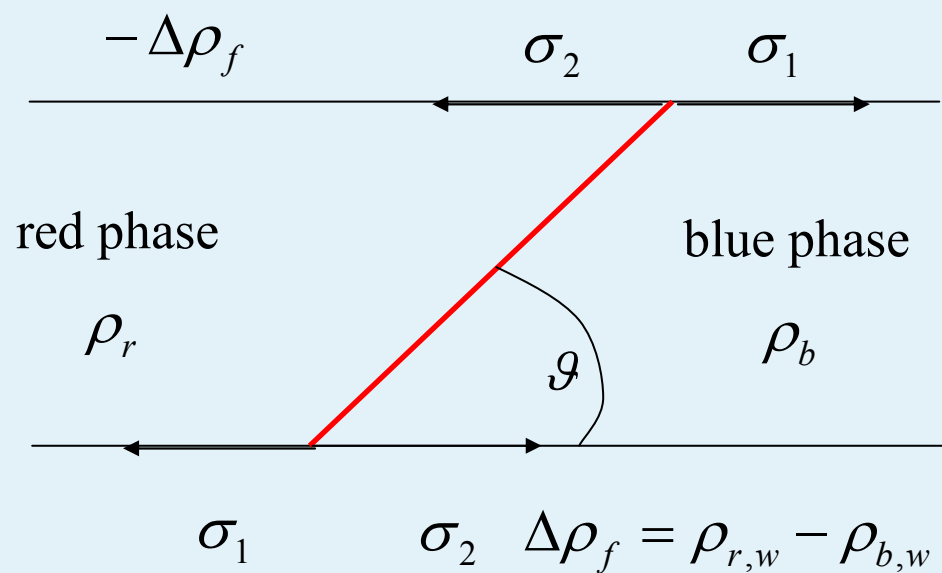
varying contact angles







## channel test (11 nodes vertical)



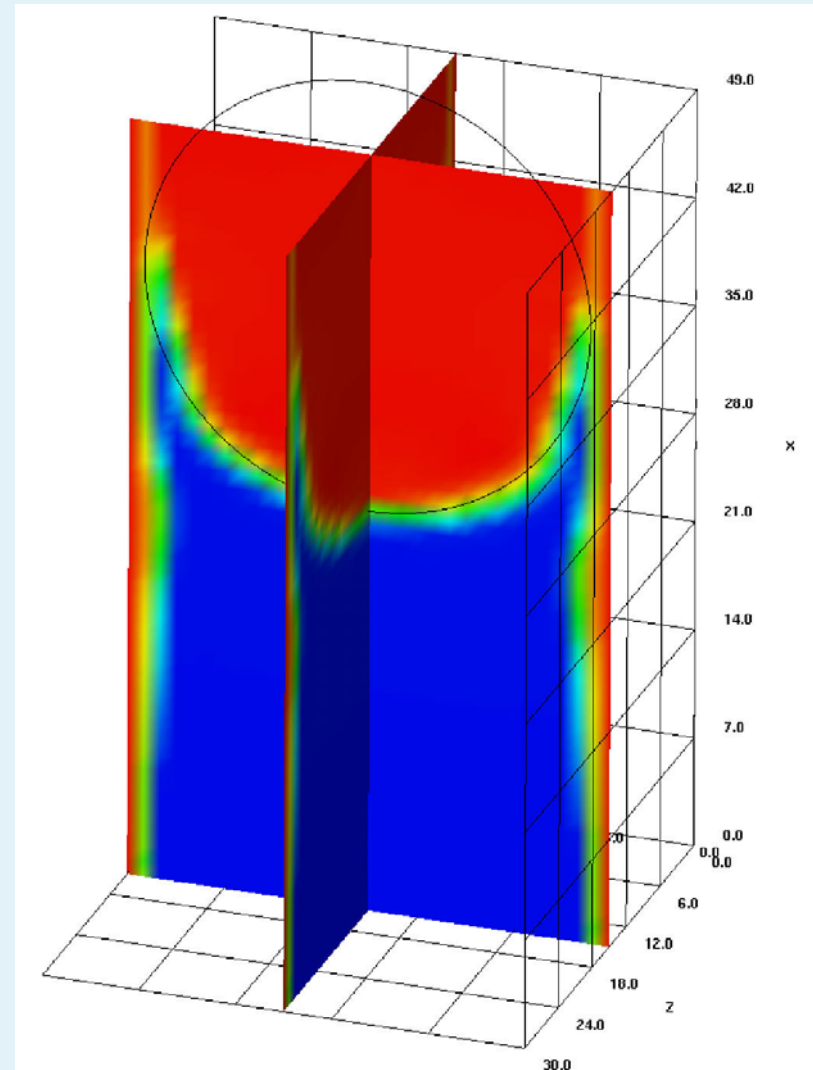
| $\rho_{r,w}$ | $\rho_{b,w}$ | $\Delta\rho_f$ | $\vartheta_{theory}$ | $\vartheta_{num}$ |
|--------------|--------------|----------------|----------------------|-------------------|
| 1.1          | 0.9          | 0.2            | 78°                  | 73°               |
| 1.2          | 0.8          | 0.4            | 66°                  | 62°               |
| 1.3          | 0.7          | 0.6            | 53°                  | 50°               |
| 1.4          | 0.6          | 0.8            | 37°                  | 33°               |



## capillary tube test

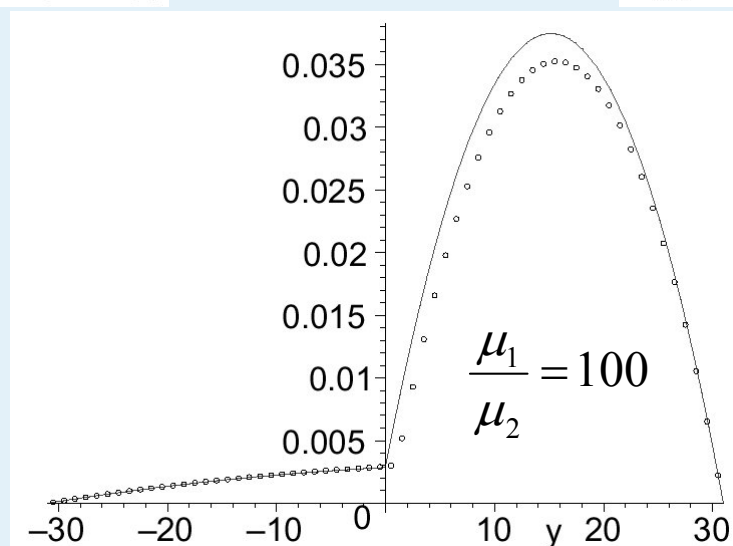
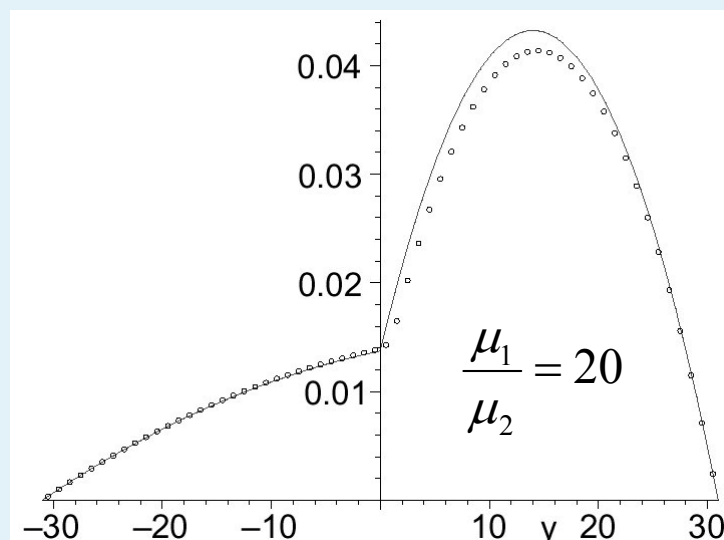
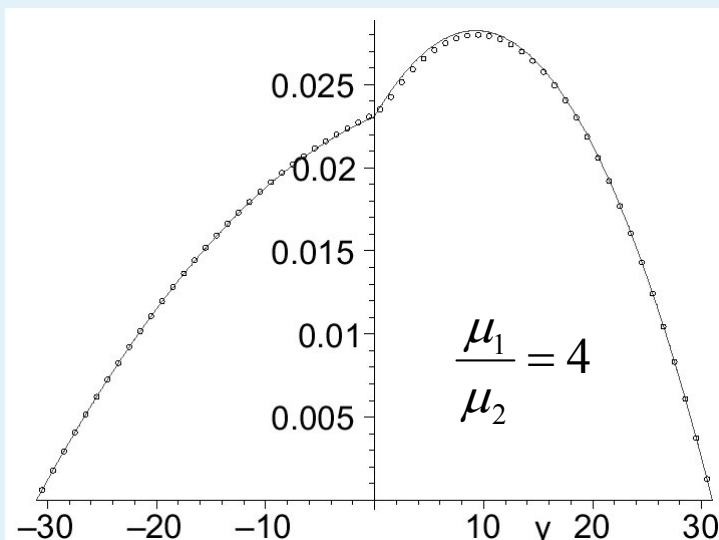
equilibrium between surface  
tension and gravity forces  
implies

$$h = \frac{2\sigma \cos(\gamma)}{r\rho g}$$





channel test  
(two-phase  
Poiseuille flow)



## implementation of a new extension of the Rothmann-Keller<sup>[1]</sup> model

[1] (Gunstensen (Rothmann-Keller), 1991)

### differences compared to one phase models:

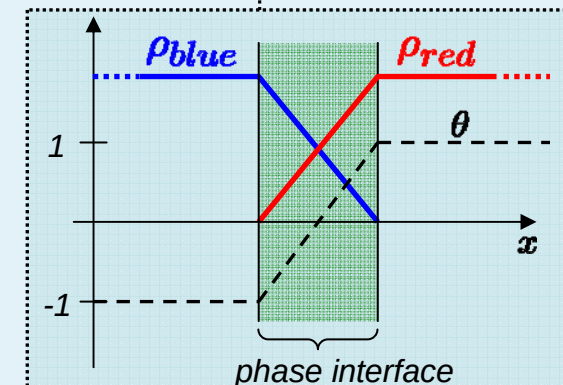
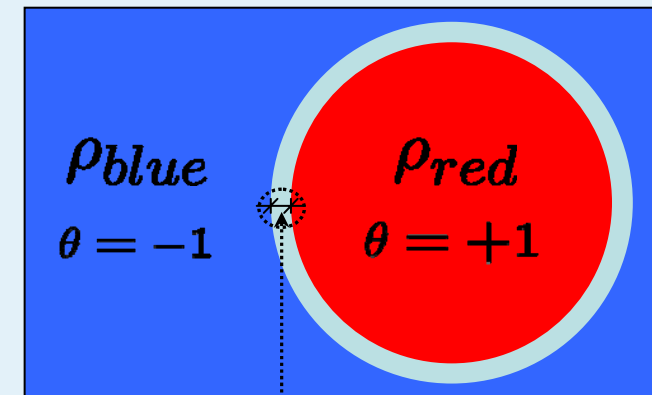
- two phases (red/blue)
- generation of surface tension (!capillary forces!)
- separation of phases (!immiscible!)

### multi phase extensions:

Lattice Boltzmann nodal information:

- **one** set of distributions

- phase parameter  $\theta = \frac{\rho_{red} - \rho_{blue}}{\underbrace{\rho_{red} + \rho_{blue}}_{\rho_{\theta}}} \in [-1; +1]$





## implementation of a new extension of the Rothmann-Keller model

surface tension: (Kehrwald, 2004 PhD, Tölke et. al., 2005)

$$m_i^{eq,l} = m_i^{eq,l} + m_i^{ST,l}$$

$$m_1^{ST,l} = -2\sigma |\vec{C}_l| (n_{l,x}^2 + n_{l,y}^2 + n_{l,z}^2)$$

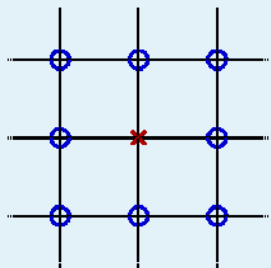
$$m_9^{ST,l} = -\sigma |\vec{C}_l| (2n_{l,x}^2 - n_{l,y}^2 - n_{l,z}^2)$$

$$m_{11}^{ST,l} = -\sigma |\vec{C}_l| (n_{l,y}^2 - n_{l,z}^2)$$

$$m_{13}^{ST,l} = -\sigma |\vec{C}_l| (n_{l,x} n_{l,y})$$

$$m_{14}^{ST,l} = -\sigma |\vec{C}_l| (n_{l,y} n_{l,z})$$

$$m_{15}^{ST,l} = -\sigma |\vec{C}_l| (n_{l,x} n_{l,z})$$



$\sigma$  : surface tension

$\vec{C}_l$  : gradient of phase field

$$\vec{C}_l(t, \vec{x}) = \frac{3}{2c\Delta t} \sum_i w_i \frac{\vec{e}_i}{c} \theta(t, \vec{x} + \vec{e}_i \Delta t_l)$$

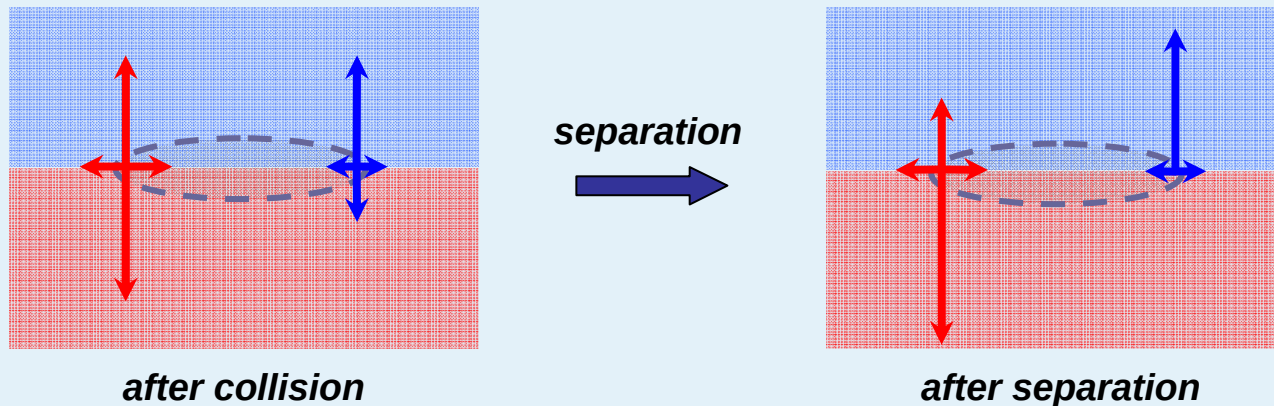
$n_{l,\alpha}$  : vector normal to phase interface  $n_{l,\alpha} = \frac{C_{l,\alpha}}{|\vec{C}_l|}$

## implementation of a new extension of the Rothmann Keller model

separation: (algorithm of Toelke et. al., 2001)

$$\max \vec{C} \cdot \vec{j}^p(\text{after separation}) = \max \vec{C} \cdot \sum_i \vec{e}_i f_i^p(\text{after separation})$$

maximum separation of phases by recoloring (optimization problem!)

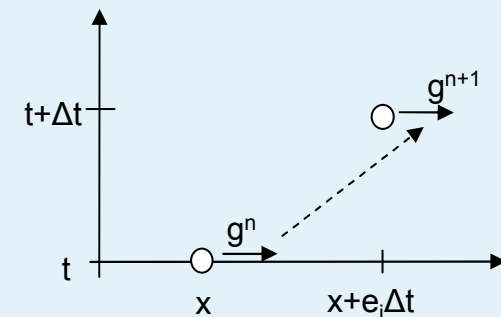


advection of phase field information (additional to the flow field advection):

$$g_{i,l,p}(t + \Delta t_l, \vec{x} + \vec{e}_i \Delta t_l) = g_{i,p}^{eq}(\rho_p(t, \vec{x}), \vec{u}(t, \vec{x}))$$

$$\text{with } g_{i,p}^{eq}(\rho_p(t, \vec{x}), \vec{u}(t, \vec{x})) = w_i \rho_p(t, \vec{x}) \left(1 + \frac{3}{c^2} \vec{e}_i \cdot \vec{u}(t, \vec{x})\right)$$

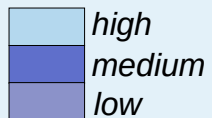
$p = \text{red, blue}$



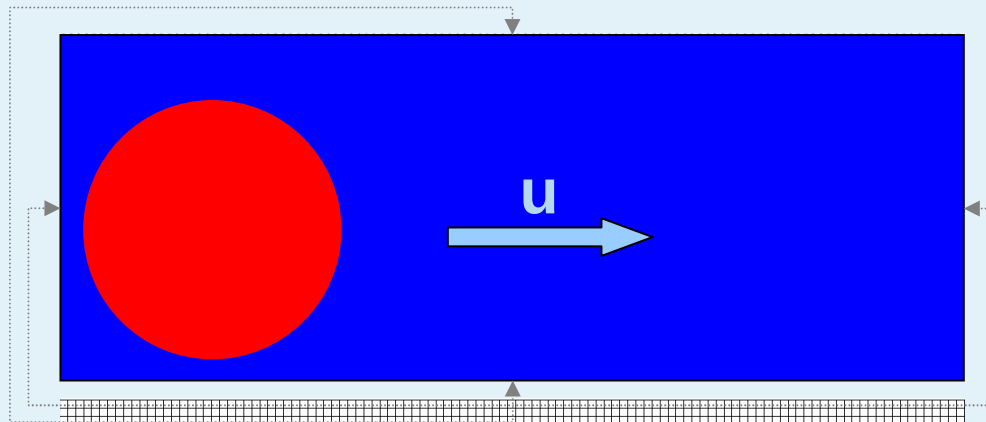
## comparison of refinement types for one and multi phase flow simulations

| grid     | one phase simulation  | multi phase simulation          |                                 |
|----------|-----------------------|---------------------------------|---------------------------------|
|          |                       | calculation                     | computational efficiency        |
| uniform  | <p>solid cylinder</p> | <p>time: 😞</p> <p>result: 😊</p> | <p>time: 😞</p> <p>result: 😞</p> |
| a priori |                       | <p>time: 😊</p> <p>result: 😊</p> | <p>time: 😞</p> <p>result: 😞</p> |
| adaptive |                       | <p>time: 😊</p> <p>result: 👑</p> | <p>time: 😊</p> <p>result: 👑</p> |

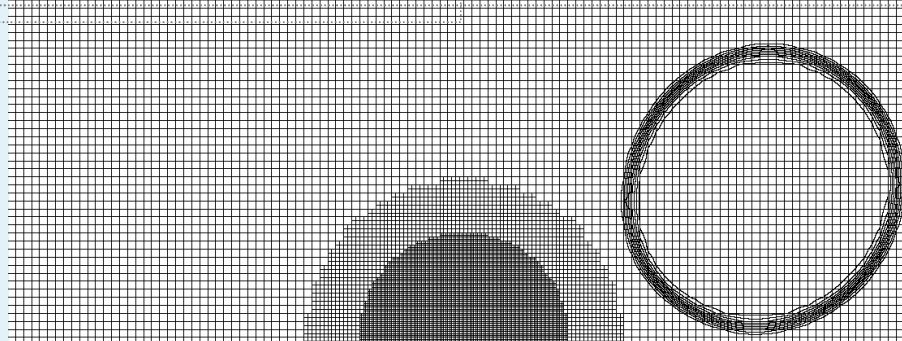
grid resolution:



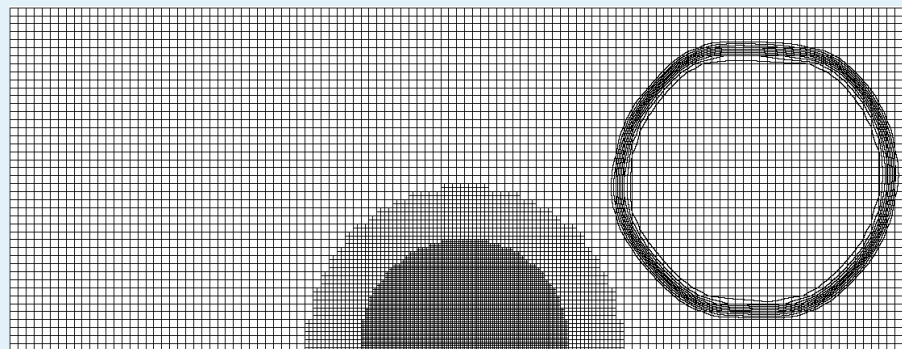
## multiphase simulations on a priori refined grids (phase interface crosses grid interface) I



$$u = 0.05 \text{ m/s}, \sigma = 0.01 \text{ N/m}$$

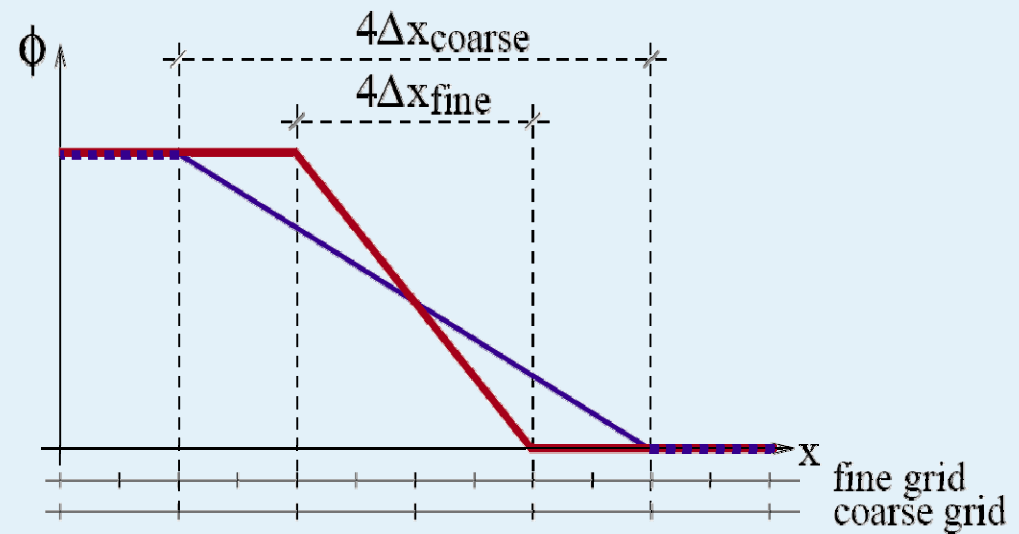
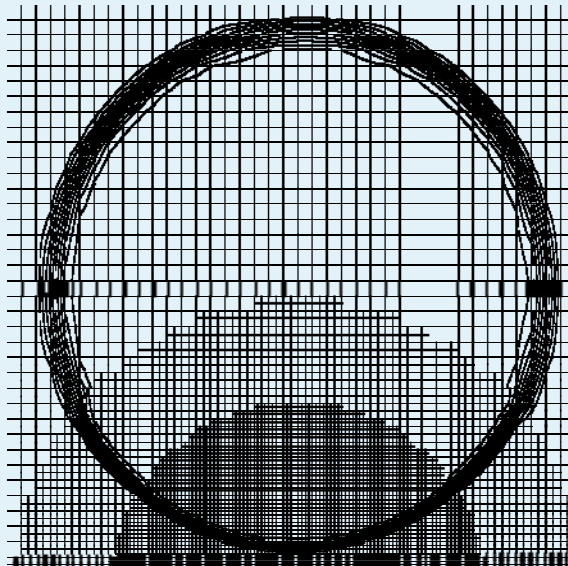


$$u = 0.05 \text{ m/s}, \sigma = 0.1 \text{ N/m}$$



$$u = 0.05 \text{ m/s}, \sigma = 0.00 \text{ N/m}$$





*phase field gradient depends on grid level*



## conclusion I

### **multiphase simulations with phase interface crossing grid levels**

- *possible with limitations*
- *stable parameter range is limited*
- *different width of phase interface on different grid levels*

### **fundamental idea of non uniform grids:**

local resolution of gradients

→ relating to multiphase flow simulations: resolving the phase interface

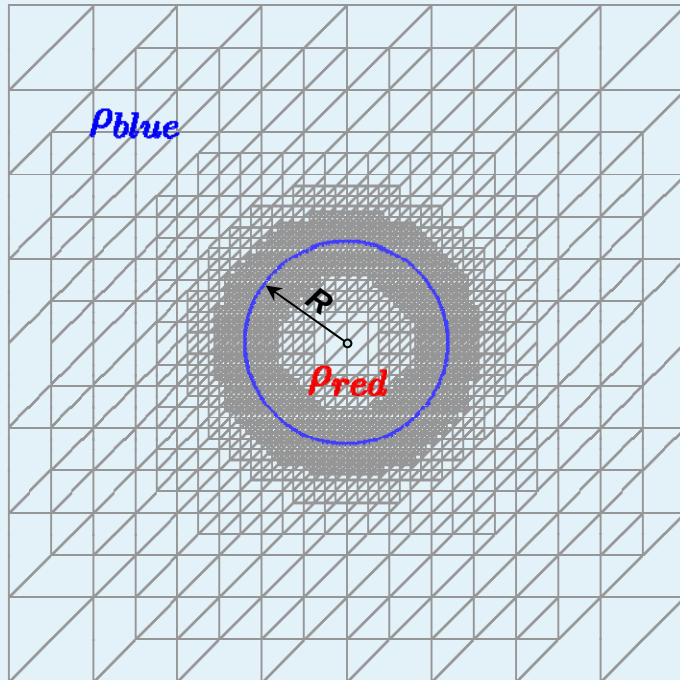
implementation possible at

- *a priori grid refinement?*
- *adaptive grid refinement?*





## validation I – surface tension



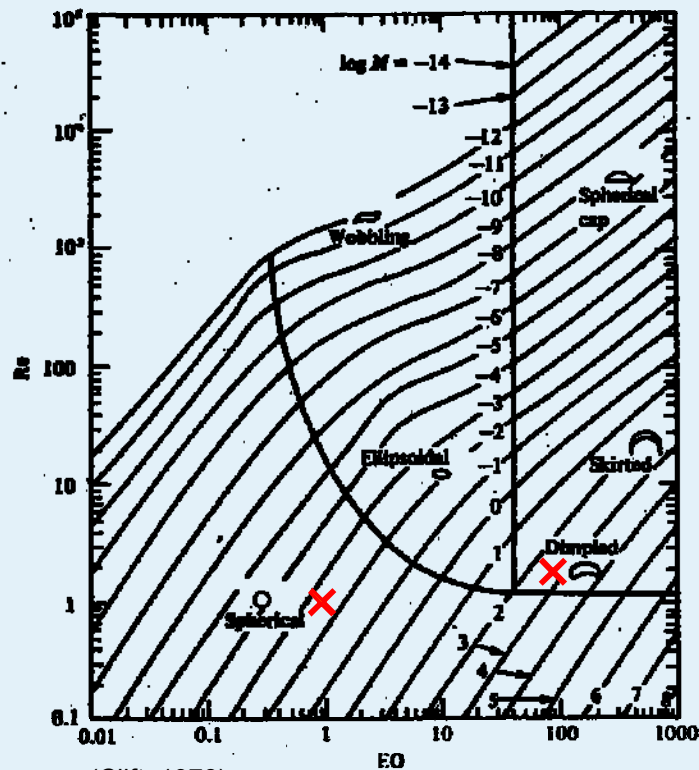
boxed bubble (128x128x128)  
6 level refinement  
 $\vec{v} = 0$

$$\text{Laplace law: } \sigma = \frac{\Delta p R}{2}$$

| $\nu$ | $\rho_b$ | $\rho_r$ | $R$ | $\sigma$ | rel. error |
|-------|----------|----------|-----|----------|------------|
| 0.06  | 1.0      | 1.0      | 19  | 0.1      | $1.0E-5$   |
| 0.06  | 1.0      | 1.0      | 19  | 0.01     | $1.9E-5$   |
| 0.06  | 2.0      | 0.5      | 19  | 0.1      | $1.5E-5$   |
| 0.06  | 2.0      | 0.5      | 19  | 0.01     | $1.3E-5$   |
| 0.25  | 1.0      | 1.0      | 19  | 0.1      | $1.0E-5$   |
| 0.25  | 1.0      | 1.0      | 19  | 0.01     | $2.3E-5$   |
| 0.25  | 2.0      | 0.5      | 19  | 0.1      | $2.1E-5$   |
| 0.25  | 2.0      | 0.5      | 19  | 0.01     | $1.6E-5$   |

*non uniform calculation is ~8 times faster  
than the uniform calculation*

## raising bubble in infinite expanded space - validation II



(Clift, 1978)

Eötvös number  $E_o = \frac{g \Delta \rho d_e^2}{\sigma}$

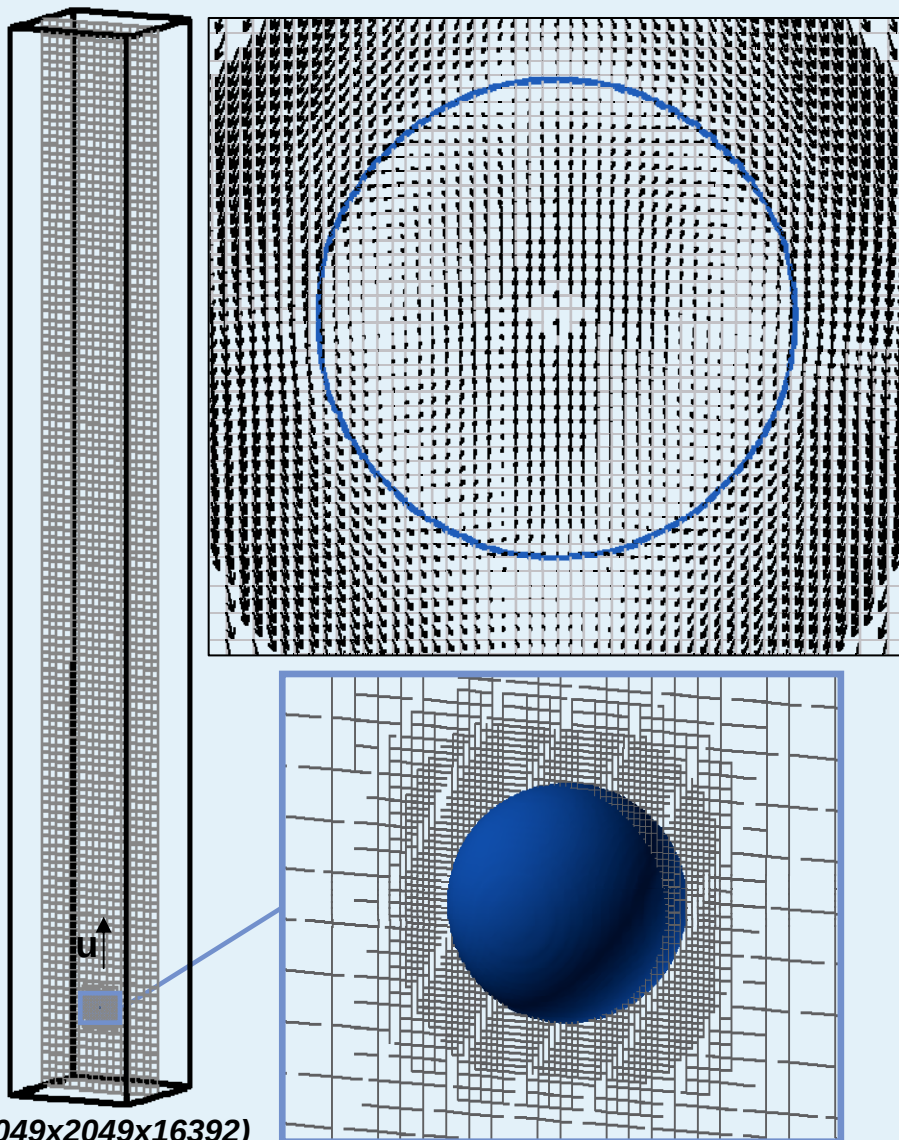
Reynolds number  $Re = \frac{U_T d_e \rho}{\mu}$

Morton number  $M = \frac{g \mu^4 \Delta \rho}{\rho^2 \sigma^3}$

dimpled regime:  $2Re^2 + 6Re^2 \frac{2 + 3\frac{\mu_r}{\mu_b}}{1 + \frac{\mu_r}{\mu_b}} - E_o^{\frac{2}{3}} M^{-\frac{1}{2}} = 0$

spherical regime:  $u = \frac{1}{6} \frac{g d_e^2 \Delta p}{\mu_b} \frac{\frac{\mu_r}{\mu_b} + 1}{3\frac{\mu_r}{\mu_b} + 2}$

## raising bubble (spherical regime) - validation II



| $\rho_b$ | $\rho_r$ | $d$ | $\nu$ | $\sigma$ | $g$       |
|----------|----------|-----|-------|----------|-----------|
| 1.0      | 1.0      | 35  | 0.25  | 0.01     | $2.14E-5$ |

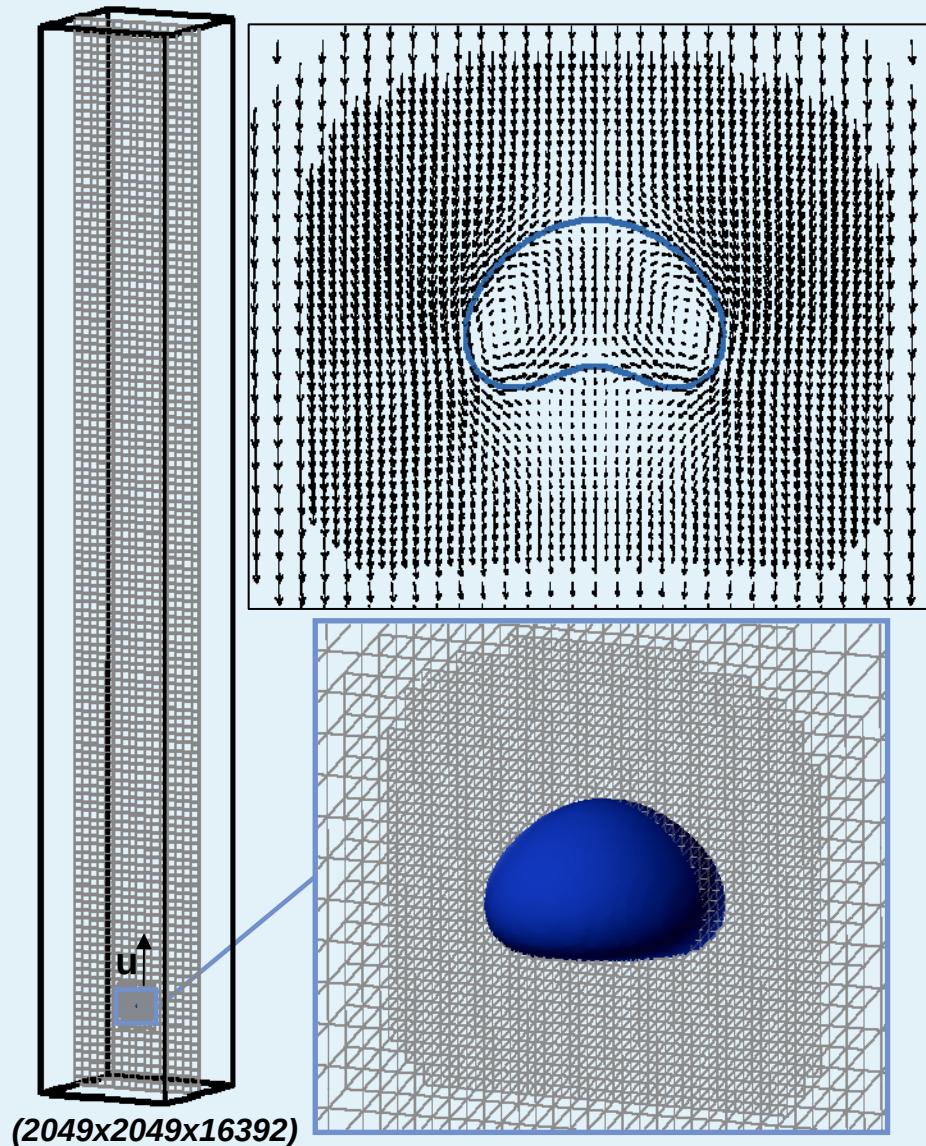
| $Eo$ | $M$   | $Re$ | $u_t$ | $u_{num}$ |
|------|-------|------|-------|-----------|
| 2.63 | 0.083 | 0.98 | 0.007 | 0.006     |

*non uniform calculation is ~5 orders of magnitude  
faster than uniform calculation*

|          | #nodes (*)    | level | #nodes per level | %       |
|----------|---------------|-------|------------------|---------|
| uniform  | $\sim 8.8E12$ | 11    | $6.9E10$         | 100.0 % |
| adaptive | $\sim 1.7E07$ | 11    | 128270           | 68.3 %  |
|          |               | 10    | 11799            | 6.2 %   |
|          |               | 9     | 4237             | 2.2 %   |
|          |               | 8     | 2541             | 1.4 %   |
|          |               | 7     | 1238             | 0.7 %   |
|          |               | 6     | 1181             | 0.7 %   |
|          |               | 5     | 1206             | 0.7 %   |
|          |               | 4     | 37156            | 19.8 %  |

(\*) required node updates for 128 time steps = refinement interval

## raising bubble (dimpled regime) - validation II



| $\rho_b$ | $\rho_r$ | $d$ | $\nu$ | $\sigma$ | $g$       |
|----------|----------|-----|-------|----------|-----------|
| 2.0      | 0.5      | 20  | 0.25  | 0.003    | $1.35E-3$ |

| $Eu$ | $M$ | $Re$ | $u_t$ | $u_{num}$ |
|------|-----|------|-------|-----------|
| 90   | 390 | 2.4  | 0.03  | 0.035     |

*non uniform calculation is ~5 orders of magnitudes faster  
than the uniform calculation*

|          | #nodes (*)    | level | #nodes per level | %       |
|----------|---------------|-------|------------------|---------|
| uniform  | $\sim 8.8E12$ | 11    | $6.9E10$         | 100.0 % |
| adaptive | $\sim 1.3E07$ | 11    | 97013            | 70.0 %  |
|          |               | 10    | 10369            | 7.0 %   |
|          |               | 9     | 3692             | 2.6 %   |
|          |               | 8     | 2249             | 1.6 %   |
|          |               | 7     | 1041             | 0.8 %   |
|          |               | 6     | 964              | 0.7 %   |
|          |               | 5     | 989              | 0.7 %   |
|          |               | 4     | 23309            | 16.6 %  |

(\*) needed node updates for 128 time steps = refinement interval



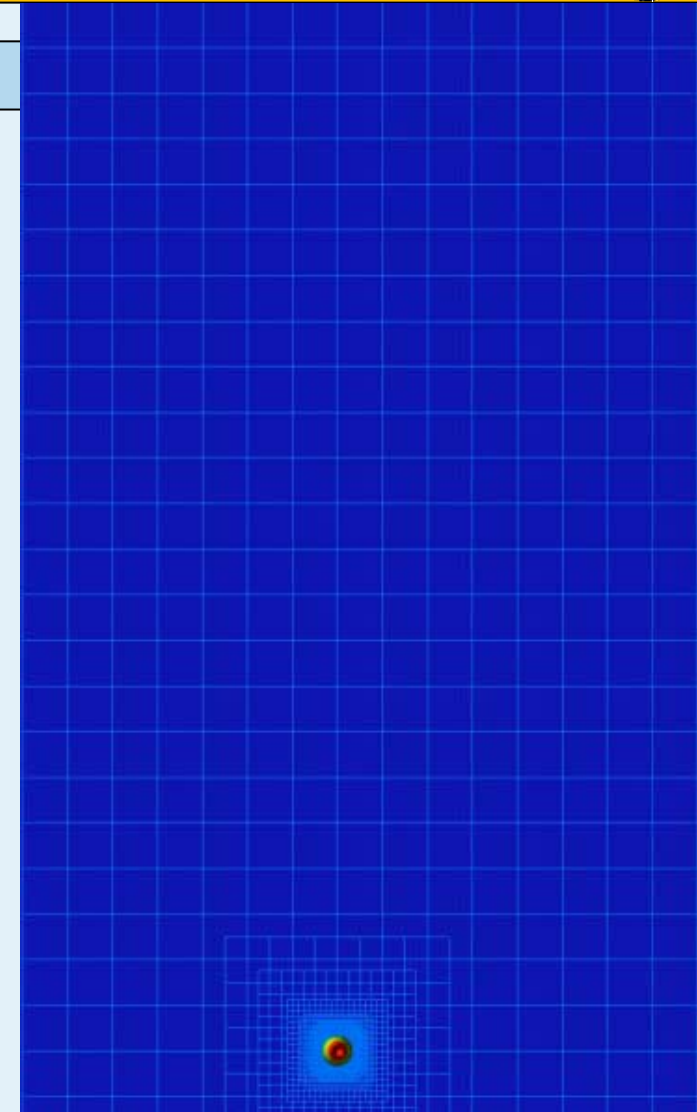


## conclusion II and outlook

- *adaptive grid refinement fulfills fundamental idea for non uniform (multiphase) simulations*
- *encouraging first results*
- *present implementation of mesh refinement is still time-consuming*

### To Do

- *improvement of adaptive algorithms*
- *parallelization of the program for:*
  - *uniform grids*
  - *a priori grids*
  - ***adaptive grids***
- *extending program for other simulation models (e. g. LES, Free Surface)*



*don't try this with uniform grids  
(YES, it is mass conservative)*



## Simulation of turbulent flows

|      | model credibility              | computational effort                | field of application                           |
|------|--------------------------------|-------------------------------------|------------------------------------------------|
| DNS  | no modelling                   | extremely high, all scales resolved | low Re flows                                   |
| LES  | modelling of small scales only | medium and large scales resolved    | often too complex for engineering applications |
| RANS | critical closure assumptions   | low, only mean flow is calculated   | method of choice for engineering applications  |





# Large Eddy Simulation (LES) for LBGK Eggels, 1998 Teixeira, 1998

algebraic approach:

$$\nu = \nu_0 + \nu_T \quad \nu_T \propto l^2 |S_{\alpha\beta}|$$

based on filterwidth / mixing  
length  $l$   
and stress / strain rate tensor  $S$

$S$  is a local quantity !  $S_{\alpha\beta} \propto \sum_i e_{i\alpha} e_{i\beta} (f_i - f_i^{(eq)})$

Smagorinsky:  $\nu_T = (C_s \Delta x)^2 \|\bar{\varepsilon}\| \quad C_s \in \{0.05, 0.2\}$



## Turbulence: RANS and turbulent viscosity

With  $u_i = \underbrace{U_i}_{\text{mean}} + \underbrace{u'_i}_{\text{fluctuating}}$ ,

the Reynolds averaged momentum equation becomes

$$\frac{\partial U_i}{\partial t} + \frac{\partial}{\partial x_j} (U_i U_j + \overline{u'_i u'_j}) = -\frac{\partial p}{\rho \partial x_i} + \nu \frac{\partial}{\partial x_j} \left( \frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right)$$

Using the turbulent-viscosity hypothesis (Boussinesq 1877), we obtain

$$\frac{\partial U_i}{\partial t} + \frac{\partial}{\partial x_j} (U_i U_j) = -\frac{\partial p}{\rho \partial x_i} + (\nu + \nu_T) \frac{\partial}{\partial x_j} \left( \frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right)$$



## Turbulence: two equation models

$$\frac{\partial k}{\partial t} + \frac{\partial(U_j k)}{\partial x_j} = \text{sourceterms} + \frac{\partial}{\partial x_j} \left[ (\nu + \sigma_k \nu_t) \frac{\partial k}{\partial x_j} \right]$$

$$\frac{\partial \omega}{\partial t} + \frac{\partial(U_j \omega)}{\partial x_j} = \text{sourceterms} + \frac{\partial}{\partial x_j} \left[ (\nu + \sigma_\omega \nu_t) \frac{\partial \omega}{\partial x_j} \right]$$

$$\nu_t = \frac{k}{\omega}$$



## Turbulence: two equation models

$$\frac{\partial k}{\partial t} + \frac{\partial(U_j k)}{\partial x_j} = \text{sourceterms} + \frac{\partial}{\partial x_j} \left[ (\nu + \sigma_k \nu_t) \frac{\partial k}{\partial x_j} \right]$$

$$\frac{\partial \omega}{\partial t} + \frac{\partial(U_j \omega)}{\partial x_j} = \text{sourceterms} + \frac{\partial}{\partial x_j} \left[ (\nu + \sigma_\omega \nu_t) \frac{\partial \omega}{\partial x_j} \right]$$

$$\nu_t = \frac{k}{\omega}$$

$$\frac{\partial k}{\partial t} + \frac{\partial \left( U_j k + \sigma_k \frac{\partial \nu_t}{\partial x_j} k \right)}{\partial x_j} = \text{sourceterms} + \frac{\partial}{\partial x_j} \left[ \frac{\partial [(\nu + \sigma_k \nu_t) k]}{\partial x_j} \right]$$

$$\frac{\partial \omega}{\partial t} + \frac{\partial \left( U_j \omega + \sigma_\omega \frac{\partial \nu_t}{\partial x_j} \omega \right)}{\partial x_j} = \text{sourceterms} + \frac{\partial}{\partial x_j} \left[ \frac{\partial [(\nu + \sigma_\omega \nu_t) \omega]}{\partial x_j} \right]$$

"apparent velocity"



## Two equation turbulence models on hierarchical grids

LB methods can be used for solving two-equation turbulence models such as

- k- $\epsilon$ -model (Jones, Launder 1973)
- k- $\omega$ -model (Wilcox)
- zonal models (Shear-Stress-Transport-Model (SST) [Menter, 1992])
- for the source terms, numerical differentiation is necessary



## The SST model

- combining  $k$ - $\omega$ -model near walls and  $k$ - $\varepsilon$ -model in the free stream
- using smart switching function
- able to integrate through the boundary layer without wall functions
- suitable for adverse pressure gradient boundary-layer flows



## The SST model: Boundary conditions

at no-slip walls ( $u=0$ ):

$$k = 0,$$

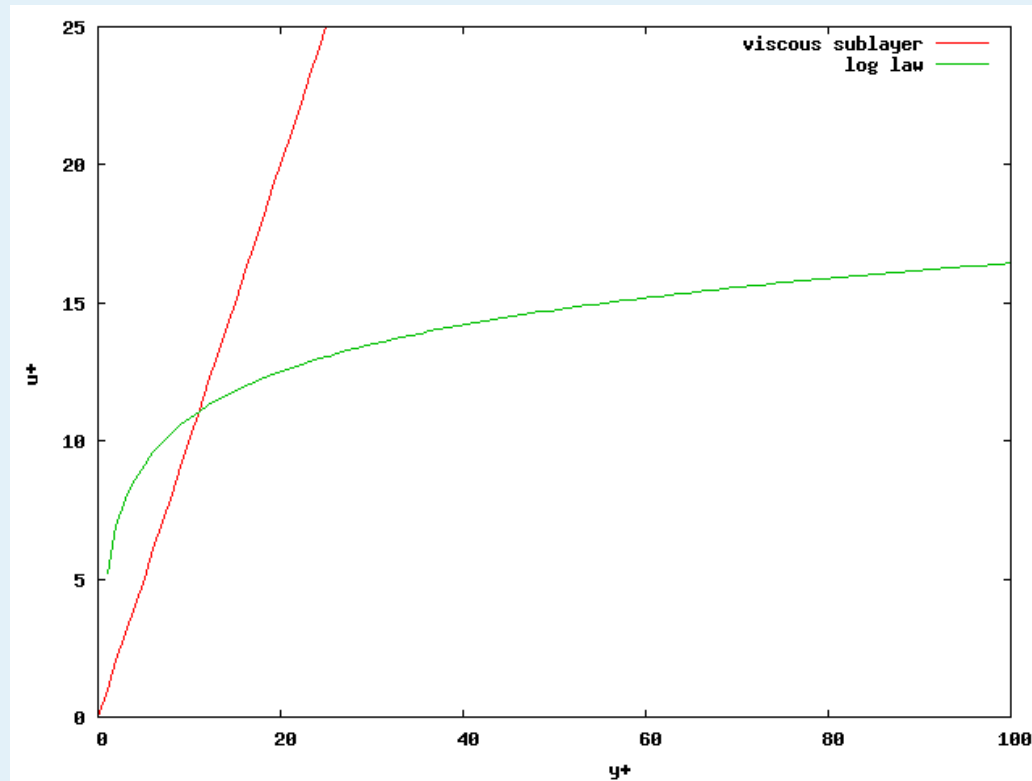
$$\omega = \frac{2500\nu}{k_s^2} \quad (\text{"slightly-rough-surface"-BC, Wilcox}), \quad k_s < 5\delta_\nu$$

=> multireflection for Dirichlet boundary conditions (Ginzburg 2005)

$$f_i(\vec{r}_b, t+1) = (0.5 - \delta_i) \tilde{f}_i(\vec{r}_b, t) + (\delta_i - 1) \tilde{f}_i(\vec{r}_b - \vec{e}_i, t) + 0.5 \tilde{f}_i(\vec{r}_b, t) + f_i^{eq}(\text{wall})$$



## Turbulent channel flow: The law of the wall



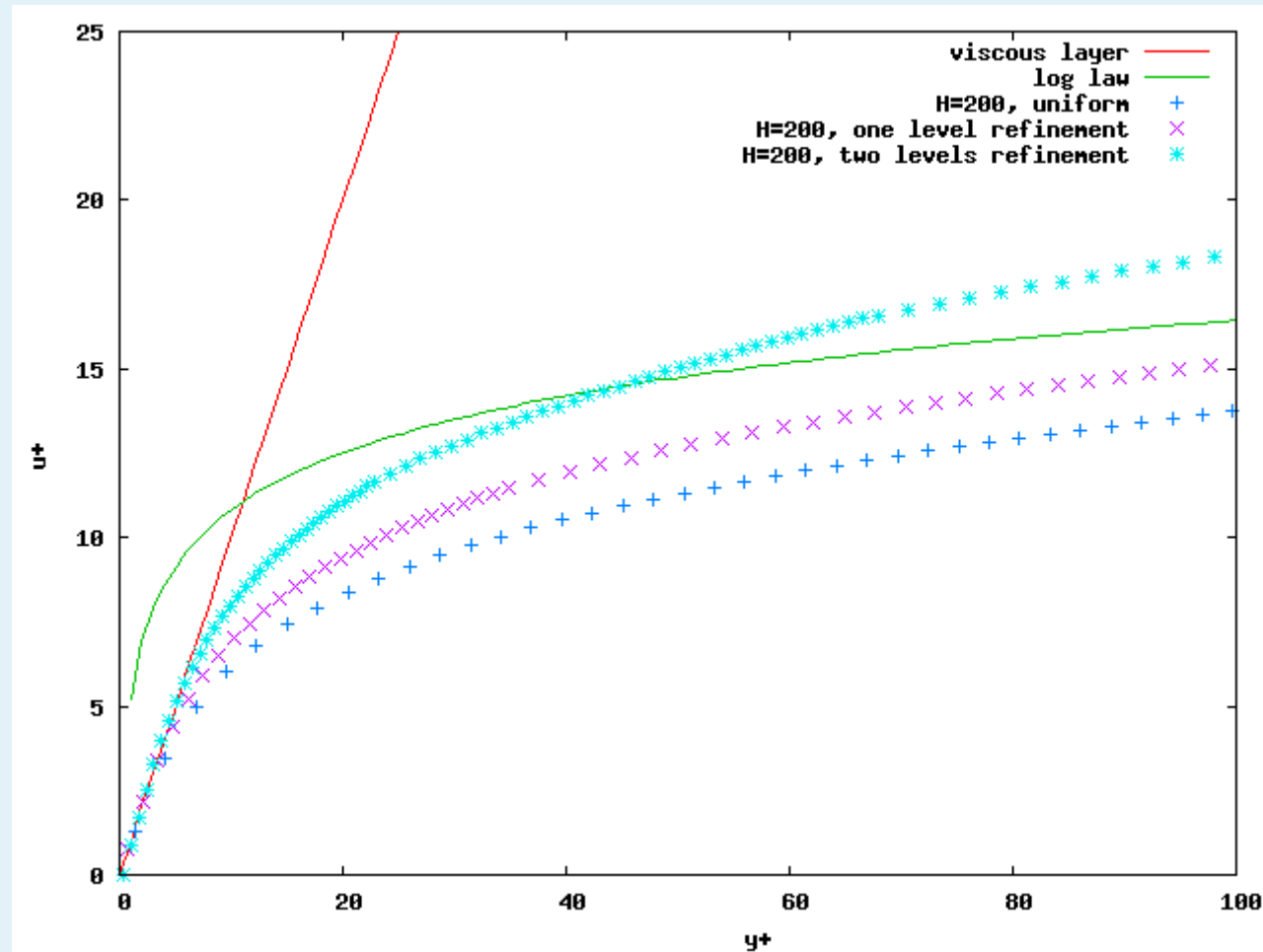
$$u^+ = \frac{\bar{u}}{u_\tau}, \quad y^+ = \frac{y}{\delta_v}$$

$$u_\tau = \sqrt{\frac{\tau_w}{\rho}}, \quad \delta_v = \frac{\nu}{u_\tau}$$





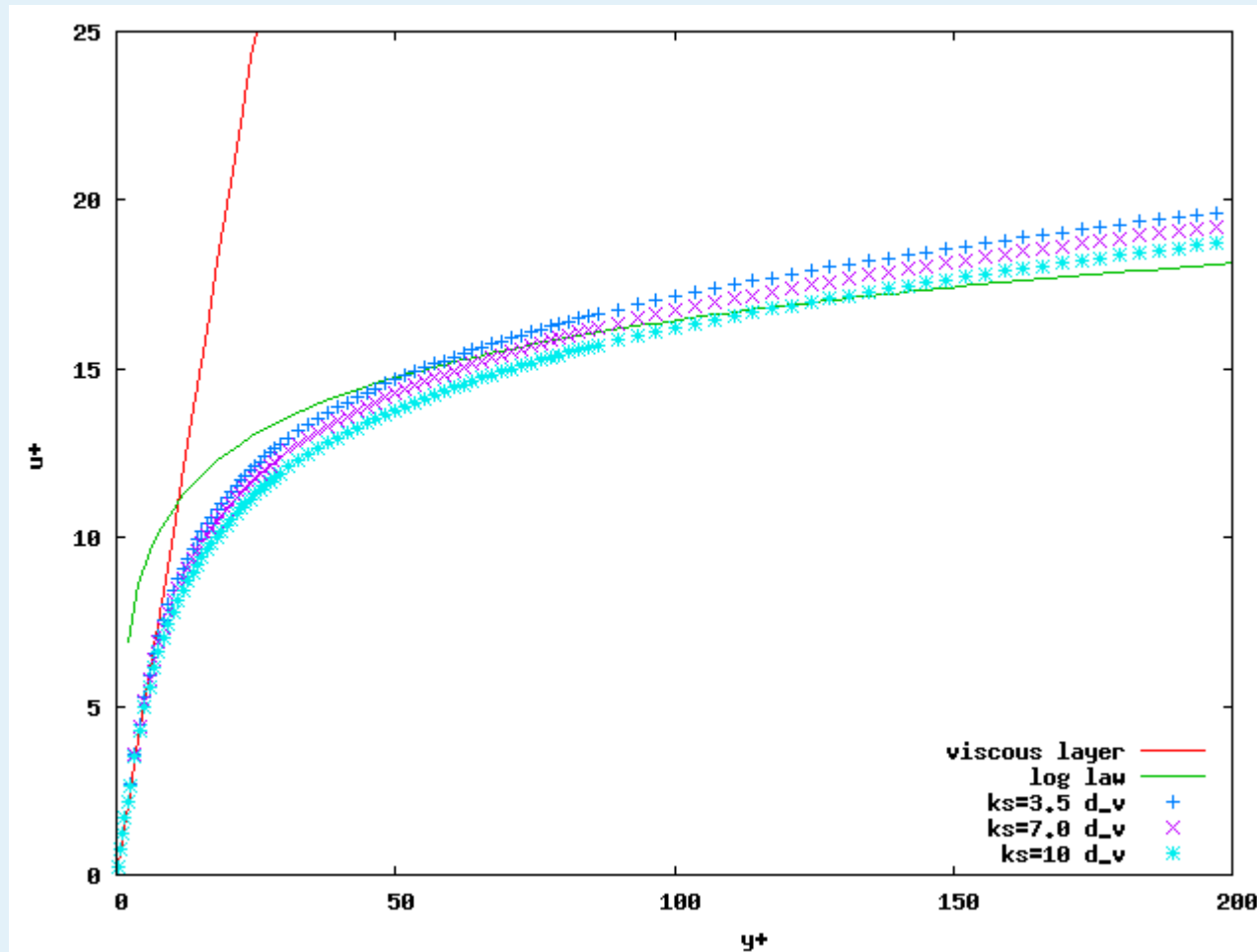
## Refinement of near wall region



Re=11.000



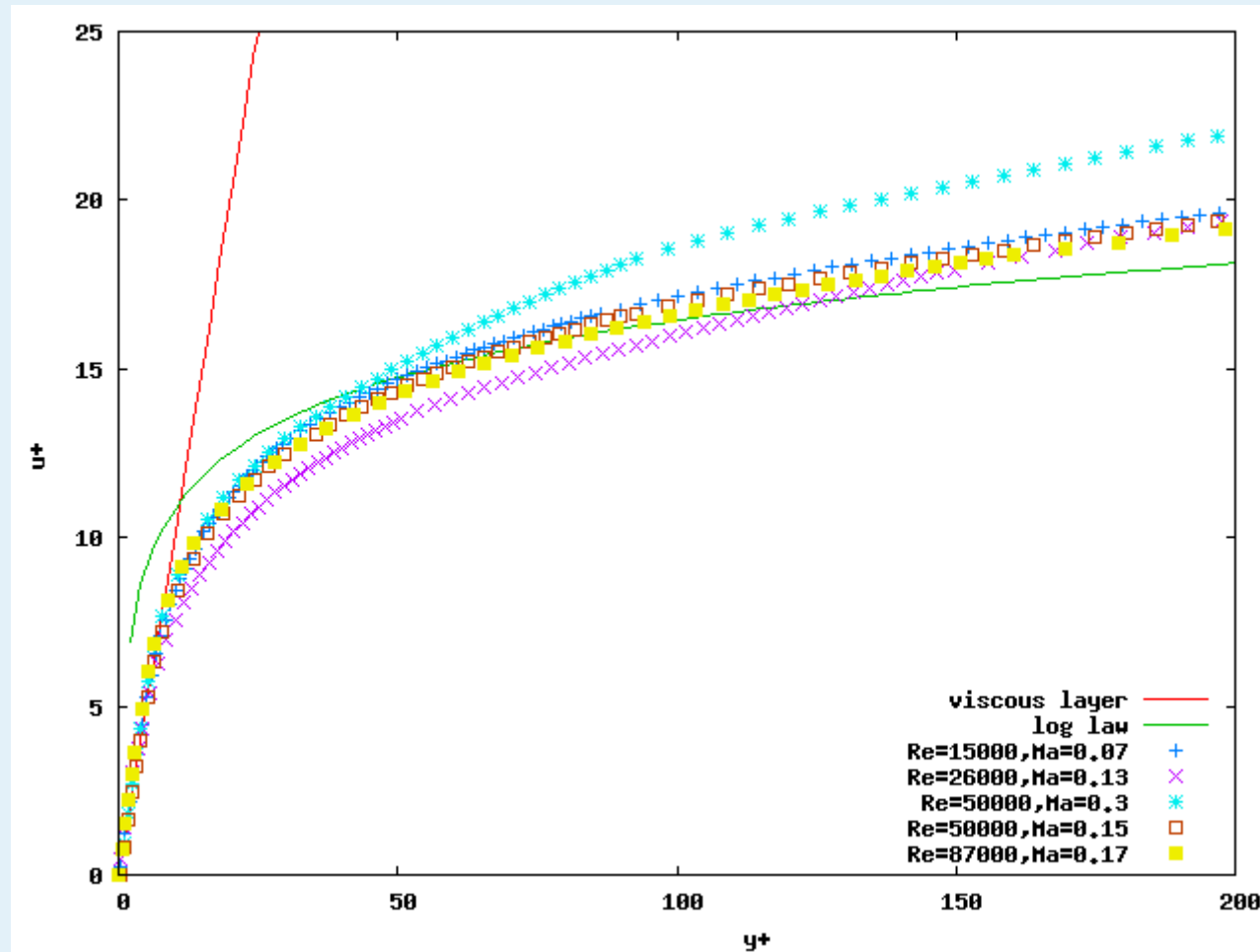
## Influence of wall roughness



$Re=15,000$ ,  
 $Ma=0.07$

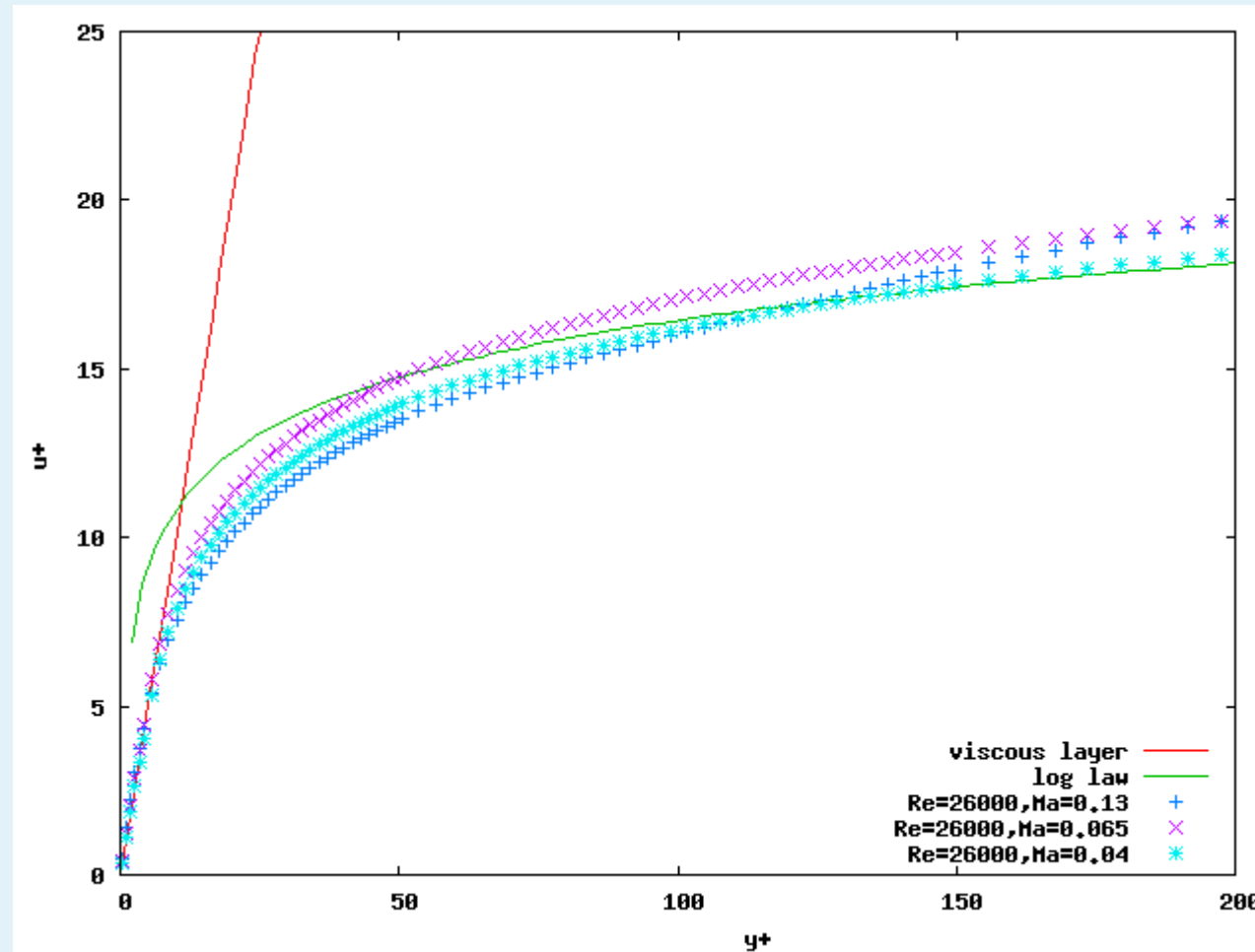


## Channel flow at different Re numbers





## Channel flow at different Ma numbers



Re=26.000



## kinetic turbulence modelling

the vast majority of LB simulations of turbulent flows are based on LES or other classical closure models.

Recently so-called entropic models have been developed (S. Ansumali et al. Physica A 338 (2004) 379-394, Bruce M. Boghosian et al., Physica D 193 (2003) 169-181). These schemes are unconditionally stable due to a built-in „H-function“. Yet, the unresolved scales do not yet show the correct wave number spectrum. Thus at present these models can only be regarded as numerical limiters. A genuinely kinetic turbulence model is yet to be developed.

Another line to substantially improve the stability of LB-methods is the so-called cascaded LB approach by Geier (PRE 2006). A specific sequence of MRT-type relaxations in combination with improved Galilean invariance of third order moments allows A substantial increase in cell Reynolds numbers